

# Digital Controllers

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# Digital Controller in a Process Control Loop

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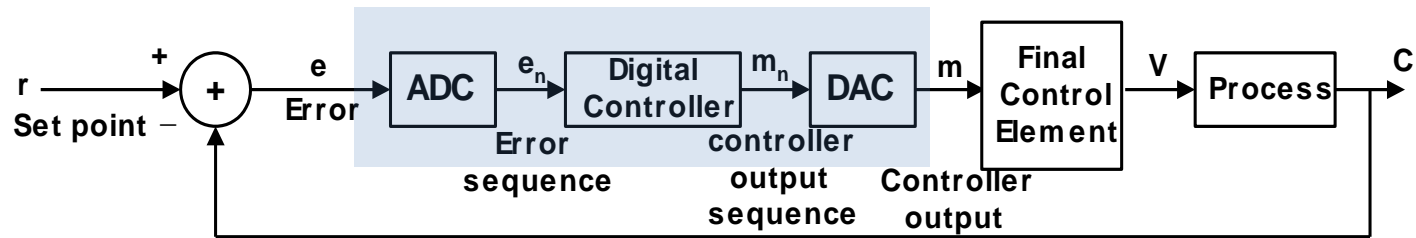
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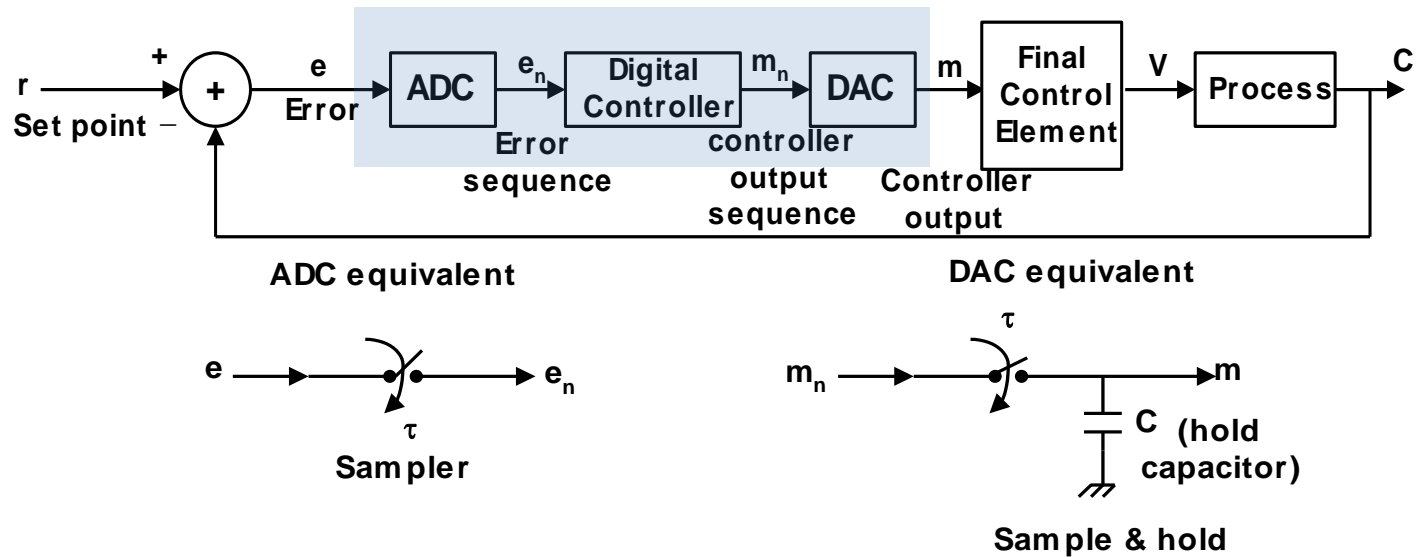
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**In a processor based digital controller, rapid switching from one algorithm to another (*e.g. a P controller to a PID controller*) and automatic tuning of controller parameters are possible.**

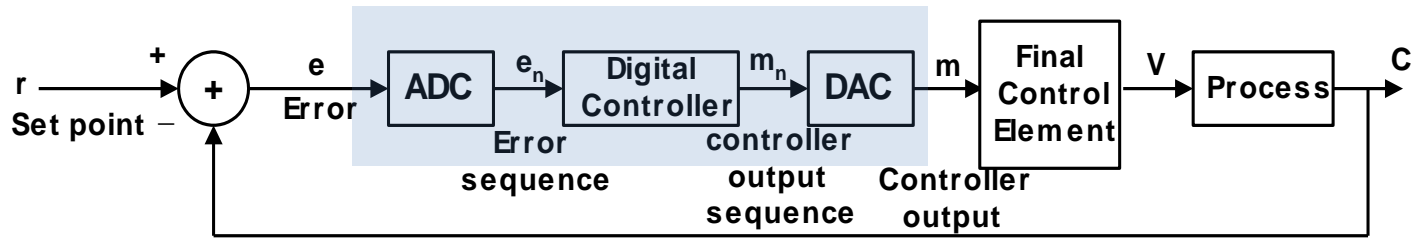
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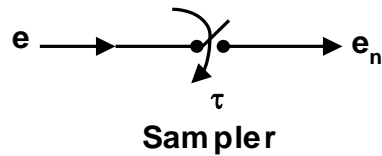


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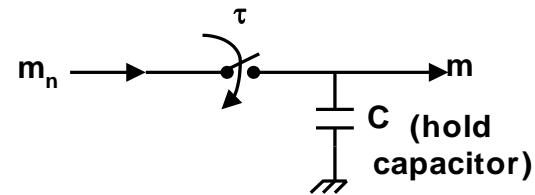


ADC equivalent

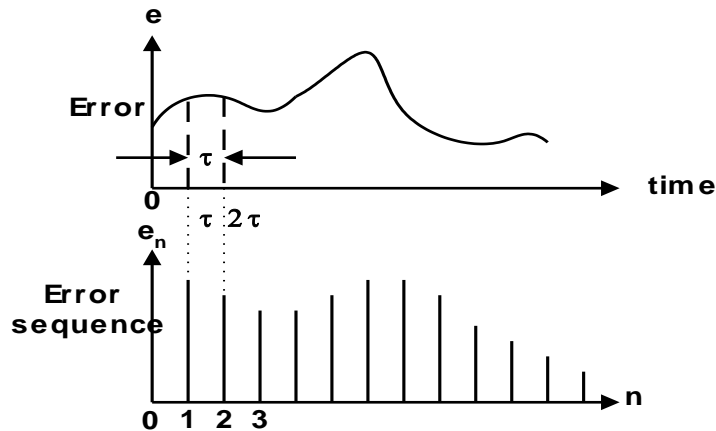
DAC equivalent



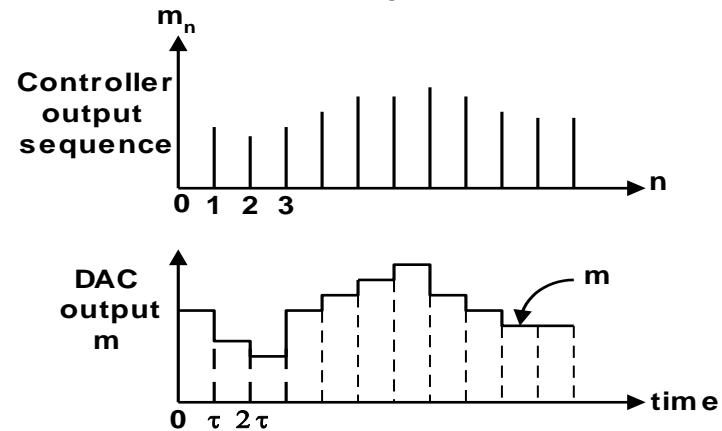
Sampler



Sample & hold



$\tau \rightarrow$  Sampling interval



$\tau \geq$  (ADC conversion time + computation time)

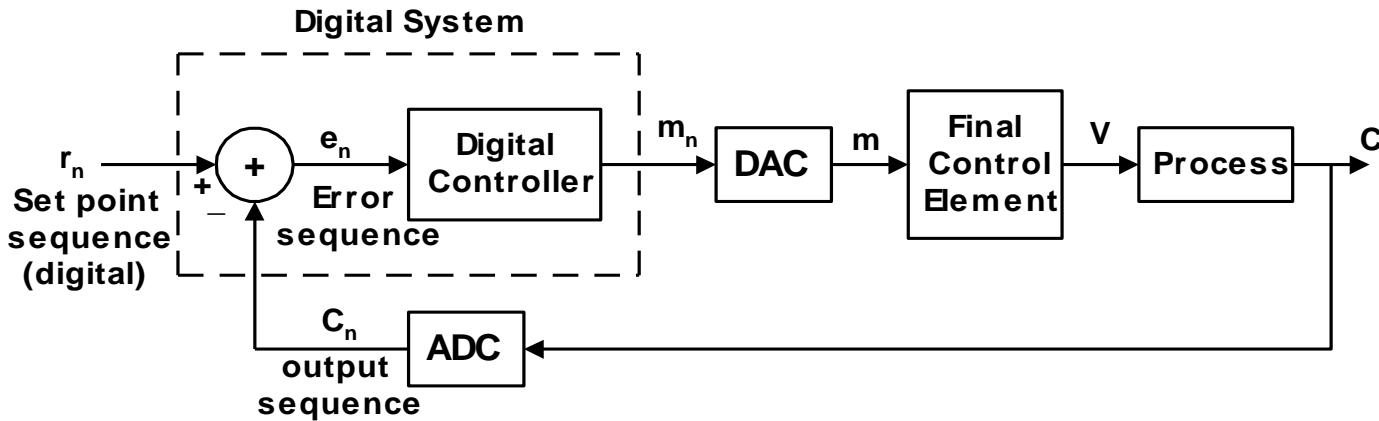


## Digital Controller in a Process Control Loop

**The error computation may be performed digitally if the set-point is available in digital form (say, from digital keyboard) and the measured variable is digitized with the ADC.**

