

**B.E. CHEMICAL ENGINEERING THIRD YEAR FIRST SEMESTER SUPPLEMENTARY  
EXAMINATION 2023**

**PROCESS HEAT TRANSFER**

Time : Three hours

Full Marks : 100

( 50 Marks for each Part ) Use separate answer script for each Part

**PART I (50 Marks)**

CO-1	<p>1. A spherical container of negligible thickness holding a hot fluid at <math>140^{\circ}\text{C}</math> and having an outer diameter of 0.4 m is insulated with three layers of each 50 mm thick insulation of <math>k_1 = 0.02</math>; <math>k_2 = 0.06</math> and <math>k_3 = 0.16</math> W/mK. (Starting from inside). The outside surface temperature is <math>30^{\circ}\text{C}</math>. Determine (i) the heat loss, and (ii) Interface temperatures of insulating layers.</p> <p align="center"><b>Or</b></p> <p>2. A spherical element of 40 mm diameter is initially at temperature of <math>27^{\circ}\text{C}</math>. It is placed in boiling water for 4 minutes. After 4 minutes, at what temperature, the spherical element will reach? If the same spherical element is initially at <math>0^{\circ}\text{C}</math>, find out by lump theory that how much time will be taken by the element to reach at that temperature? Take properties of the given spherical element as: <math>K = 10\text{W/m}^{\circ}\text{c}</math>; <math>\rho = 1200\text{ kg/m}^3</math>; <math>C_p = 2\text{kJ/kg}^{\circ}\text{C}</math>; <math>h = 100\text{ W/m}^2\text{c}</math></p>	10
CO-2	<p>A steam pipe of 10 cm ID and 11 cm OD is covered with an insulating substance <math>k = 1\text{W/mK}</math>. The steam temperature is <math>200^{\circ}\text{C}</math> and ambient temperature is <math>20^{\circ}\text{C}</math>. If the convective heat transfer coefficient between insulating surface and air is <math>8\text{ W/m}^2\text{K}</math>, find the critical radius of insulation for this value of <math>r_c</math>. Calculate the heat loss per meter of pipe and the outer surface temperature. Neglect the resistance of the pipe material.</p> <p align="center"><b>Or</b></p> <p>A motor body is 360 mm in diameter (outside) and 240 mm long. Its surface temperature should not exceed <math>55^{\circ}\text{C}</math> when dissipating 340W. Longitudinal fins of 15 mm thickness and 40 mm height are proposed. The convection coefficient is <math>40\text{W/m}^2\text{C}</math>. determine the number of fins required. Atmospheric temperature is <math>30^{\circ}\text{C}</math>. Thermal conductivity = <math>40\text{ W/m}^{\circ}\text{C}</math>.</p>	10
CO-3	<p>A 70 mm thick metal plate with a circular hole of 35 mm diameter along the thickness is maintained at a uniform temperature <math>250^{\circ}\text{C}</math>. Find out the associated view factors and the loss of energy to the surroundings at <math>27^{\circ}\text{C}</math>, assuming the two ends of the hole to be as parallel discs and the metallic surfaces and surroundings have black body characteristics. Given : <math>F_{2-3} = 0.065</math> and <math>F_{2-2} = 0</math></p>	10
CO-5	<p>1. Hot oil enters into a counter flow heat exchanger at <math>150^{\circ}\text{C}</math> and leaves at <math>40^{\circ}\text{C}</math>. The mass flow rate of oil is 4500 kg/hr and its specific heat is 2 kJ/kg-K. The oil is cooled by water which enters the heat exchanger at <math>20^{\circ}\text{C}</math>. The overall heat transfer coefficient is <math>1400\text{ W/m}^2\text{K}</math>. The exit temperature is not to exceed <math>80^{\circ}\text{C}</math>. Using effectiveness-NTU method, find</p> <ol style="list-style-type: none"> <li>Mass flow rate of water</li> <li>Effectiveness of heat exchanger</li> <li>Surface area required.</li> </ol> <p>2. Write short note on Temperature Cross.</p>	15+5

Ex/Che/PC/B/T/314/2023(S)

**B.E. CHEMICAL ENGINEERING SUPPLEMENTARY EXAM – 2023**3<sup>rd</sup> Year, 1<sup>st</sup> Semester**PROCESS HEAT TRANSFER**Use Separate Answer Scripts for Part I and Part II**PART II ( 50 Marks)**

Time: 3 Hours (Maximum)

Full Marks: 100

Answer Q1, Q2 and Q3 OR Q4**Q1. Natural Convection****[8+12=20]**

- Define: *Rayleigh Number* and *Grashof Number*. What are the physical significances of each of them?
- Derive the dimensionless equation for the heat transfer coefficient for natural convection in a horizontal pipe. The controlling physical variables, given below, are to be represented in terms of the fundamental dimensions length (L), mass (M), temperature (T), and time ( $\theta$ ). Use Buckingham's pi theorem.

$$h = f(\rho, L, v, \mu, C_p, k)$$

L: Length of the Pipe;  $\mu$ : Absolute viscosity;  $v$ : Velocity;  $C_p$ : Specific heat;  $k$ : Thermal conductivity;  $h$ : Heat transfer coefficient;  $\rho$ : Density.

**Q2. Condensation and Boiling****[7+7+3+3=20]**

- State two differences between dropwise and film-wise condensation. Which one is greatly influenced by the presence of non-condensable gases? Explain briefly.
- Draw a Pool Boiling Curve. Explain with the help of the pool boiling curve: a) Leiden Frost Point and b) Critical Heat Flux.
- Write a short note on the effectiveness of nucleate boiling.
- What are the factors on which the heat transfer coefficient of nucleate boiling depends ?

**Q3. Radiation****[10]**

Consider a copper kettle that has a flat bottom with a 0.254 m diameter. Water is boiled at a rate of 22.68 kg/hr at atmospheric pressure. Find the burning out heat flux for nucleate boiling.

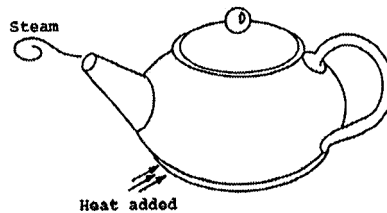


Fig. 1

Assume that the heat transfer from the surface of the kettle to the surrounding liquid takes place purely by convection until the temperature of the kettle surface is a few degrees above the boiling temperature of the liquid (pool boiling). Also, assume that steady-state conditions prevail in the system. From steam tables, at atmospheric pressure:  $T_{\text{sat}} = 100^\circ\text{C}$ .  $h_{fg} = 2256 \text{ kJ/kg}$ ;  $\sigma = 0.00006 \text{ kN/m}$ ;  $\rho_l = 961.1 \text{ kg/m}^3$ ;  $\rho_v = 0.61 \text{ kg/m}^3$ .

**Q4. Evaporation****[6+4=10]**

- Sketch the diagram of Forward Feed arrangement of a Triple-Effect evaporator.
- Why do you think it is less energy efficient in comparison to Backward Feed evaporator.  
[Qualitative answer expected]