

Example 1:

For flow of a liquid metal through a circular tube, the velocity and temperature profiles at a particular axial location may be approximated as being uniform and parabolic, respectively. That is, $u(r) = C_1$ and $T(r) - T_s = C_2[1 - (r/r_o)^2]$, where C_1 and C_2 are constants. What is the value of the Nusselt number Nu_D at this location?

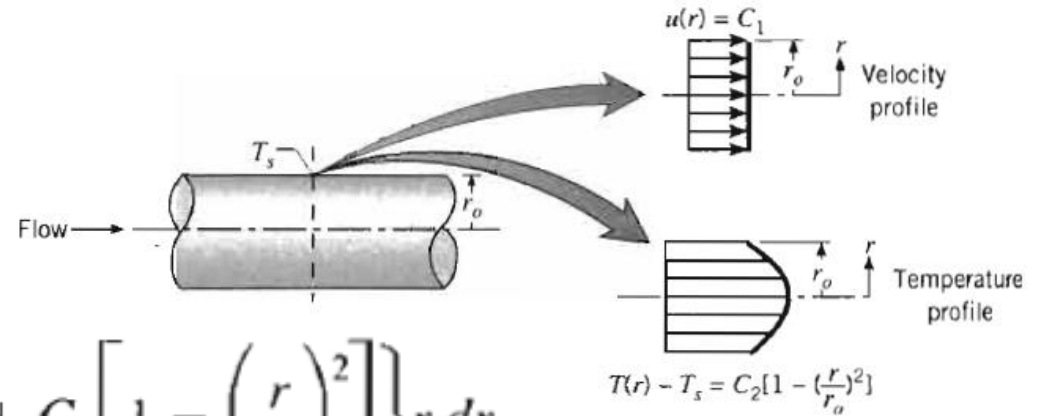
- Heat Transfer Coefficient: $h = \frac{q_s''}{(T_m - T_s)}$
- Average velocity: $u_m = \frac{2}{r_o^2} \int_0^{r_o} r u(r) dr = C_1$
- Bulk Mean Temperature:

$$T_m = \frac{2}{u_m r_o^2} \int_0^{r_o} u T r dr = \frac{2C_1}{u_m r_o^2} \int_0^{r_o} \left\{ T_s + C_2 \left[1 - \left(\frac{r}{r_o} \right)^2 \right] \right\} r dr$$

$$T_m = \frac{2}{r_o^2} \int_0^{r_o} \left\{ T_s + C_2 \left[1 - \left(\frac{r}{r_o} \right)^2 \right] \right\} r dr = \frac{2}{r_o^2} \left(T_s \frac{r_o^2}{2} + \frac{C_2}{2} r_o^2 - \frac{C_2}{4} r_o^2 \right) = T_s + \frac{C_2}{2}$$

- Wall Heat flux: $q_s'' = -k \frac{\partial T}{\partial r} \Big|_{r=r_o} = -k C_2 2 \frac{-r}{r_o^2} \Big|_{r=r_o} = 2C_2 \frac{k}{r_o}$

$$h = \frac{q_s''}{(T_m - T_s)} = \frac{2C_2 (k/r_o)}{C_2/2} = \frac{4k}{r_o}$$



$$\rightarrow Nu_D = \frac{hD}{k} = \frac{(4k/r_o) \times 2r_o}{k} = 8$$