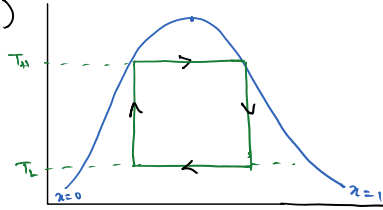


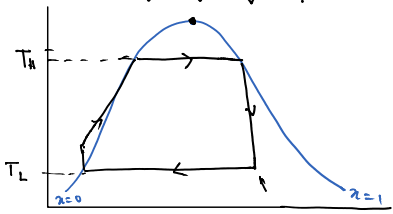
Vapor power cycles

Carnot Cycle

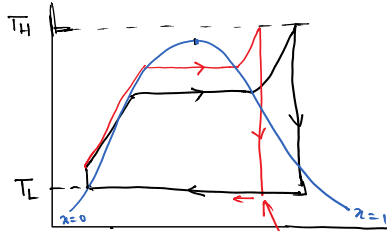
All cycles are Internally Reversible  
(No friction, unresisted expansion, Joule heating, etc.)



Rankine Cycle



Rankine Cycle with Superheat

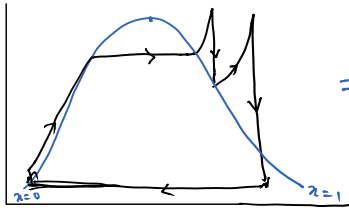


Better  $\eta_a$ , SSC  
Poorer  $2$ ,  $2_{II}$

with increasing  $P_{boiler}$ ,  $\eta \uparrow$  but

$x @ \text{Turbine ext} \downarrow$   
 $\Rightarrow$  Turbine blade erosion

Reheat Cycle

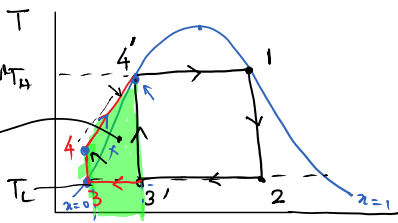


$\Rightarrow$  Better specific work output (swot)  
(lower SSC,  $\therefore SSC = \frac{1}{z_{net}}$ )

$\eta$  may  $\uparrow$  or  $\downarrow$ , depending on  $P_{brt}$ .

@  $P_{reheat} \approx 0.25 P_b$ ,  $\eta$  is max.

Regenerative Feed Heating



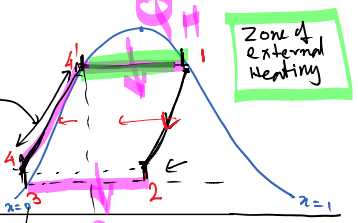
We do regenerative feed heating to minimize the subcooled heating regime, thus improving  $\bar{T}_H$

$\eta_R < \eta_c$

$\eta \approx 1 - \frac{\bar{T}_L}{\bar{T}_H}$

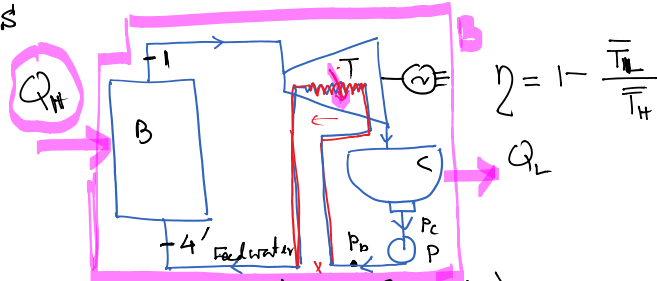
Carnot cycle  $\bar{T}_H = T_H$   
4-4' subcooled liquid heating  
 $\hookrightarrow$  done at  $< T_H$

Heat is added only from another part of the cycle which is within the system boundary