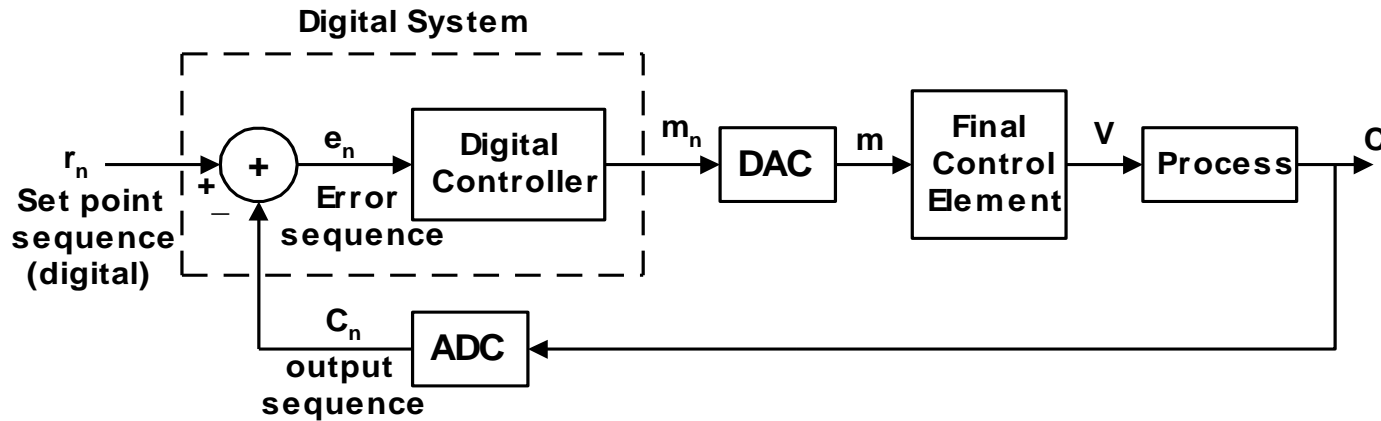
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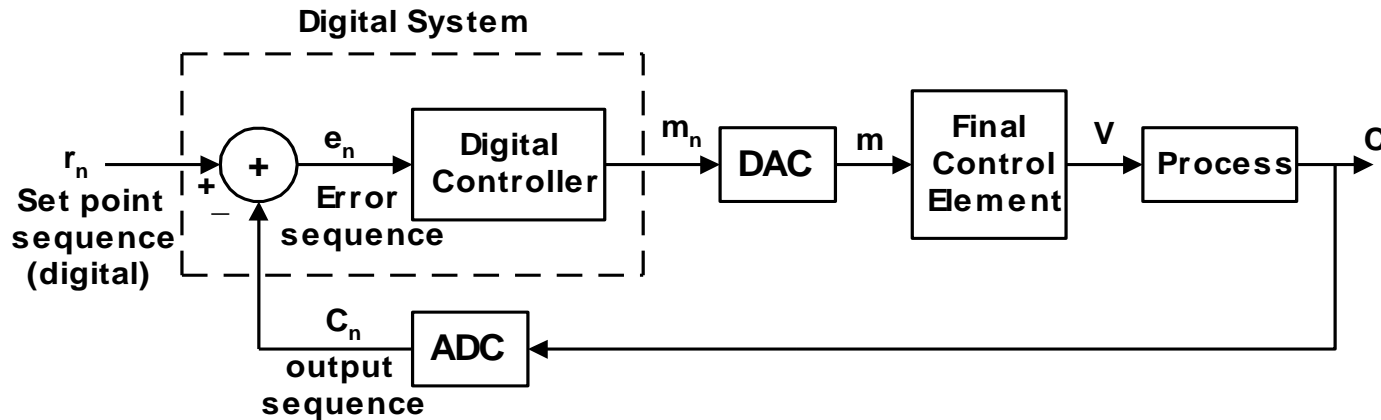
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Proper selection of the **sampling interval** ' $\tau$ ' is necessary for satisfactory operation of the process control loop.

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Proper selection of the **sampling interval** ' $\tau$ ' is necessary for satisfactory operation of the process control loop.

A large ' $\tau$ ' may lead to **unstable operation** of the loop (because of the extra lag introduced in the loop), whereas a very small ' $\tau$ ' requires a **high speed digital hardware** (hence high cost) to implement the controller.

# Realization of Digital Controllers (through discrete approximation of analog controllers)

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$$m_n = K_p e_n + b_n = m'_n + b_n$$

where,  $K_p$  = proportional gain,  
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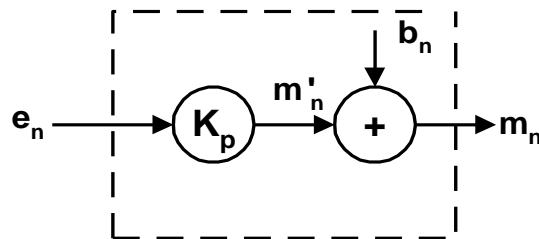
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**Realization of the P controller:**





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## Proportional-Integral (PI) Controller

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Then,  $I_n = I_{n-1} + \int_{(n-1)\tau}^{n\tau} e \cdot dt$

## PI Controller

$$I_n = I_{n-1} + \int_{(n-1)\tau}^{n\tau} e \cdot dt$$

The second term of the above relation represents the area under the curve 'e' for  $(n - 1)\tau \leq t \leq n\tau$ .

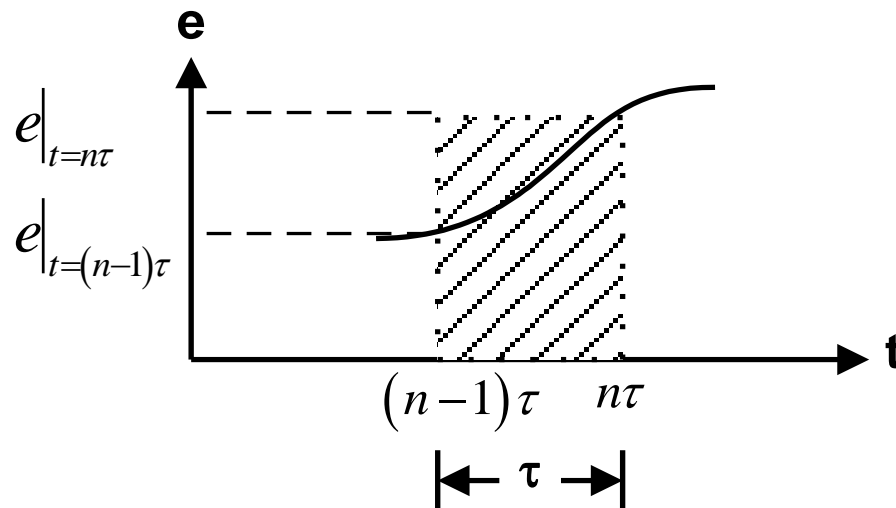


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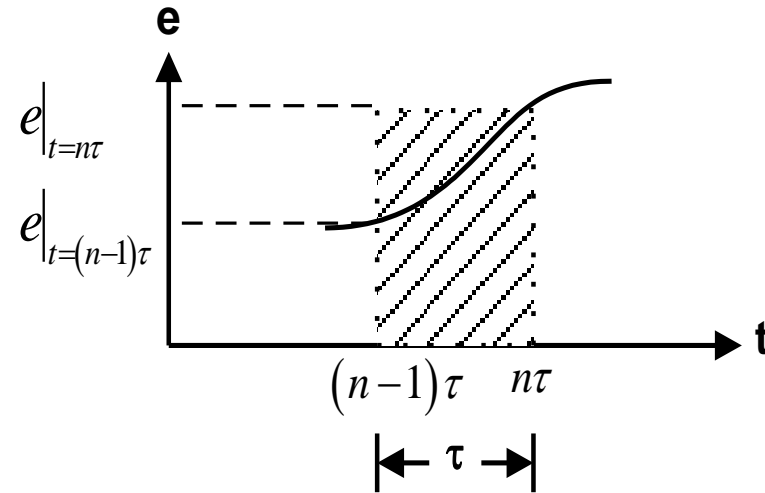
The second term of the above relation represents the area under the curve 'e' for  $(n-1)\tau \leq t \leq n\tau$ .

