M.E. BIO-PROCESS ENGINEERING FIRST YEAR SECOND SEMESTER 2024

Bioenergy Engineering

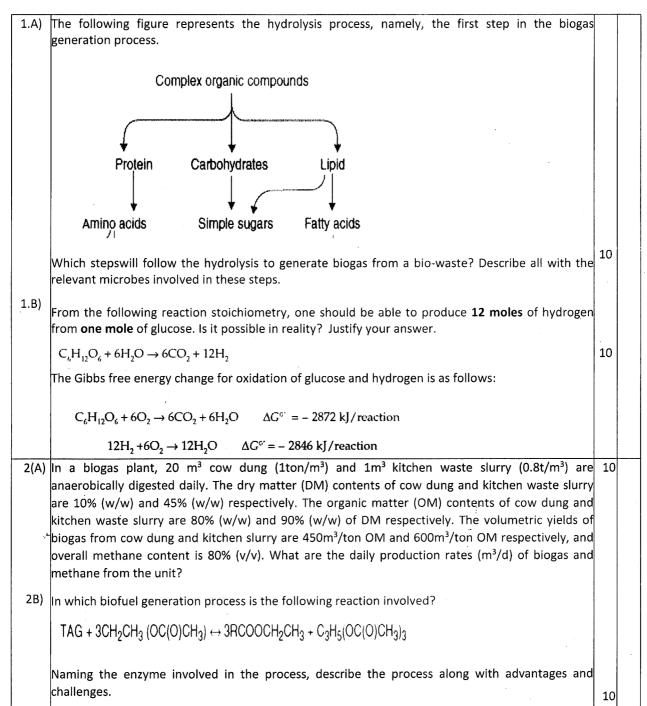
Answer any five questions

Full Marks 100

Assume any missing data

All symbols have usual significance

Time: 3 Hours



2//\	E.coli is genetically modified by the insertion of PET operon represented by the following. Describe	10			
	overall strategy with the pathway for the production of ethanol using genetically modified <i>E.coli</i> strains.				
	Acetaldehyde ADH Ethanol				
3B)	When the bacterium <i>Methylotrophicum</i> is used to produce acetic and butyric acid from CO the following reaction occurs:	10			
	$CO + xO_2 + yN_2 + zH_2O \rightarrow 0.52CO_2 + 0.42CH_2O$				
	$+ 0.024 \text{CH}_2\text{O}_{0.5} + 0.036 \text{ C-mole cells}$				
	The biomass has an elemental composition of $CH_{1.8}O_{0.5}N_{0.2}$. How many moles of oxygen, nitrogen and water are consumed per mole of CO? How many moles of butyric acid and acetic are produced per mole of CO?				
	Discuss on different routes of production of bio-hydrogen. A considerable amount of methane is produced in Norway from its North Sea oil and gas wells. Some of this methane is converted to methanol by partial oxidation and then is biochemically converted to biomass that is used as animal feed. The reported stoichiometry of the biochemical reaction is	10			
	$CH_3OH + 0.731O_2 + 0.146 NH_3 \rightarrow 0.269CQ_2 + 0.731C - mol\ biomass$				
	What is the atomic composition of biomass produced?				
	How much heat is produced per mole of methanol consumed?				
	What fraction of Gibbs free energy of reactants is present in the biomass?				
	Assume the validity of energy regularity approximation ($\Delta_c G=112\xi~and~\Delta_c H=110.9\xi$).				
		12			
	You have been asked to produce electricity from wastewater containing organic waste and the COD value is 0.64g/L . Which bioprocess would you recommend. Describe the process with its typical arrangement, microbe specificity, calculation of efficiency and challenges.				
5B)	Describe the role of algae in CO₂ capture and generation of biochemicals.	7			
6A)	What do you mean by "Energy transition" and "Biorefinery" concept?	2+			
00,	A single chambered MFC equipped with PEM and an air cathode is run using glucose at a concentration of $1g/L$. The available anode surface area is $5\times 10^{-4}m^2$ and the anode volume is $0.025L$. The average voltage has been determined to be $0.3V$ over $10h$ operation when a 500Ω resistor is used. Determine the average power density on the basis of surface area and the coulombic efficiency of the cell. [F=96485C/mol $e^ available$]				
6C)	A bioprocess uses substrate, S, NH ₃ as nitrogen source along with oxygen and water to generate biomass, B, and a product, P along with CO ₂ . Defining $Y_{Q/S}$, correlate $Y_{Q/S}$ with $Y_{B/S}$, $Y_{P/S}$, $Y_{N/S}$, ξ_B , ξ_P , ξ_N and ξ_S .				

