

M.E. CHEMICAL ENGINEERING FIRST YEAR SECOND SEMESTER EXAM 2024**Subject : BIOENERGETICS AND
BIOPROCESS ENGINEERING****Time : 3 hr****Full Marks : 100****Part I (50 Marks)****Assume any missing data
Answer any two questions**

1. a.. Describe encapsulation immobilization process and its application 5

b. An enzyme has a K_m of $4.2 \times 10^{-5} M$. If the V_{max} of the preparation is $24 \mu\text{moles l}^{-1} \text{Mole}^{-1}$, what velocity would be observed in the presence of $2 \times 10^{-4} M$ substrate and 5.4×10^{-4} of a) a competitive inhibitor, b) a non competitive inhibitor c) an uncompetitive inhibitor. K_i in all three cases is $3 \times 10^{-4} M$. d) What is the degree of inhibition in all three cases. 20

2. A strain of mold was grown in a batch culture on glucose and the following data were obtained:

Time, hr	Cell concentration (g/L)	Glucose concentration, g/L
0	1.25	100
9	2.42	97
14	5	90.4
24	10.5	76.9
30	22	48.1
34	33	20.6
36	37.5	9.38
42	41	0.36

Calculate the maximum net specific growth rate, apparent growth yield and maximum cell concentration could one expect if 120 gm of glucose were used with the same size inoculum. 9

Derive the expression for un-competitive inhibition. 8

Write the application of enzyme in Food and textile industry 4 + 4

3. The following data have been obtained two different initial enzyme concentration for an enzyme-catalyzed reaction.

v ($[E_0] = 0.012 \text{ g/l}$) g/l-min	$[S]$ (g/l)
1.14	20
0.86	10
0.7	6.7
0.59	5
0.5	4
0.45	3.0

- i) Find K_m ii) k_2 and iii) find V_m

[Turn over

[2]

Where V_m is maximum forward velocity of the reaction, K_m is dissociation constant of the ES (Enzyme – substrate) complex, k_2 is rate constant. 20

What is the difference between structured and unstructured models? What will be the Monod model equation for two limiting substrate 5

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Part-II

Use Separate Answer scripts for each part

Answer any *two* questions

1	<p>(a) What are the advantages and disadvantages of different types of coagulation and flocculation agents used in algae harvesting.</p> <p>(b) Develop the expression to calculate the settling velocity of an algae biomass particle of spherical shape in a fluid in the laminar flow region ($Re < 1$)</p> <p>(c) To produce a new algae in a location with low sunlight irradiance, halogen lamps are planned to be installed to irradiate tubular photobioreactors (PBRs) in parallel arrangement with floor area occupied by one PBR=18.6 m^2. The effective continuous irradiance provided by these lamps is $500 \text{ } \mu\text{mol m}^{-2} \text{ s}^{-1}$. The initial biomass concentration in the feed is 1 kg m^{-3}. Calculate:</p> <p>(i) The algae biomass productivity in a tubular PBR with a volume of 1.7 m^3 for a liquid feed flow rate of $10 \text{ m}^3 \text{ h}^{-1}$.</p> <p>(ii) The number of PBRs of the given volume capacity and the land used for an oil production of 10000 t y^{-1} assuming an oil content of 35% by mass in the algae biomass. (Assume 300 operating days in a year, $\mu_{\text{max}} = 0.1 \text{ h}^{-1}$, $K_I = 70 \text{ } \mu\text{mol m}^{-2} \text{ s}^{-1}$)</p> <p>(iii) If CO_2 is supplied by bubbling 200 mol h^{-1} of a flue gas stream containing 10% by mole of CO_2 what will be the CO_2 capture rate in relation to the CO_2 input in the gas stream.</p>	5+5+15																																							
2	<p>(a) Estimate the annual algae biomass production per unit of land for the species X [$P_{c,\text{max}} = 1 \text{ d}^{-1}$, $r_m = 0.05 \text{ d}^{-1}$, $\theta_{\text{max}} = 0.09 \text{ g chlorophyll g}^{-1} \text{ C}$, $a = 5 \text{ g C (mol}^{-1} \text{ photons) m}^2 \text{ g}^{-1} \text{ chlorophyll}$]. The steady state concentration is 0.5 kg/m^3 and the pond depth is $z = 0.3 \text{ m}$. The actual water surface is 80% of the total area, $h = 0.8$. Assume algae cultivation at average pond water temperature and sunlight. Neglect the effect of CO_2 and variations in concentration with depth. The monthly average irradiation for the pond location and average pond water temperature is as follows:</p> <table><tr><th>Month</th><th>Jan</th><th>Feb</th><th>Mar</th><th>April</th><th>May</th><th>June</th><th>July</th><th>Aug</th><th>Sept</th><th>Oct</th><th>Nov</th><th>Dec</th></tr><tr><td>Irradiation (W/m^2)</td><td>35</td><td>50</td><td>80</td><td>100</td><td>120</td><td>150</td><td>140</td><td>130</td><td>100</td><td>75</td><td>40</td><td>35</td></tr><tr><td>Water Temp ($^{\circ}\text{C}$)</td><td>3</td><td>5</td><td>8</td><td>12</td><td>15</td><td>20</td><td>21</td><td>18</td><td>16</td><td>13</td><td>11</td><td>3</td></tr></table> <p>Calculate the annual oil yield if the avg. oil content in the algae biomass cell is 30%. Given: $T_{\text{op}} = 22^{\circ}\text{C}$, $T_d = 35^{\circ}\text{C}$, $\beta = 1.5$, oil density = 0.87 kg/L</p> <p>(b) What is algae shadowing effect and how light irradiation is affected by it?</p>	Month	Jan	Feb	Mar	April	May	June	July	Aug	Sept	Oct	Nov	Dec	Irradiation (W/m^2)	35	50	80	100	120	150	140	130	100	75	40	35	Water Temp ($^{\circ}\text{C}$)	3	5	8	12	15	20	21	18	16	13	11	3	20+5
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3	<p>(a) Working procedure of microbial fuel cell (MFC) in a single chamber and two chamber set up.</p>	5+5+5+10																																							