This area may be approximated by the shaded rectangle (called the **method of rectangular integration**) as



## PI Controller

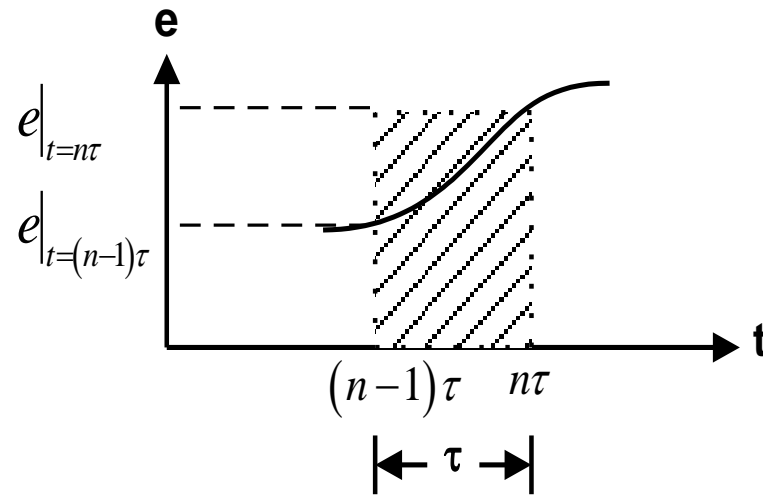
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Thus, 
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Using the notation  $e_n$  for  $e \Big|_{t=n\tau}$ ,  $I_n = I_{n-1} + \tau e_n$

## PI Controller

Now, output  $m'$  at the  $n$ th instant may be expressed as

$$m'_n = K_p \left[ e_n + \frac{I_n}{T_i} \right] \quad \text{where} \quad I_n = I_{n-1} + \tau e_n$$

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$$m'_{n-1} = K_p \left[ e_{n-1} + \frac{I_{n-1}}{T_i} \right]$$

The difference between these two outputs is

$$m'_n - m'_{n-1} = K_p \left[ e_n - e_{n-1} + \frac{1}{T_i} (I_n - I_{n-1}) \right]$$

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Substituting the value of  $(I_n - I_{n-1})$  for rectangular integration,  $[(I_n - I_{n-1}) = \tau e_n]$

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or, 
$$m'_n = e_n K_p \left( 1 + \frac{\tau}{T_i} \right) - K_p e_{n-1} + m'_{n-1}$$

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$$= a_0 e_n + a_1 e_{n-1} + m'_{n-1}, \quad \text{say}$$

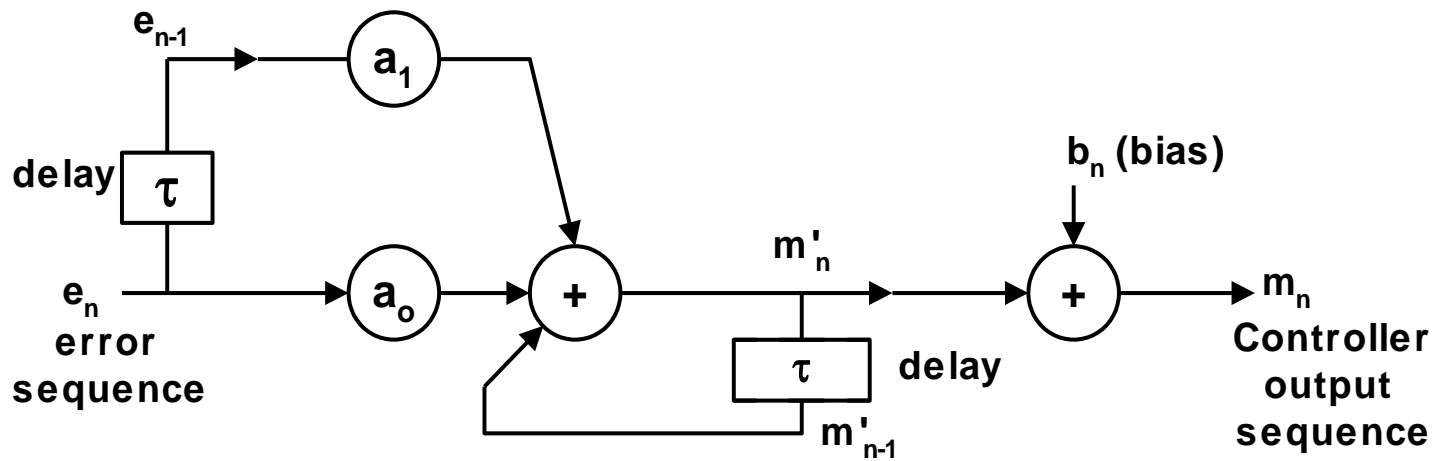
where, 
$$a_0 = K_p \left[ 1 + \frac{\tau}{T_i} \right] \quad \text{and} \quad a_1 = -K_p$$

## Realization of the PI Controller

Controller output at the nth instant:

$$m_n = m'_n + b_n$$

$$m'_n = a_0 e_n + a_1 e_{n-1} + m'_{n-1}$$

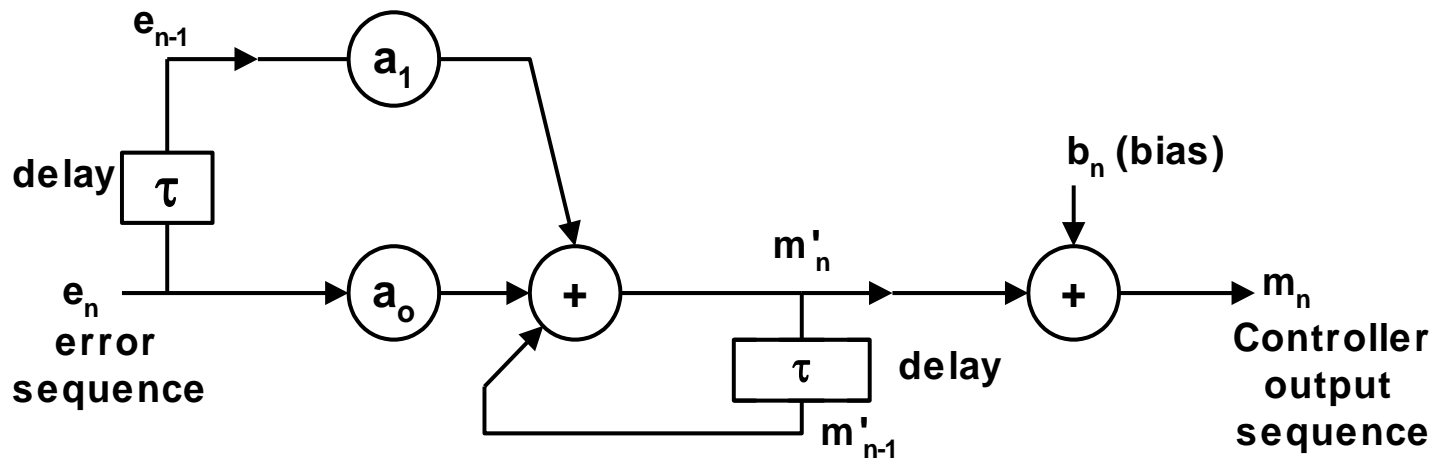


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**Problem:** Develop a digital PI Controller using Trapezoidal rule for integration.

## Velocity or incremental form of PI controller

The controller output is proportional to the derivative of a standard PI controller and it may be expressed as (without bias):

$$\Delta m_n = m_n - m_{n-1} = m'_n - m'_{n-1} = a_0 e_n + a_1 e_{n-1}$$

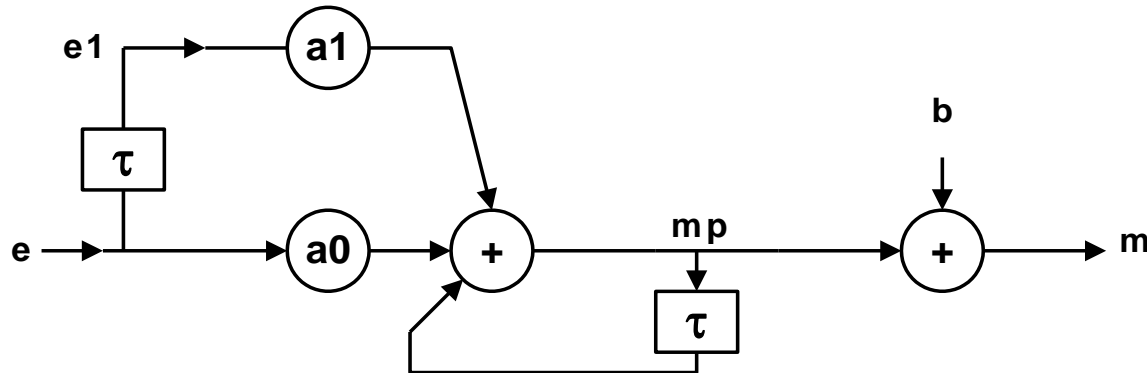
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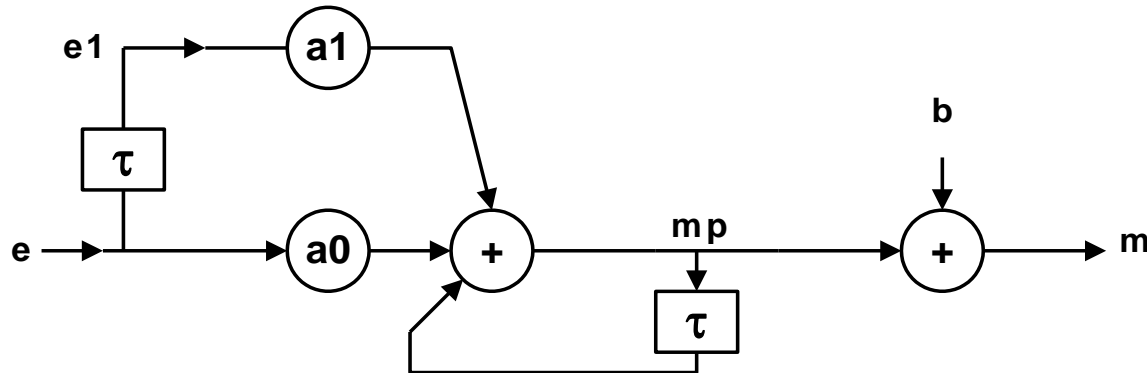
**Velocity form of controller is useful when the actuator is some kind of adder (integral action), like a stepping motor.**