	trogen source is cons S (Substrate)	N (Nitrogen source)	B (Biomass)	P (Product)	
nd 0.0399 mole of ni		***************************************			
and 0.0399 mole of nitrogen source is consumed.					
Per C-mole of a substrate, 0.451C-mole of a product and 0.235C-mole of biomass are produced					
(iv)Limit of 2 nd law of thermodynamics on a bioprocess from the following case study:					
(iii) Algal lipid and Strategy for enhancement of Production					
	on through ED nathur	/av			5x 4
	a representative gro	wth rate equal	ion under such	situation.	_
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		-		aring the validity of both	
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		f hydrogen ger			
initially. Generation of hydrogen is growth associated and from the perspective of growth under					
•	sure of hydrogen	ı in overhea	d aas phase :	$= v_{\mu_{-}} * P_{T}$	
	e concentration of	nyarogen in	equilibrium w	itn tne	
		- (-)		14h 4h a	
			•	•	
vhere,					
$n_{H_2} = y_{H_2} * P_T \left(\frac{v_{ove}}{r} \right)$	$rac{crhead}{RT} + K_{H_2} * V_{Liqui}$	$_d$) * (MW_{H_2})	(i)	
				ly time can be correlated	
hase concer	ntration of	hydrog	en, in	terms of	
					13
	ydrogen using hyper he dilution rate is or ressure (gauge) means hase concernole fraction (or vectormined using gastlenry's law. It is know that the total overhead $m_{H_2} = y_{H_2} * P_T \left(\frac{v_{overhead}}{v_{overhead}} \right)$, where, $m_{H_2} = m_{overhead} $ $m_{H_2} = m_{H_2} + m_{overhead} $ $m_{H_2} = m_{overhead} $ $m_{H_2} = m_{H_2} + m_{H_2} + m_{Overhead} $ $m_{H_2} = m_{H_2} + m_{H$	ydrogen using hyperthermophilic bacter he dilution rate is $0.84h^{-1}$ and the feet ressure (gauge) measured under steady hase concentration of mole fraction (or volume fraction) of etermined using gas chromatograph (Gilenry's law. It is known that mass of hypith the total overhead pressure (P_T) with $n_{H_2} = y_{H_2} * P_T \left(\frac{V_{overhead}}{RT} + K_{H_2} * V_{Liquit} \right)$ where, $N_{H_2} = M_{I} + N_{I} $	ydrogen using hyperthermophilic bacterial strain T . M he dilution rate is $0.84h^{-1}$ and the feed concentration ressure (gauge) measured under steady state is $175kP$ hase concentration of hydrogen N hase concentration of hydrogen N determined using gas chromatograph (GC). Liquid phase lenry's law. It is known that mass of hydrogen general with the total overhead pressure (P_T) with the following $N_{H_2} = N_{H_2} * P_T \left(\frac{V_{overhead}}{RT} + K_{H_2} * V_{Llquid} \right) * \left(\frac{MW_{H_2}}{R} \right)$ where, $N_{H_2} = M_{O} = M_{O}$	ydrogen using hyperthermophilic bacterial strain T . $maritima$ at optice dilution rate is $0.84h^{-1}$ and the feed concentration of glucose is ressure (gauge) measured under steady state is $175kPa$ (atmospheric hase concentration of hydrogen, in the fraction (or volume fraction) of hydrogen gas in the overhetermined using gas chromatograph (GC). Liquid phase concentration lenry's law. It is known that mass of hydrogen generated (m_{H_2}) at a right the total overhead pressure (P_T) with the following equation: $m_{H_2} = y_{H_2} * P_T \left(\frac{v_{overhead}}{RT} + K_{H_2} * V_{Liquid} \right) * \left(MW_{H_2} \right)$ (if there, $MW_{H_2} = molecular$ weight of hydrogen. $MW_{H_2} = molecular$ weight of hydrogen. $MW_{H_2} = molecular$ weight of hydrogen. $MW_{H_2} = molecular$ weight of hydrogen in equilibrium we overhead gas; $MW_{H_2} = partial$ pressure of hydrogen in overhead gas phase in the growth is uninhibited and follows Monod kinetics. There is no hydrogen in the growth is uninhibited and follows Monod kinetics. There is no hydrogen state, equation (ii) gives the mass of hydrogen generated as follows $MW_{H_2} = mW_{H_2} + WW_{H_2} + W$	etermined using gas chromatograph (GC). Liquid phase concentration is determined applying lenry's law. It is known that mass of hydrogen generated (m_{H_2}) at any time can be correlated with the total overhead pressure (P_T) with the following equation: $n_{H_2} = y_{H_2} * P_T \binom{V_{overhead}}{RT} + K_{H_2} * V_{Liquid} $ $* (MW_{H_2})$ (i) where, $MW_{H_2} = molecular\ weight\ of\ hydrogen.$ $K_{H_2} = Henry's\ law\ constant;\ Henry'slaw: C_{H_2(I)} = K_{H_2}p_{H_2}$ $K_{H_2(I)} = liquid\ phase\ concentration\ of\ hydrogen\ in\ equilibrium\ with\ the\ loverhead\ gas; K_{H_2} = partial\ pressure\ of\ hydrogen\ in\ overhead\ gas\ phase = y_{H_2} * P_T\ he\ growth\ is\ uninhibited\ and\ follows\ Monod\ kinetics.\ There is\ no\ hydrogen\ present\ in\ the\ system\ intially.\ Generation\ of\ hydrogen\ is\ growth\ associated\ and\ from\ the\ perspective\ of\ growth\ under\ teady\ state,\ equation\ (ii)\ gives\ the\ mass\ of\ hydrogen\ generated\ as\ follows: n_{H_2} = Y_{H_2/X} * C_{XS} * V_{Liquid} (ii) Where, C_{XS} = biomass\ concentration\ under\ steady\ state omehow, the laboratory GC is temporarily not in operation. Considering the validity of both quations (ii) and (iii), determine the\ hydrogen\ concentration\ in\ the\ overhead\ in\ terms\ of\ y_{H_2}. ata: \mu_{max} = 0.94h^{-1};\ K_s = \frac{0.57g}{L};\ Y_{x/s} = 0.248\frac{g\ biomass}{g\ substrate};\ Y_{H_2/X} = 0.19\frac{g\ H_2}{g\ biomass};\ R = .314\ L.\ kPa/mol.\ K;\ K_{H_2} = 7.21X10^{-6}\ M/kPa\ at\ 70^{\circ}C. The growth of hydrogen generating microorganism is usually inhibited\ at\ high\ hydrogen\ partial\ ressure. Write\ down\ a\ representative\ growth\ rate\ equation\ under\ such\ situation. Discuss on (i) Ethanol production\ through\ ED\ pathway (ii) Algal lipid\ and\ Strategy\ for\ enhancement\ of\ Production$