M. TECH. ENVIRONMENTAL BIOTECHNOLOGY FIRST YEAR SECOND SEMESTER - 2024

Subject: WASTEWATER TREATMENT Time: Three Hours Full Marks: 100 (70/30 for Part-I/Part-II) & BIOREMEDIATION

Part: Part-I (70 Marks)

Use a Separate Answer-Script for Each Part Answer any 3 (Three) questions (One Mark for Neatness)

- 1. Design a bar rack and screen chamber for fully cleaned as well as 50% clogged conditions with raised 2 floor downstream to the bars. Also, sketch a hydraulic profile through the bar rack and screen chamber. The data given is as follows: Average Flow = 60 MLD; Peak Flow = 180 MLD; Diameter of Incoming Sewer = 1.40 m; Depth of Flow in Sewer at Peak Flow = 1.05 m; Velocity in Sewer at Peak Design Flow = 1.16 m/sec; Drop of Screen Chamber Floor with respect to Sewer Invert = 0.10m; Width of Rectangular Bars = 10 mm; Clear Spacing between Bars = 25 mm; Bar Shape Factor β = 2.42; Inclination of the Bar Screen = 75°. Assume any other suitable data and suitable formula as and when necessary.
- 2. Design grit chamber to remove grit particles based on the following given data. Also design a 23 proportional flow weir (symmetrical sharp-edged; c = 0.61) which acts as a control device at the effluent point. Average Flow = 60 MLD; Peak Flow = 180 MLD; Size and Specific Gravity of the Grit Particles to be removed = 0.15 mm and 2.65; The Minimum Temperature = 15°C and Viscosity $v = 1.14 \times 10^{-6}$ m²/s; Efficiency of Removal $\eta = 75\%$; Measured Settling Basin Performance n = 1/8; K = 0.04 and f = 0.03. Assume any other suitable data and suitable formula as and when necessary.
- 3. (a) Applying the mass balance approach on bio-mass and food, derive the driving equations for an 5 activated sludge process with a completely mixed reactor (with a neat diagram).
 - (b) An activated-sludge system will be used to secondary treatment of 60 MLD municipal wastewater. Raw Wastewater BOD₅ = 300 mg/L; Raw Wastewater SS Concentration = 400 mg/L; Primary Sedimentation Efficiency for BOD Removal = 30%; Primary Sedimentation Efficiency for SS Removal = 70%; Primary Sludge SS Concentration = 40 kg/m³. It is desired to have not more than 5 mg/L of soluble BOD in the ASP effluent. A completely mixed reactor is to be used, and pilot plant analysis has established flowing kinetic values: Y = 0.5 kg/kg, k_d = 0.05/day. Assuming an MLSS concentration of 3000 mg/L and an underflow concentration of 10 kg/m³ from the secondary clarifier. Determine the following: Volume of the Reactor; Quantity of the Secondary Sludge; The Sludge Recycle Ratio. Assume any other suitable data and suitable formula as and when necessary.
- 4. Design a secondary sedimentation tank (circular) to treat effluent from an Activated Sludge Process based 23 on the following data: Average Flow = 60 MLD and Peak Flow Factor = 2.25; Influent MLSS concentration = 3000 mg/L; Surface Loading Rate = 20 m³/ day/ m²; Solid Loading Rate = 80 kg/ day/ m² (Average Flow); Solid Loading Rate = 210 kg/ day/ m² (Peak Flow); Permissible Weir Loading = 150 m³/ day/ m; For effluent weir, provide 90° V-notches @ 20 cm c-c with C_d = 0.60.

Ref. No.: Ex/PG/EBT/T/127/2024

2nd Semester Examination

M. Tech. (Environmental Biotechnology) Session 2023-24

BIOREMEDIATION

Full marks: 100

Time 3 hrs

Part - II (30 Marks)

Each question carries 10 marks. Answer any three questions

- 1. Discuss briefly the biochemical pathways for the anaerobic biodegradation of perchloroethene and aerobic degradation of trichloroethene.
- 2. Discuss briefly the biochemical pathways for the biodegradation of aliphatic and aromatic petroleum hydrocarbons.
- 3. Discuss briefly the importance of biodegradable plastics.
- 4. Discuss briefly how the molecular modification of a detergent transformed it from a recalcitrant to a biodegradable one.
- 5. With diagrams briefly explain sequential anaerobic and aerobic bioremediation in the real field situation.
- 6. Briefly discuss the Lasagna Process of soil bioremediation.