## Software Realization of the PI Controller



```
# include < studio.h>
void main (void)
{
    float e = 0, e1, m, mp = 0;
    float a0, a1, b;
    float adc (void) ;    // digitized error
    void dac (float m ) ; // analog output
    a0 = ----- ; // Kp [1 + τ/Ti]
    a1 = ----- ; // -Kp
    b = ----- ; // bias
```

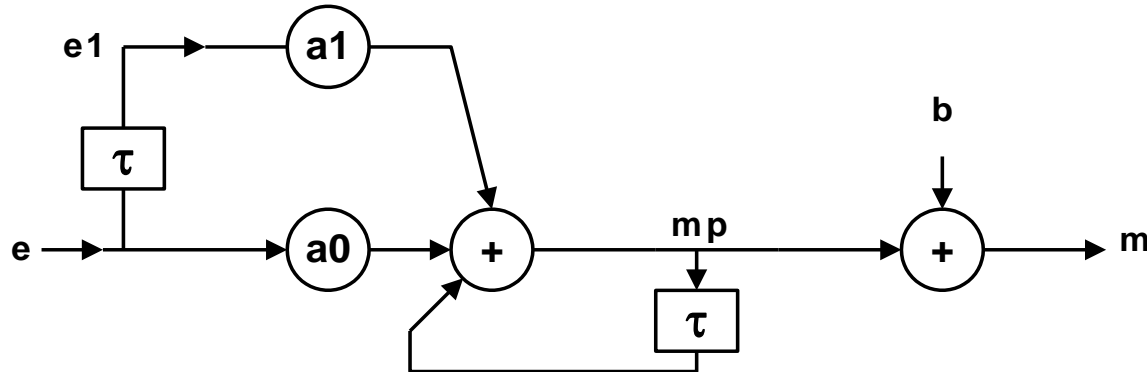
## Software Realization of the PI Controller



```
for (;;) // continuous loop
{ // loop time is the sampling interval  $\tau$ 
  e1 = e;
  e = adc ();
  mp = mp + a0*e + a1*e1;
  m = mp + b;
  // provision for saturation
  if (m < 0) m = 0;
  if (m > 100) m = 100;
  dac (m);
}
}
```



## Software Realization of the PI Controller



```
float adc (void) // Analog-to-digital conversion
{
    float v;
    scanf ("%f", &v); // for (keyboard) simulation
    return v; // (to be replaced for actual
} // realization)
```

```
void dac (float m) // Digital-to-analog conversion
{
    printf ("%f\n", m); // for (VDU) simulation
} // (to be replaced for actual realization)
```

# Realization of Digital Controllers (through discrete approximation of analog controllers)

## Proportional-Derivative (PD) Controller

The analog controller output is

$$m = K_p \left[ e + T_d \frac{de}{dt} \right] + b \quad \text{where } T_d \text{ is the derivative time.}$$

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$D_n$  may be approximated using the **backward difference algorithm** as

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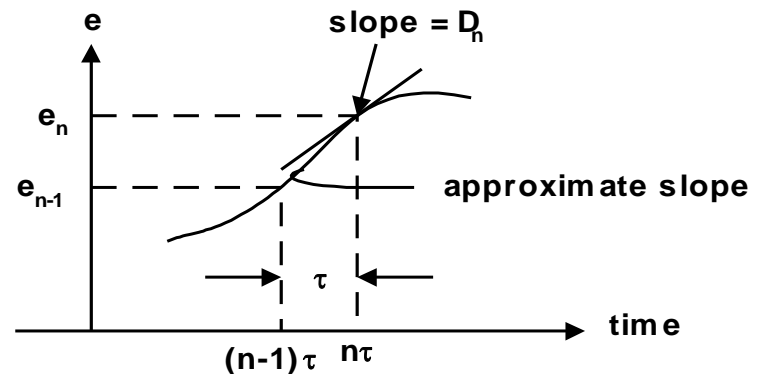
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## PD Controller

Thus the controller output at the nth instant is

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## PD Controller

Thus the controller output at the nth instant is

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$$\text{or } m_n = K_p \left[ 1 + \frac{T_d}{\tau} \right] e_n - \left[ \frac{K_p T_d}{\tau} \right] e_{n-1} + b_n$$

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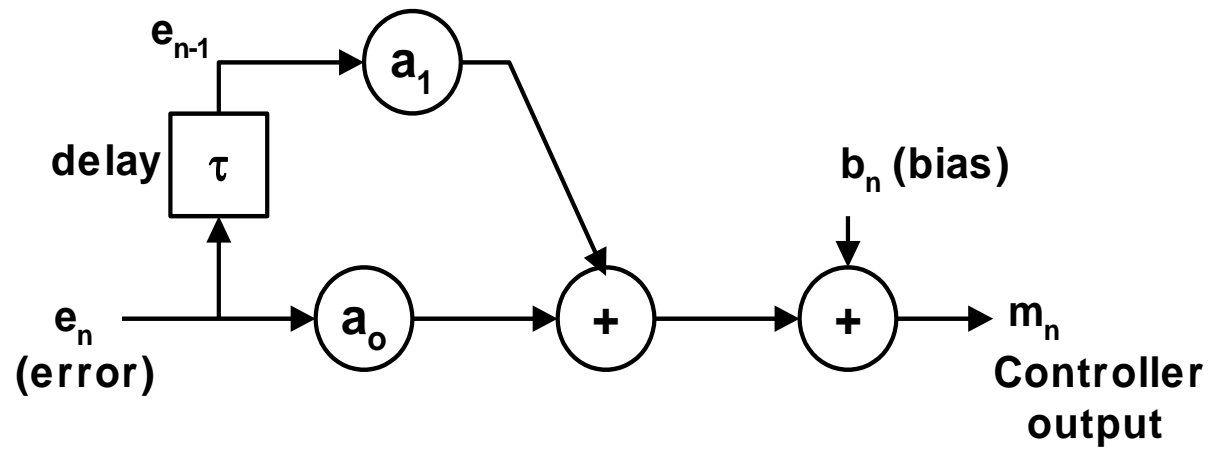
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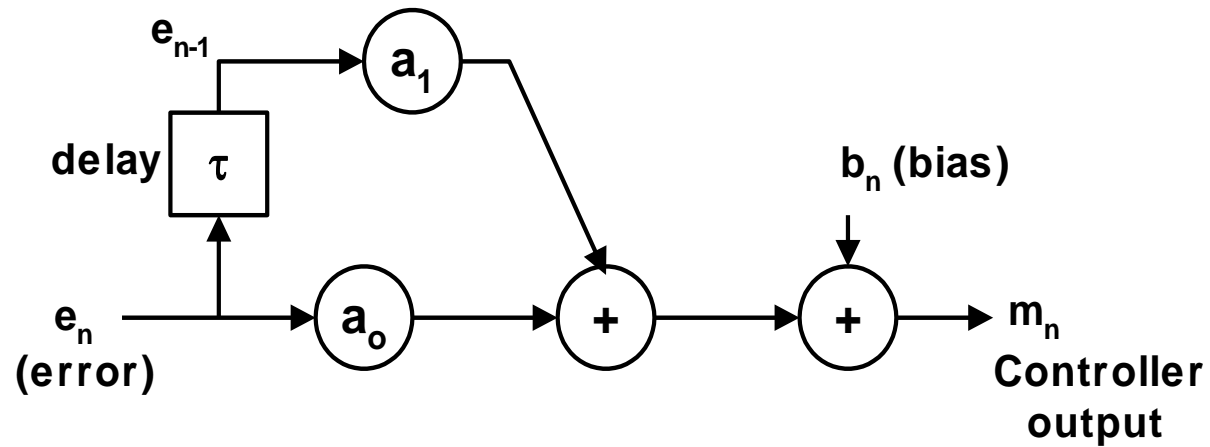
$$\text{where } a_o = K_p \left( 1 + \frac{T_d}{\tau} \right) \quad \text{and} \quad a_1 = -\frac{K_p T_d}{\tau}$$



## Realization of the PD Controller



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**Problem:** Develop a 'c' program for software realization of the PD Controller.