$\dot{Q}_L = \dot{m}(h_{4'} - h_4)$

$\eta = 1 - \frac{\bar{T}_L}{\bar{T}_H}$



$\frac{dE}{dt} = \dot{Q} - \dot{W} + \dot{m}(h_i - h_e)$   
 $\frac{dS}{dt} = \int \dot{Q}/T_b + \dot{S}_{gen} + \dot{m}(s_i - s_e)$   
 $\therefore \dots (h_i - h_e) - \dot{Q}$  (if  $\dot{Q} = -\dot{Q}$ )

$$m \cdot \dot{Q}_L = m(h_4' - h_4)$$

$$\eta = 1 - \frac{\bar{T}_L}{\bar{T}_H}$$

$$= 1 - \frac{T_L}{T_H}$$

Regenerative Heating

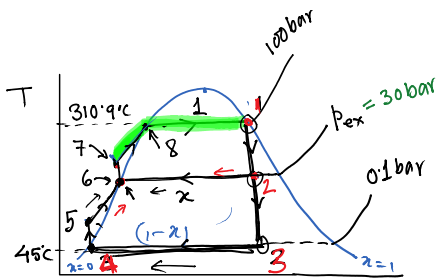
- reduces work output
- reduces heat input
- improves the  $\bar{T}_H \Rightarrow \eta \uparrow$

Practical Difficulty of the above schematic:



$$F = \rho A u = \rho \frac{du}{dy} \cdot A$$

- i) Turbine cannot work well as a heat exchanger
- ii) LPT wetness problem



Per kg of steam generated from boiler,

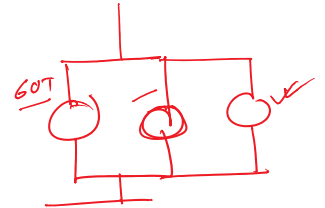
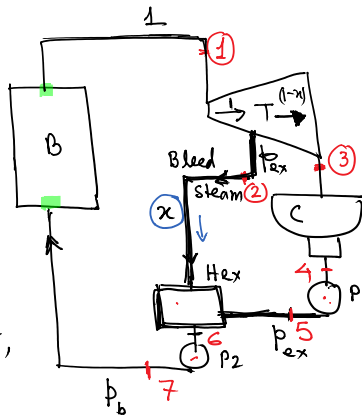
$$w_T = (h_1 - h_2) + (1-x)(h_2 - h_3)$$

$$w_p = (1-x)(h_5 - h_4) + x(h_7 - h_6)$$

$\approx v_4(p_{ex} - p_c)$        $\approx v_6(p_b - p_{ex})$

$$q_H = (h_1 - h_7)$$

$$\eta = \frac{w_T - w_p}{q_H}$$



For Rankine, R/H & Reg. cycle s, the pump work is often neglected.

We need to know

$$h_1 = 2730 \text{ kJ/kg}$$

$$h_2 = 2420 \text{ "}$$

$$h_3 = 1780 \text{ "}$$

$$h_4 = 192 \text{ kJ/kg}$$

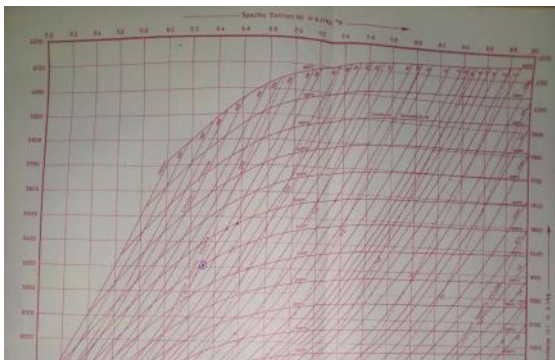
$$h_5 = h_4 + v_4(p_{ex} - p_c) = 200 \text{ kJ/kg}$$

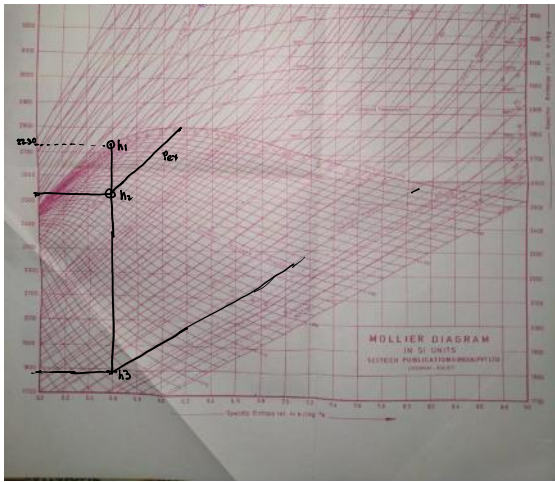
$$h_6 = h_f \text{ at } p_{ex} = 1008.2 \text{ kJ/kg}$$

