BACHELOR OF CHEMICAL ENGINEERING EXAMINATION, 2024

(2nd Year, 1st Semester)

CHEMICAL PROCESS PRINCIPLES

Time: Three hours Full Marks: 100

(Attempt all questions)

		Marks
	CO ₁	
Q1	Do solve the followings: (i) Convert the 67 PSI to Pa (ii) Convert the 14.7 atm to Pa	5×3=15
,	(iii) Convert the 54 PSF to atm (iv) Convert pressure of 1 mm H2O to Pa (v) Convert the poundal to N	3/3-13
	CO ₃	
Q2	An experiment on the growth rate of certain organisms requires an environment of humid air enriched in oxygen. Three input streams are fed into an evaporation chamber to produce an output stream with the desired composition. A: Liquid water, fed at a rate of 20.0 cm /min B: Air (21 mole% O, the balance N) C: Pure oxygen, with a molar flow rate one-fifth of the molar flow rate of stream B	15
Q3	The output gas is analyzed and is found to contain 1.5 mole% water. Draw and label a flowchart of the process, do degrees of freedom analysis and calculate all unknown stream variables. Elaborate the followings:	
	(i) Wet-bulb temperature and dry-bulb temperature(ii) Degree of freedom	5×2=10
	CO ₄	
Q4	Assuming ideal gas behavior, calculate the heat that must be transferred in each of the following cases. (i) A stream of nitrogen flowing at a rate of 100 mol/min is heated from 20 °C to 100 °C. (ii) Nitrogen contained in a 5-liter flask at an initial pressure of 3 bar is cooled from 80 °C to 20 °C	15
Q5	One hundred g-moles per hour of liquid -hexane at 30 °C and 7 bar is vaporized and heated to 250 °C at constant pressure. Neglecting the effect of pressure on enthalpy, estimate the rate at which heat must be supplied.	20
	CO ₅	
Q6	Air at 75 °F and 75% relative humidity is cooled to 56 °F at a constant pressure of 1 atm. Use the psychrometric chart to calculate the fraction of the water that condenses and the rate at which heat must be removed to deliver 1000 ft³/min of humid air at the final condition.	25

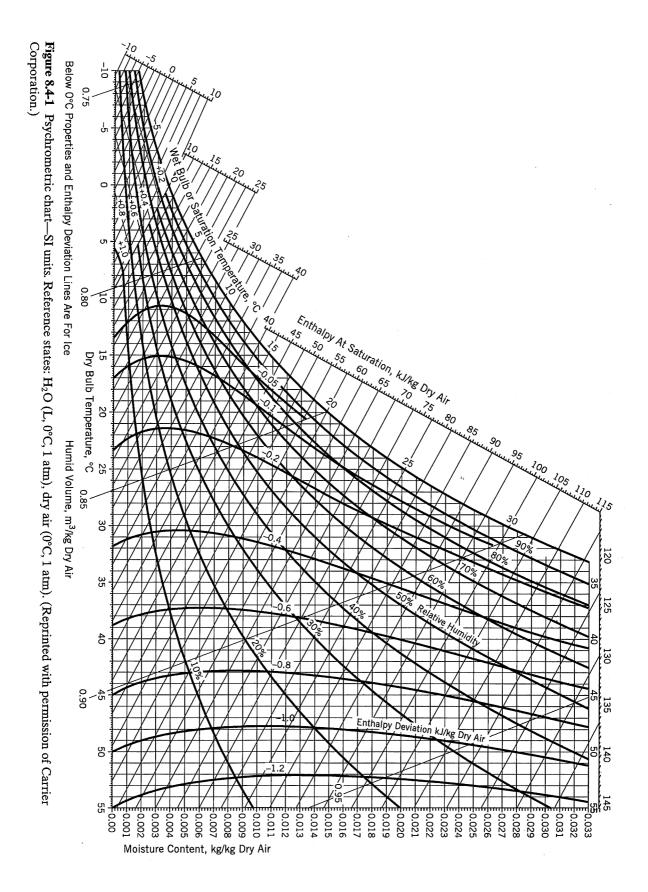
Properties Table

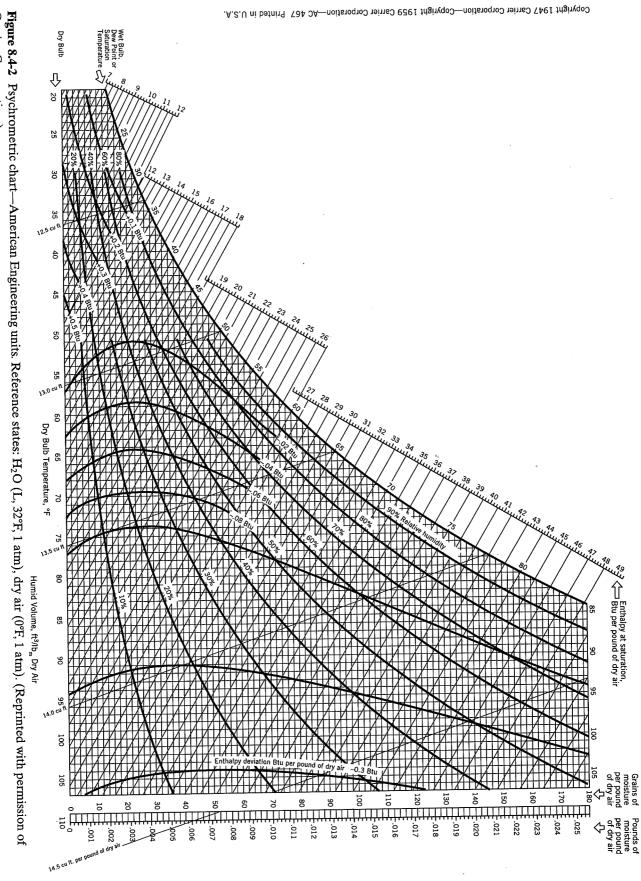
Table B.1: Selected Physical Property Data

Compou nd	Formul a	Mol. Wt.	SG (20° /4°)	$T_m(^{\circ}\mathbb{C})^b$	$\Delta \widehat{H}_m(T_m)^c$ kJ/mol	$T_b(^{\circ}\mathrm{C})^d$	$\Delta \widehat{H}_V(T_b)^{e,j}$ kJ/mol	$T_C(K)^f$	P _C (atm	$\left(\Delta H_f^o\right)^{h,j}$ kJ/mol	(ΔH _c ^o) ^{i,j} kJ/mol
N-Hexane	C ₆ H ₁₄	86.17	0.659	- 95.32	13.03	68.74	28.85	507.9	29.9	198.8(l) 167.2(g)	- 4163.1(l) - 4194.8(g)
Nitrogen	N ₂	28.02		- 210.0	0.720	- 195.8	5.577	126.20	33.5	o (g)	

Table B.2: Heat Capacities

Compo und	Form ula	Mol. Wt.	Sta te	Form	Temp Unit	a×103	b×10 ⁵	C×10 ⁸	d×1012	Range (Units of T)
N-	C ₆ H ₁₄	86.17	Ť	4	°C	216.3				20–100
N- Hexane	C6H14	80.17	g	1	°C	137.44	40.85	- 23.92	57.66	0-1200
Nitrogen	N ₂	28.02	g	1	°C	29.00	0.2199	0.5723	- 2.871	0–1500





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