# PD Controller

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To avoid derivative action from a sudden change in set-point, the derivative action is generally derived from the measured output.

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Thus, the controller output may be expressed as,

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## PD Controller

### Provision for anti-derivative kick

$$m = K_p \left( e - T_d \frac{dc}{dt} \right) + b$$

using **backward difference** algorithm, the controller output at the nth instant is

$$m_n = K_p \left[ e_n - T_d \left( \frac{c_n - c_{n-1}}{\tau} \right) \right] + b_n$$



## PD Controller

### Provision for anti-derivative kick

$$m = K_p \left( e - T_d \frac{dc}{dt} \right) + b$$

using **backward difference** algorithm, the controller output at the nth instant is

$$m_n = K_p \left[ e_n - T_d \left( \frac{c_n - c_{n-1}}{\tau} \right) \right] + b_n$$

$$\text{or } m_n = K_p e_n - \frac{K_p T_d}{\tau} c_n + \frac{K_p T_d}{\tau} c_{n-1} + b_n$$

## PD Controller

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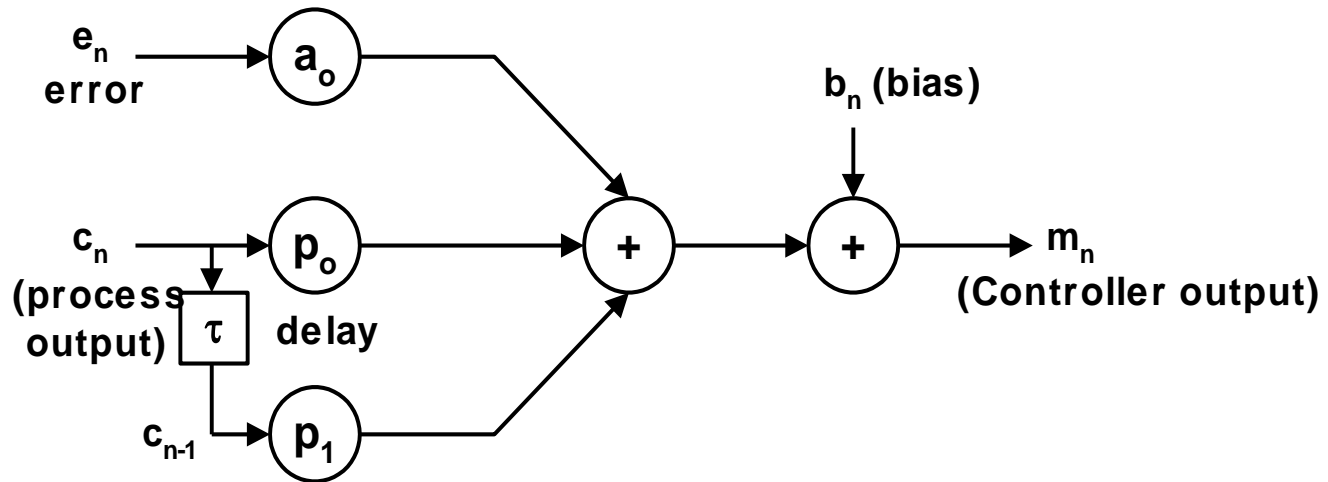
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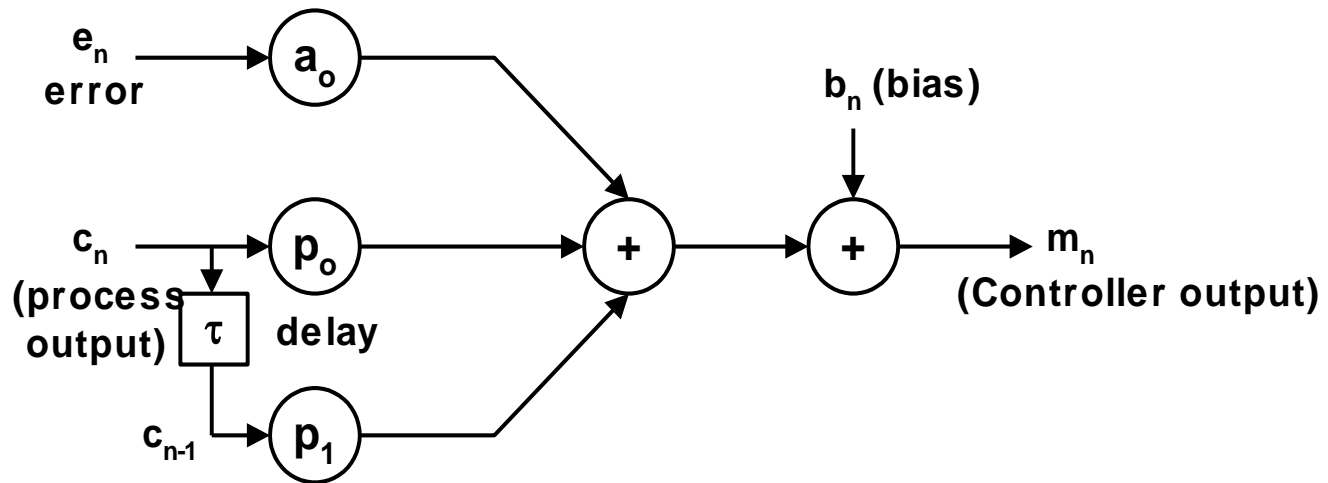
$$\begin{aligned} \text{or } m_n &= K_p e_n - \frac{K_p T_d}{\tau} c_n + \frac{K_p T_d}{\tau} c_{n-1} + b_n \\ &= a_o e_n + p_o c_n + p_1 c_{n-1} + b_n \quad \text{where} \end{aligned}$$

$$\begin{aligned} a_o &= K_p \\ p_o &= -\frac{K_p T_d}{\tau} \\ p_1 &= \frac{K_p T_d}{\tau} = -p_o \end{aligned}$$

## Realization of PD Controller with anti-derivative kick



## Realization of PD Controller with anti-derivative kick



**Problem:** Develop a 'c' program for software realization of the PD Controller with anti-derivative kick

# Realization of Digital Controllers (through discrete approximation of analog controllers)

## Proportional-Integral-Derivative (PID) Controller

The analog controller output is

$$m = K_p \left[ e + \frac{1}{T_i} \int_0^t e dt + T_d \frac{de}{dt} \right] + b$$
$$= m' + b \quad (\text{say})$$

where  $m' = K_p \left[ e + \frac{1}{T_i} \int_0^t e dt + T_d \frac{de}{dt} \right]$

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The controller output (without bias) at the  $n$ th instant, using backward difference algorithm, is

$$m'_n = K_p \left[ e_n + \frac{I_n}{T_i} + T_d \left( \frac{e_n - e_{n-1}}{\tau} \right) \right]$$

## PID Controller

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The controller output at the (n-1)th instant is

$$m'_{n-1} = K_p \left[ e_{n-1} + \frac{I_{n-1}}{T_i} + T_d \left( \frac{e_{n-1} - e_{n-2}}{\tau} \right) \right]$$

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Subtracting,

$$m'_n - m'_{n-1} = K_p \left[ e_n - e_{n-1} + \frac{I_n - I_{n-1}}{T_i} + \frac{T_d}{\tau} (e_n + e_{n-2} - 2e_{n-1}) \right]$$



## PID Controller

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$$I_n - I_{n-1} = \tau e_n$$

## PID Controller

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then, 
$$m'_n - m'_{n-1} = K_p \left[ e_n - e_{n-1} + \frac{\tau}{T_i} e_n + \frac{T_d}{\tau} (e_n - 2e_{n-1} + e_{n-2}) \right]$$

## PID Controller

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or, 
$$m'_n = e_n \left( 1 + \frac{\tau}{T_i} + \frac{T_d}{\tau} \right) K_p - e_{n-1} \left( \frac{2T_d}{\tau} + 1 \right) K_p + e_{n-2} \left( \frac{K_p T_d}{\tau} \right) + m'_{n-1}$$

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or, 
$$m'_n = a_0 e_n + a_1 e_{n-1} + a_2 e_{n-2} + m'_{n-1}$$

