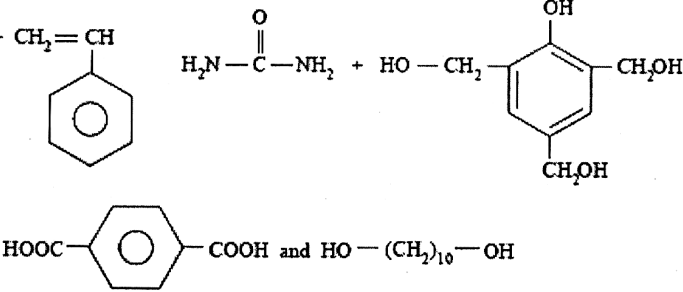


**B.E. CHEMICAL ENGINEERING FOURTH YEAR
SECOND SEMESTER EXAM 2024**

HIGH POLYMER TECHNOLOGY

FM-100

Time-3hrs

Question No	CO No.	Question	Marks
1	CO-1	<p>(i) How molecular weight distribution is related with functionality for bi/polyfunctional system?</p> <p>(ii) Show the branch point formation considering the reaction between diamine and epoxy.</p> <p>(iii) Derive the kinetic relations of self-catalysed condensation reaction. Write down the reasons behind deviation from linearity in degree of polymerization vs time curve.</p> <p>(iv) Write down the structure of the repeat unit of the following:</p> <div style="text-align: center;"> $\text{CH}_2=\text{CH}-\text{CN} + \text{CH}_2=\text{CH}-\text{C}_6\text{H}_5$  $\text{HOOC}-\text{C}_6\text{H}_4-\text{COOH} \text{ and } \text{HO}-(\text{CH}_2)_{10}-\text{OH}$ </div>	4+4+6+6=20
2	CO-2	<p>(i) a. Polyester fibers can be produced from ω = hydroxycaproic acid.</p> <div style="text-align: center;"> $n\text{HO}-(\text{CH}_2)_5-\text{C}(=\text{O})-\text{OH} \xrightarrow{\Delta} \left[-(\text{CH}_2)_5-\text{C}(=\text{O})-\text{O}- \right]_n + 2n\text{H}_2\text{O}$ </div> <p>If the initial 100 moles of the hydroxyl acid are reduced to 5 moles after 12 hours reaction time, calculate:</p> <ol style="list-style-type: none"> The number average molecular weight M_n The weight average molecular weight M_w <p>b. As a result of extraneous reactions of the hydroxyl groups, a 3% excess of the carboxylic acid is present in the reaction mixture. Calculate the number-average molecular weight for the same extent of reaction in a.</p> <p>c. If 4 mol% of monoacid is present as impurity. What will be the maximum degree of polymerization?</p> <p>(ii) Write short notes on: (a) Zeigler Natta polymerization (c) Retardation effect</p> <p>(iii) From the data given below for the emulsion polymerization styrene in water at 60°C:</p> <ol style="list-style-type: none"> Calculate the rate of polymerization. (4) 	10+10+10=30

[Turn over

		<p>b. Show that the number average degree of polymerization. (4)</p> <p>c. Estimate the number of polymer chains in each. (4)</p> <p>Data:</p> <p>$K_p = 200 \text{ l mol}^{-1} \text{ s}^{-1}$</p> <p>$R_i = 5 \times 10^{12} \text{ radicals cc}^{-1} \text{ s}^{-1}$</p> <p>$N = 10^{13} \text{ particles cc}^{-1}$</p> <p>$[M] = 10 \text{ M}$</p> <p>Latex particle size = $0.20 \mu\text{m}$</p> <p>Particle density = 1.5 g/cc</p>																																																														
3	CO-3	<p>(i) Discuss glass-rubber transition behaviour of polymer.</p> <p>(ii) Estimate the feed and copolymer compositions for the azeotropic copolymerization of 1,3 butadiene and vinyl chloride at 50°C.</p> <table><thead><tr><th>Monomer 1</th><th>Monomer 2</th><th>r_1</th><th>r_2</th><th>T ($^\circ\text{C}$)</th></tr></thead><tbody><tr><td rowspan="5">Acrylonitrile</td><td>1,3-Butadiene</td><td>0.02</td><td>0.30</td><td>40</td></tr><tr><td>Methyl methacrylate</td><td>0.15</td><td>1.22</td><td>80</td></tr><tr><td>Styrene</td><td>0.04</td><td>0.40</td><td>60</td></tr><tr><td>Vinyl acetate</td><td>4.2</td><td>0.05</td><td>50</td></tr><tr><td>Vinyl chloride</td><td>2.7</td><td>0.04</td><td>60</td></tr><tr><td rowspan="3">1,3-Butadiene</td><td>Methyl methacrylate</td><td>0.75</td><td>0.25</td><td>90</td></tr><tr><td>Styrene</td><td>1.35</td><td>0.58</td><td>50</td></tr><tr><td>Vinyl chloride</td><td>8.8</td><td>0.035</td><td>50</td></tr><tr><td rowspan="3">Methyl methacrylate</td><td>Styrene</td><td>0.46</td><td>0.52</td><td>60</td></tr><tr><td>Vinyl acetate</td><td>20</td><td>0.015</td><td>60</td></tr><tr><td>Vinyl chloride</td><td>10</td><td>0.1</td><td>68</td></tr><tr><td rowspan="2">Styrene</td><td>Vinyl acetate</td><td>55</td><td>0.01</td><td>60</td></tr><tr><td>Vinyl chloride</td><td>17</td><td>0.02</td><td>60</td></tr></tbody></table> <p>(iii) 0.25 gm of polystyrene (PS) sample is dissolved in 200 ml of butanone. Flow time of are measured employing ubbelhode capillary viscometer. Determine the molecular weight of PS.</p> <p>Given: Flow time of butanone = 130 sec and that of PS solution is 160 sec. $K = 40 \times 10^{-3}$ and $a = 0.6$</p> <p>(iv) Calculate the time required for 30 % polymerization of pure styrene at 60°C with benzoyl peroxide as the initiator in a batch reactor. Assume that the initiator concentration remains (a) constant and (b) first order decay.</p> <p>Data:</p> <p>$f = 1$</p> <p>$K_p^2/K_t = 2 \times 10^{-3} \text{ l/mol-s}$</p> <p>$[I] = 6.0 \times 10^{-3} \text{ mol/l}$</p> <p>$K_d = 2 \times 10^{-6} \text{ s}^{-1}$</p>	Monomer 1	Monomer 2	r_1	r_2	T ($^\circ\text{C}$)	Acrylonitrile	1,3-Butadiene	0.02	0.30	40	Methyl methacrylate	0.15	1.22	80	Styrene	0.04	0.40	60	Vinyl acetate	4.2	0.05	50	Vinyl chloride	2.7	0.04	60	1,3-Butadiene	Methyl methacrylate	0.75	0.25	90	Styrene	1.35	0.58	50	Vinyl chloride	8.8	0.035	50	Methyl methacrylate	Styrene	0.46	0.52	60	Vinyl acetate	20	0.015	60	Vinyl chloride	10	0.1	68	Styrene	Vinyl acetate	55	0.01	60	Vinyl chloride	17	0.02	60	5+5+5+10=25
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4	CO-4	<p>Write short note on: Extrusion, Dipping</p> <p>Or</p> <p>Discuss the different steps associated with injection molding process?</p>	10																																																													
5	CO-5	Write the manufacturing method of Poly ethylene with PFD.	15																																																													
Total			100																																																													