Ex/MET/T/314/2017(S)

## Bachelor of Metallurgical Engineering 3rd Year 1st Semester Examination, 2017 (Supplementary)

## Chemical Kinetics and Mass Transfer

Time: Three Hours

Full Marks-100

## Answer any Five questions.

1. i) The rate of a 2nd-order reaction is given as

$$r_A = 4 C_A^2$$
, mol/liter.hr

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What is the value and unit of the rate constant? If the rate is expressed in mol/cm<sup>3</sup>.sec and concentration in mol/cm<sup>3</sup>, how will the value and unit of the rate constant change?

ii) The total pressure in a closed reactor in which pure AB fed at 1 atm undergoes the 2nd-order irreversible reaction

$$\begin{array}{c}
k \\
2AB \longrightarrow A_2B_2
\end{array}$$

decreases to 0.8 atm in 5 mintes at 500 K. Determine k.

- After 8 minutes in a batch reactor, reactant ( $C_{A0} = 1 \text{ mol/liter}$ ) is 80% converted; after 18 minutes, conversion is 90%. Find a rate equation representing this reaction. (Note, A trial and error solution may be necessary.)
- 2. i) Consider a gas phase reaction  $2A + B \rightarrow A_2B$  which takes place according to the following 2-step mechanism:

i. 
$$A + B \stackrel{k_1}{\rightleftharpoons} AB^*$$

ii. 
$$AB^* + A \rightarrow A_2B$$

If the initial concentrations are  $C_{A0} = 10 \text{ mol/m}^3$  and  $C_{B0} = 5 \text{ mol/m}^3$ , find the value of  $C_{A2B}$  at t = 30 sec, when the reaction is carried out in a constant-volume batch reactor at temperature T. Given,  $k_1 = 0.02 \text{ m}^3/\text{mol.sec}$ ,  $k_2 = 3 \text{ sec}^{-1}$  and  $k_3 = 6 \text{ m}^3/\text{mol.sec}$ .

ii) Establish the following design equations for a steady-state mixed flow reactor:

$$\frac{V}{F_{40}} = \frac{\tau}{C_{40}} = \frac{X_A}{-r_A} \,.$$

3. i) Consider the following 2nd-order homogeneous reaction:

$$k$$
A+B  $\longrightarrow$  AB

Using the following data, determine the activation energy (E) of the reaction.

<i>T</i> , K	$C_A$ , mol/lit	$C_{\rm B}$ , mol/lit	$-dC_A/dt$ , mol/lit.min
1000	5	3	0.3
1500	5	2	1.0

ii) Consider the evaporation of liquid Zn taken in a rectangular tube into the stagnant film of argon formed by pure argon flowing over the tube at 764  $^{0}$ C and 1 atm. Given, the saturated vapor pressure of liquid Zn at 764  $^{0}$ C is 0.5 atm,  $Z_{2}$ -  $Z_{1}$  = 0.02 m, and  $D_{Zn-Ar}$  (at 764  $^{0}$ C) = 1.43 × 10<sup>-4</sup> m<sup>2</sup>/s. Find

a) 
$$J_{Ar(-Z), Z1}^*$$
  
b)  $V_{Zn, Z, Z1}$ 

4. Consider the reduction of a dense cylindrical FeO sample (L>>r)) with a flowing mixture of CO-CO<sub>2</sub> mixture, which is controlled by 1-dimensional pore diffusion in the r-direction though the product (Fe) layer. The reduction reaction is

$$FeO(s) + CO(g) = Fe(s) + CO_2(g)$$
.

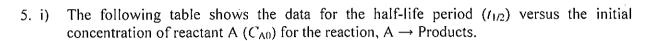
i) Show that the molar rate of reduction of FeO,  $-dn_{FeO}/dt$ , can be expressed as follows:

$$-dn_{\text{FeO}}/dt = -\frac{2\pi L(C_{\text{CO,b}} - C_{\text{CO,e}})D_{\text{pore}}}{\ln(r^{0}_{\text{FeO}}/r_{\text{FeO}})},$$

where  $r^0_{\text{FeO}}$  is the initial radius of the cylinder having the length L.

ii) Show that the progress of the reduction can be expressed as

$$X_{\text{FeO}} + (1 - X_{\text{FeO}}) \ln (1 - X_{\text{FeO}}) = \frac{4D_{\text{pore}} (C_{\text{CO,b}} - C_{\text{CO,e}})t}{\rho_{\text{m,FeO}} (r^0_{\text{FeO}})^2}.$$



Find the order of the reaction.

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Refer to the problem of dissolution of a flat plate (A) in a flowing fluid (B). If the local Sherwood Number at x = 0.5 m is 1000 and  $D_{AB} = 1.2 \times 10^{-8}$  m<sup>2</sup>/s, determine the steady rate of dissolution  $W_{A_1}$  (mole/time) of the plate. Given,

$$L = 1 \text{ m}$$
  $W \text{ (width of the plate)} = 0.3 \text{ m}$   
 $C_{As} = 40 \text{mol/m}^3$   $C_{Av} = 0$ .

iii) Considering the following 1st-order reversible reaction

$$A \rightleftharpoons_{k_b} B, M = C_{B0} / C_{A0},$$

derive the rate equation

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$$C_A$$
 -  $C_{Ae}$   
-In (-----) = At , where A = f( $k_f$ ,  $C_{A0}$ ,  $M$ ,  $C_{Ae}$ ).  
 $C_{A0}$  -  $C_{Ae}$ 

- 6. i) Give the two basic postulates, one thermodynamic and the other kinetic, of the activated complex theory.
  - ii) Give one metallurgical example for
    - (a) series reactions
    - (b) parallel reactions

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- iii) Give an example in which the term "order" does not apply in the rate equation of the reaction.
- iv) Superimpose the ln k vs 1/T plots for the two reactions,  $P \rightarrow Q$  and  $M \rightarrow N$ , for each of the following two cases:

(a) 
$$A_{P \to Q} = A_{M \to N}$$
,  $E_{P \to Q} < E_{M \to N}$ 

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(b) 
$$E_{P\rightarrow Q} = E_{M\rightarrow N}$$
,  $A_{P\rightarrow Q} < A_{M\rightarrow N}$ 

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v) Consider the half-order nonelementary homogeneous reaction

$$k$$
 $A \rightarrow B$ .

Find its integrated form of rate equation  $(X_A \text{ vs } t)$ . Explain with the help of a suitable plot how you will find out the rate constant k.

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