## PID Controller

$$m'_n = a_o e_n + a_1 e_{n-1} + a_2 e_{n-2} + m'_{n-1}$$

where,  $a_o = K_p \left( 1 + \frac{\tau}{T_i} + \frac{T_d}{\tau} \right)$

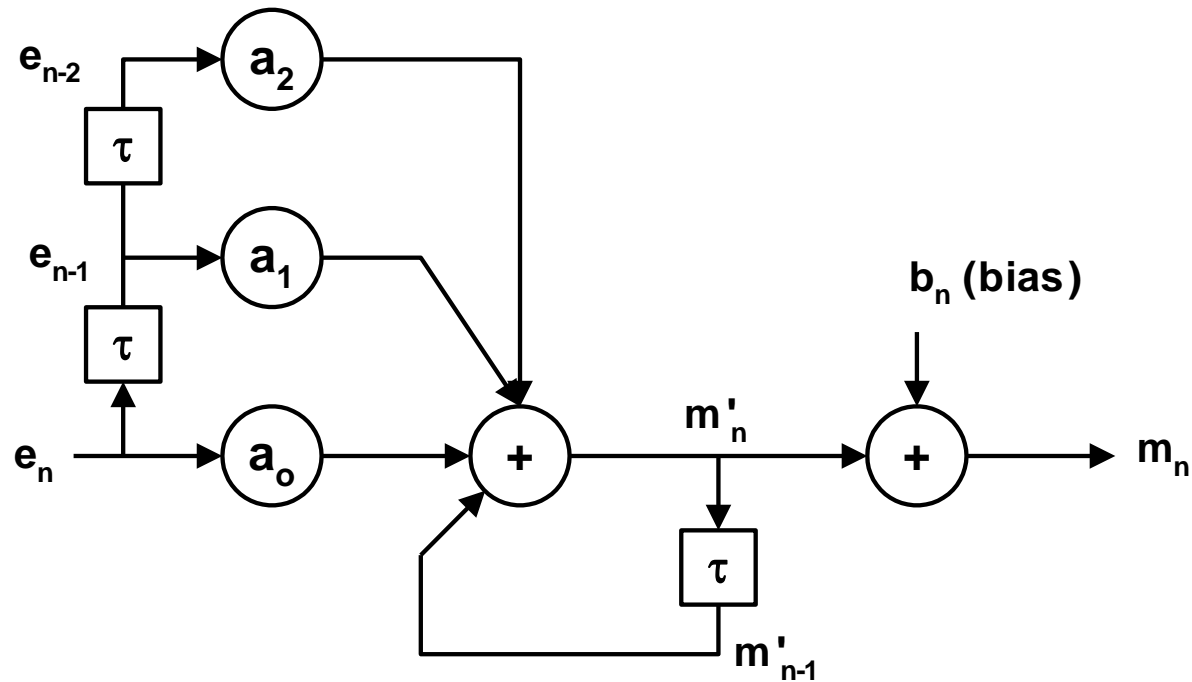
$$a_1 = -K_p \left( \frac{2T_d}{\tau} + 1 \right)$$

and  $a_2 = \frac{K_p T_d}{\tau}$

## Realization of the PID Controller

$$m'_n = a_o e_n + a_1 e_{n-1} + a_2 e_{n-2} + m'_{n-1}$$

and  $m_n = m'_n + b_n$



# PID Controller

## Problems:

1. Develop a digital PID controller using trapezoidal rule for integration
2. Develop a program in 'C' for software realization of the PID controller
3. Modify the above controller to provide anti-derivative kick feature

## Techniques used for anti-integral windup



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- **By saturating or limiting the integral value**

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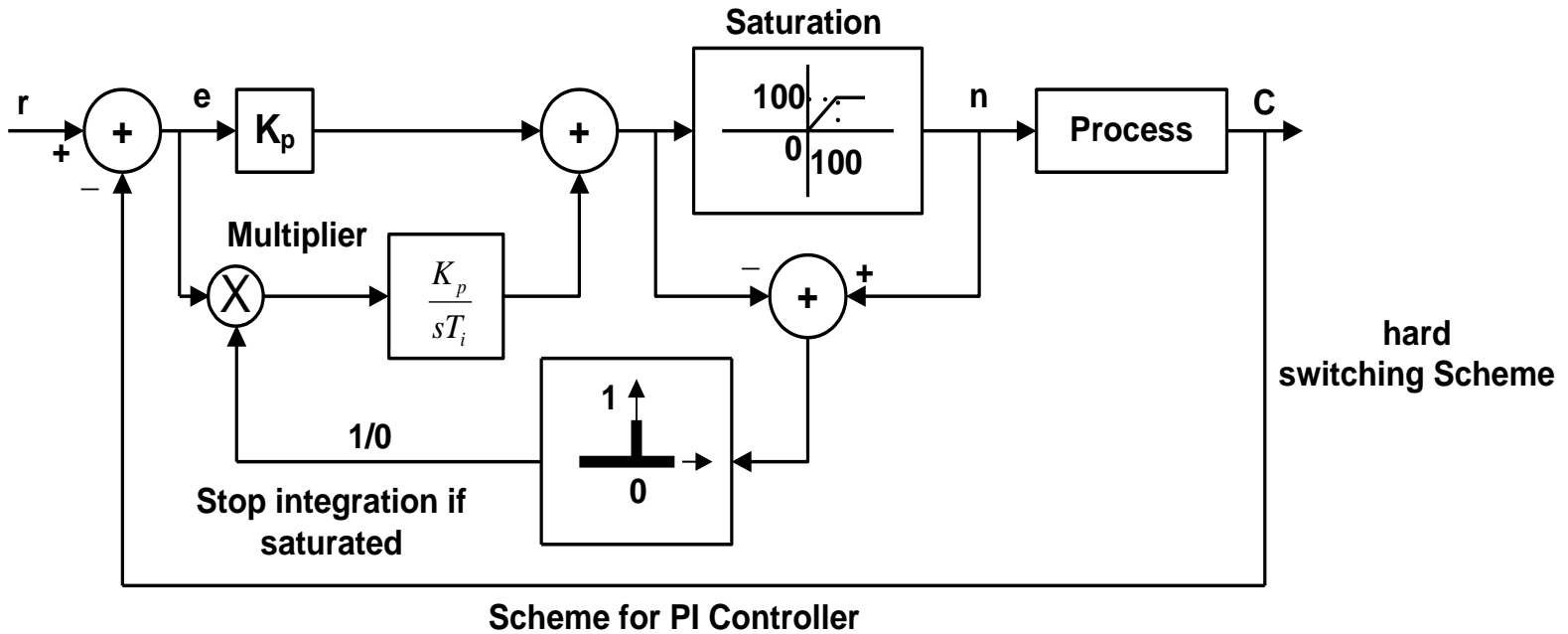
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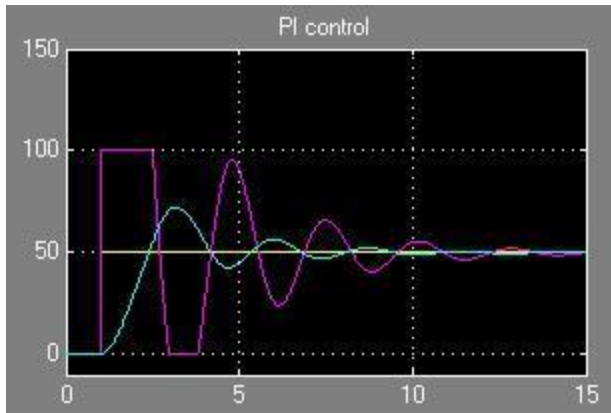
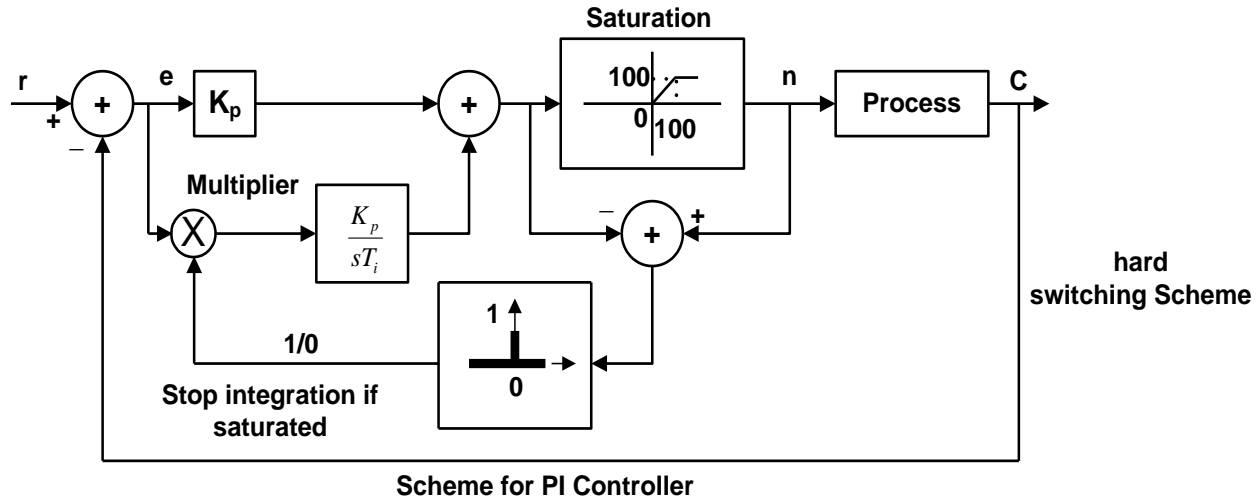
- **By saturating or limiting the integral value**
- **By resetting the integral value to zero**
- **By omitting the integral term**
- **By adaptive adjustment of controller parameters**

## Some anti-integral windup schemes

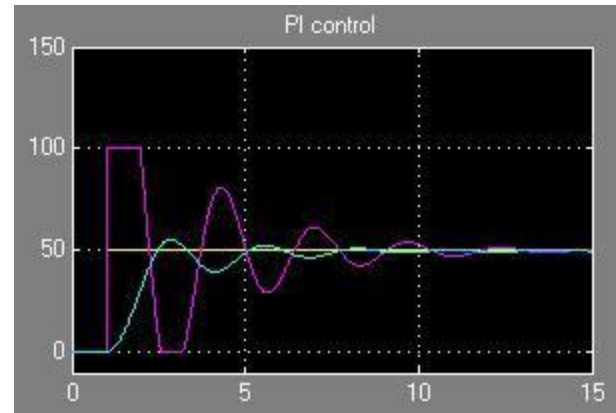
Stop integration when PI/PID controller internal output (prior to the saturation block) exceeds the saturation limits