$$h_7 = h_6 + v_6(p_b - p_{ex}) \approx 1005 \text{ kJ/kg}$$

$$x = \frac{(h_6 - h_5)}{(h_2 - h_5)} = \frac{(1008.2 - 200)}{(2420 - 200)} = 0.3640$$

$$h_4 = h_f @ 0.1 \text{ bar}$$

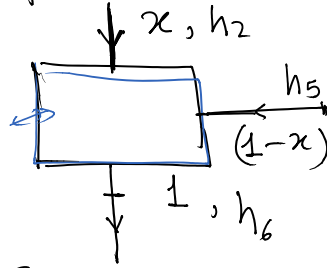




$$h_7 = h_6 + v_6 \times (P_6 - P_{ex}) \approx 1005 \text{ kJ/kg}$$

$$x = (h_6 - h_5) / (h_2 - h_5) = (1008.2 - 200) / (2420 - 200) = 0.3640$$

1st Law for the feedwater heater



SFEE  $\Rightarrow$

$$\frac{dE}{dt} = \dot{Q} - \dot{W} + \sum m_i h_i - \sum m_e h_e$$

$$x h_2 + (1-x) h_5 = h_6$$

$$\Rightarrow x = \frac{(h_6 - h_5)}{(h_2 - h_5)} = 0.364$$

$$w_T = (h_1 - h_2) + (1-x)(h_2 - h_3)$$

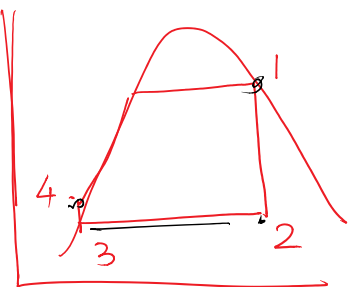
$$= (2730 - 2420) + (1 - 0.364)(2420 - 1780) = 717 \text{ kJ/kg}$$

$$w_p = 13 \text{ kJ/kg}, \quad w_{\text{net}} = 704 \text{ kJ/kg} \leftarrow$$

$$q_{\text{in}} = (h_1 - h_7) = (2730 - 1005) = 1725 \text{ kJ/kg}$$

$$\eta = 40.811 \%$$

Higher than the corresponding Rankine cycle



What was the corresponding Rankine cycle

$$h_1 = 2730 \text{ kJ/kg}$$

$$h_2 = 1780 \text{ "}$$

$$h_3 = 191 \text{ "}$$

$$h_4 = 201 \text{ "}$$

$$q_{\text{in}} = 2539 \text{ kJ/kg}$$

$$w_T - w_p = 940 \text{ kJ/kg} \uparrow$$

$$\eta = 1 - \frac{q_L}{q_{\text{in}}} = 1 - \frac{(h_2 - h_3)}{h_1 - h_4} = 1 - \frac{1780 - 191}{2730 - 191}$$

$$\eta = 1 - \frac{q_L}{q_H} = 1 - \frac{h_1 - h_4}{h_1 - h_4} = 1 \quad 2730 - 191$$

$$= 1 - \frac{1589}{?} = 37.4 \%$$

500 MW,  $\Rightarrow$  8760 hrs, 1%  $\Delta\eta$ ,

Coal  $\Rightarrow$  CV = 12000 kJ/kg,  $R_s = 2$ /kg.

Calculate the financial impact of 1%  $\Delta\eta$  about a base value of 40%.

### Effects of Regeneration

- 1)  $\eta$  increases ( $\rightarrow \bar{T}_H \uparrow$ ,  $\bar{T}_L$  remains same)
- 2)  $W_{net}$  decreases, SSE increases  
 $\Rightarrow$  For the same plant capacity (MW)  
 we need to circulate more steam  
 $\Rightarrow$  Boiler should be bigger,
- 3)  $q_H$  decreases
- 4) Condenser heat rejection decreases

In a practical Regenerative cycle