## M.E. BIO-PROCESS ENGINEERING FIRST YEAR SECOND SEMESTER - 2024 Subject: ENVIRONMENTAL BIOTECHNOLOGY Full Marks: 100

## Assume any missing data

1. An activated sludge plant is designed to reduce 95% of influent BOD of 200 mg/L. Compute (a) net sludge (solids) produced per day, (b) mean cell residence time, (c) hydraulic retention time and (d) the F/M ratio for the annual design data given below:

Wastewater flow: 2 MLD, Volume of aeration tank: 400 m<sup>3</sup>, MLVSS in aeration tank: 2500 mg/L, Kinetic coefficients: Y=0.5,  $K_d = 0.08 \text{ d}^{-1}$ .  $U=K_d/Y=K$  S. where U= specific substrate utilization rate, K= specific substrate

utilization rate,  $K_d = \text{decay coefficient}$ , Y is true yield coefficient, [25]

or

Design a conventional activated sludge plant to treat 20000 kl/d of settled solid of BOD is 320 mg/l. The effluent BOD is 30 mg/l. F/M ratio is 0.24,MLSS is 2000 mg/l. Adopt diffusion aeration system SVI = 80. Air required is 120 m $^3$ /d/kg of BOD removed. Standard diffusion plates of 0.3 m x 0.3 m x 25 mm and pore size is 0.3 mm. [25]

2. Assuming suitable design criteria design an oxidation ditch to treat 0.75 MLD flow of wastewater with an influent BOD5 is 220 mg/L to have the desired effluent BOD of 30 mg/L. F/M = 0.2 per day; MLVSS in tank = 2500 mg/L. Assume oxygenation capacity of the cage rotor at 16 cm immersion and 75 rpm equal to 2.5 kg/hr/m length of the rotor [20]

Or,

It is proposed to design an activated sludge plant to treat 7 MLD of domestic wastewater, reducing the concentration of settled BOD<sub>5</sub> from 220 mg/L to 20 mg/L at 20C. Find the volume of aeration tank & hydraulic detention time if  $F/M=0.3d^{-1}$ . At 30 C temperature, calculate  $X_{MLVSS}=3000$ mg/L,Q=2200m<sup>3</sup>/d [Flow of activated sludge from the secondary settling tank] [20]

3. Briefly describe biosensors and its applications [10]

Or

Briefly describe Bioplastic and plastic degradation [10]

4. For a new effluent treatment plant of a petrochemical Industry, which type of effluent treatment unit you suggest to be used (with brief description) and what will be the possible biodegradable product (with mechanism). With a net diagram describe the removal mechanism for anaerobic biological system with possible products. [15+10]

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Briefly describe the packed bed and upflow anaerobic sludge blanket reactor. Write down the factors affecting biodegradation. Briefly describe the mechanism of biodegradation pathways of aliphatic and aromatic compounds.. [10+5+10]

5. Determine the values of bio-kinetic constant using the data given in table derived from the laboratory experiments carried out on the CFSTR model of an activated sludge process without recycle. [20]

Table:

SI No	Influent substrate conc, (mg/L)	Reactor substrate concentration, (mg/L)	Detention time, Days	Reactor biomass concentration (mg/L)
1	300	10	3.75	132
2	300	20	2.65	130
3	300	32	1.62	132
4	300	58	1.25	123