# Performance of anti-integral windup scheme



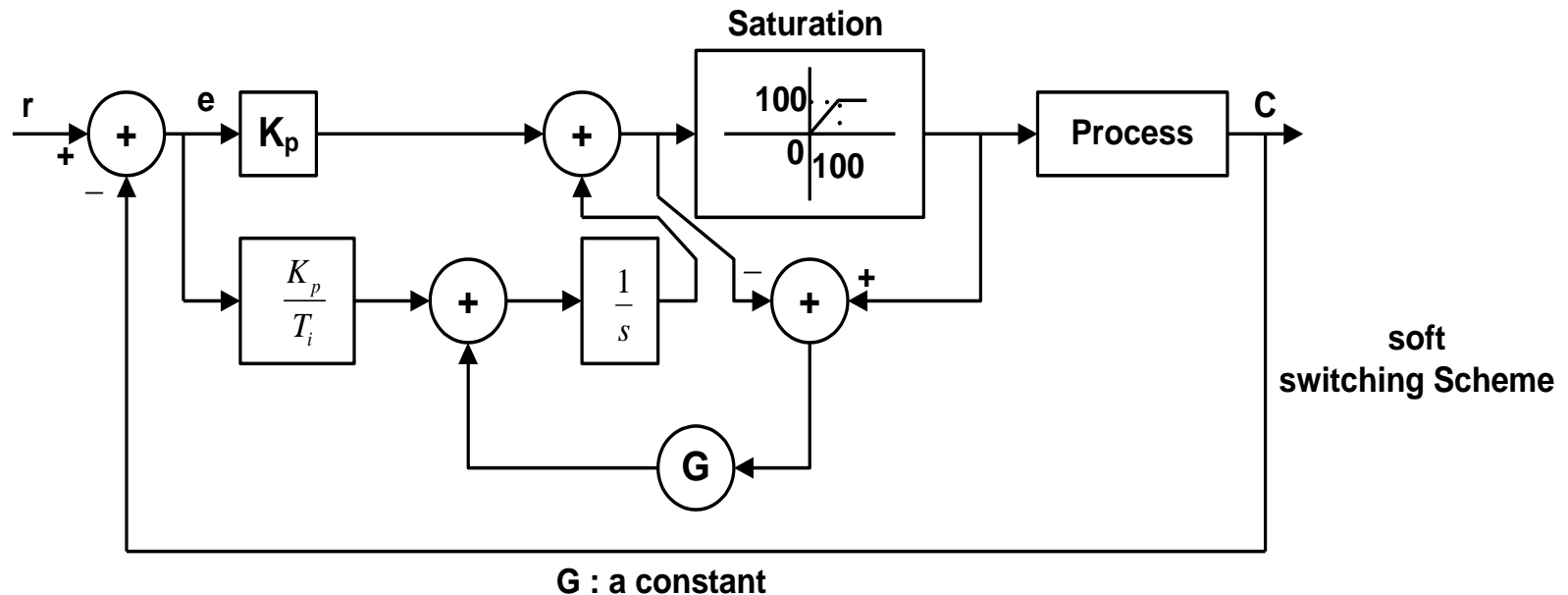
PI control without anti-integral windup



PI control with anti-integral windup

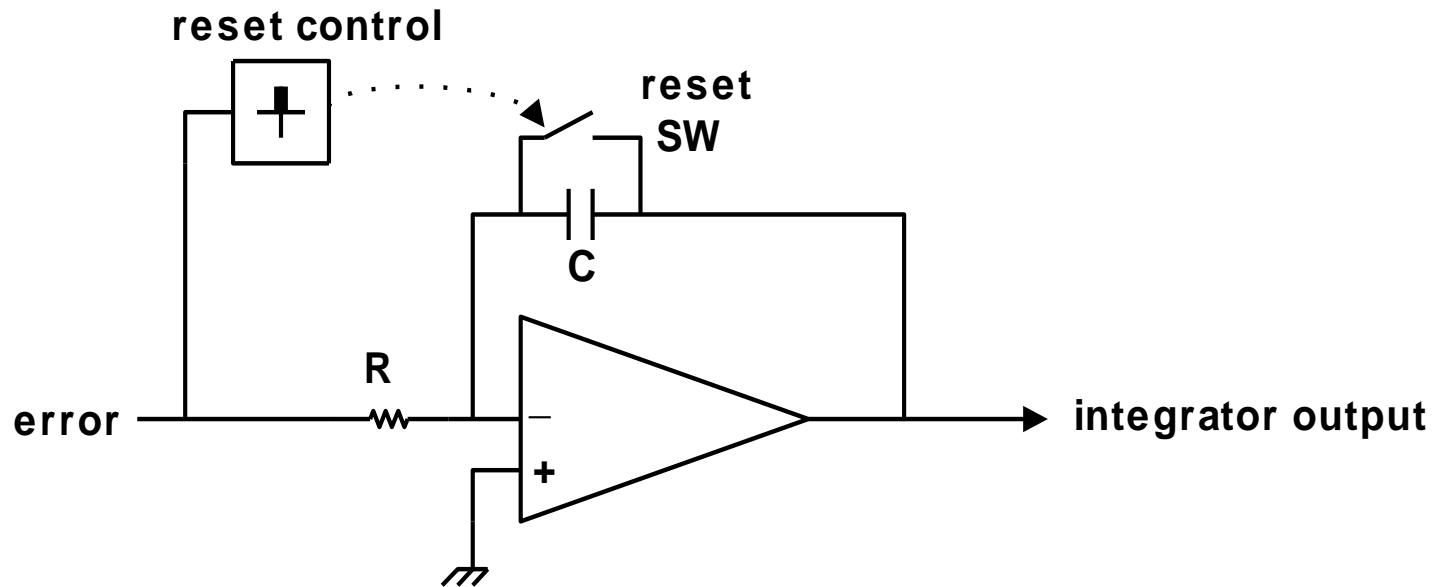
## Some anti-integral windup schemes

Reduce integration gradually as PI/PID controller internal output exceeds the saturation limits



## Some anti-integral windup schemes

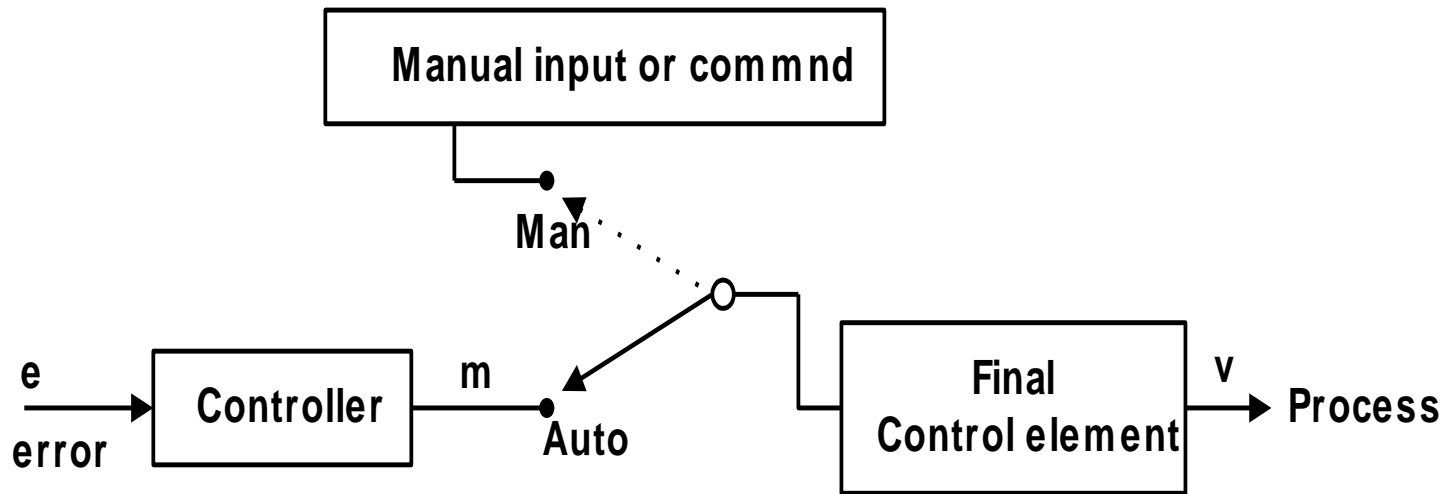
**Clegg integrator – the integrator is set to zero (reset) when the error crosses zero**



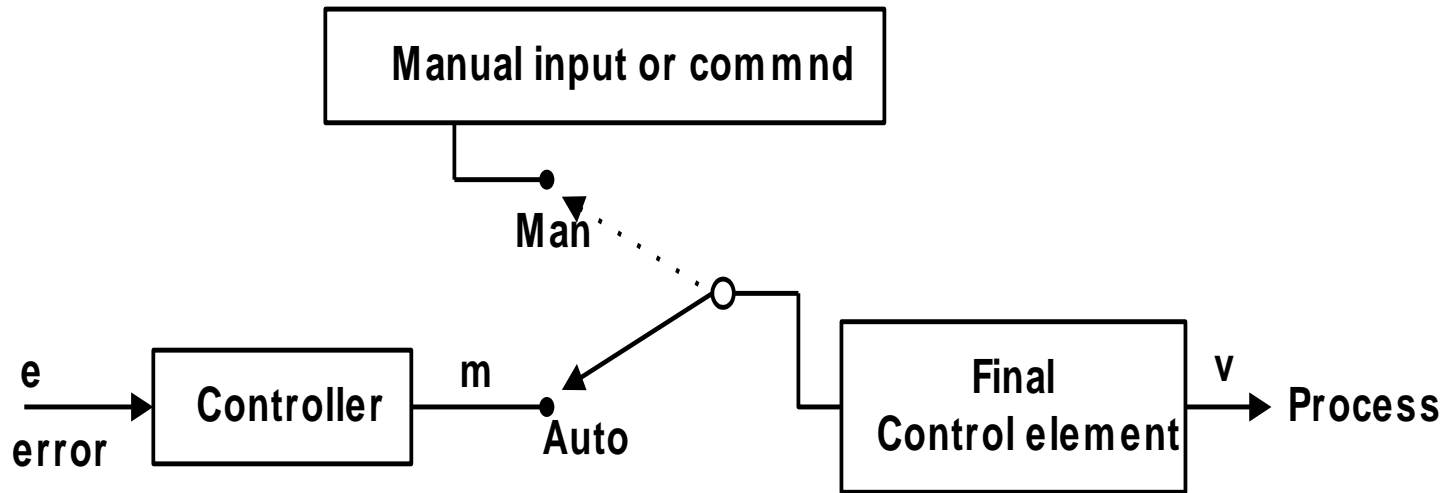


## Automatic/Manual modes of Operations

- **Automatic mode** – means automatic closed loop operation
- **Manual mode** – means open loop manual control

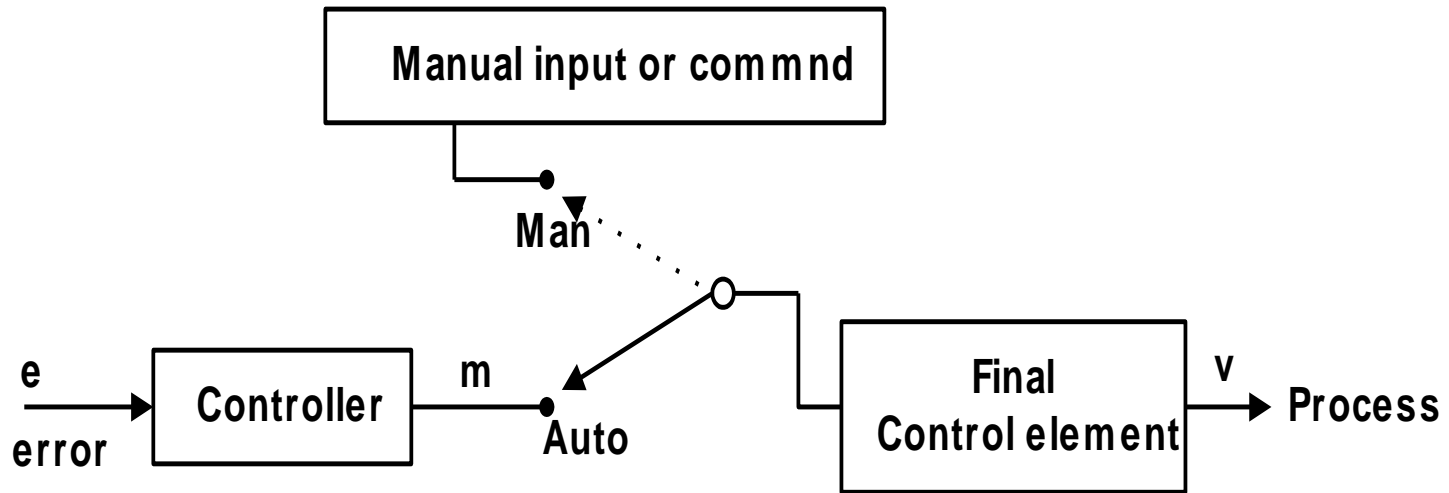


## Automatic/Manual modes of Operations



If there is any difference between the controller output and the manual command, a *bump* occurs in the process output when the switch position is altered.

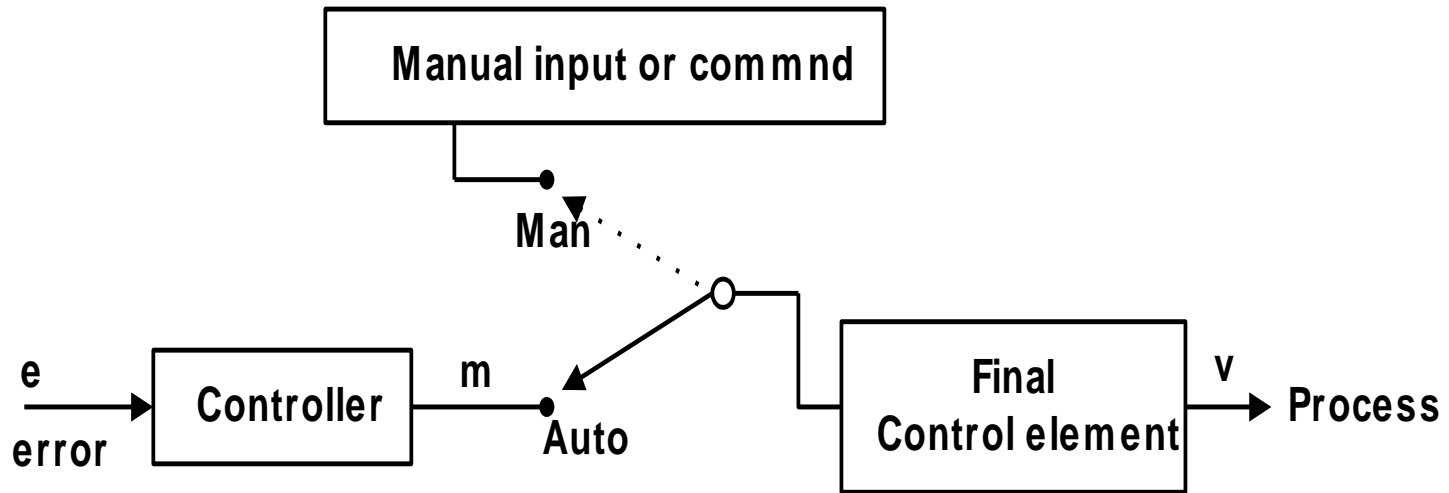
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To provide '*bump-less transfer*' from auto-to-manual change over, special arrangements may be made for '*set-point initialization*'.

## Automatic/Manual modes of Operations

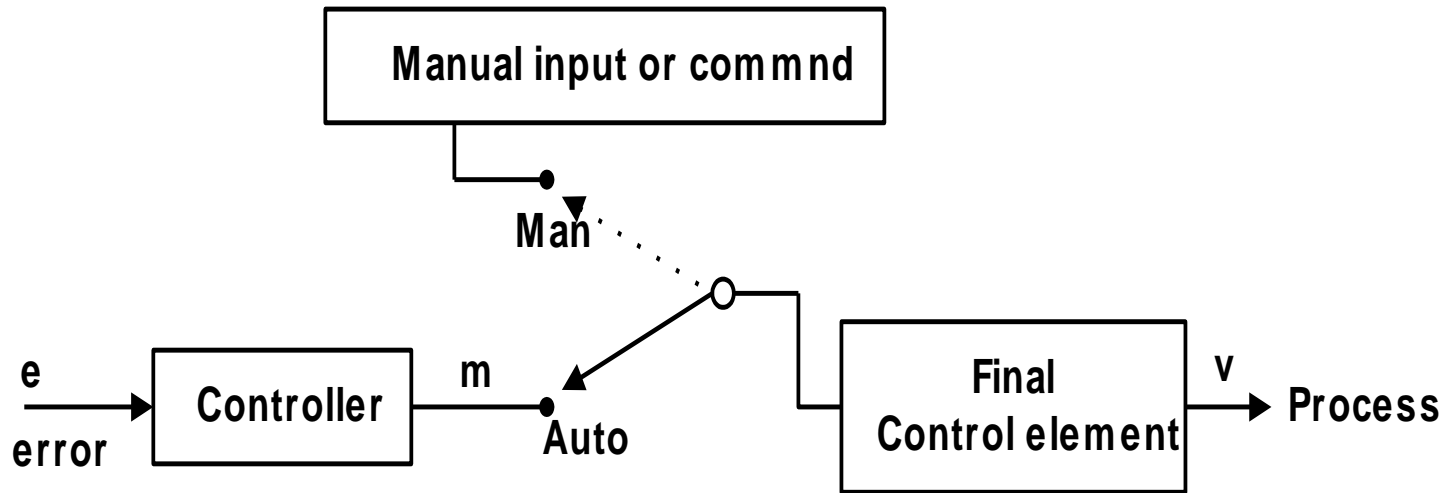


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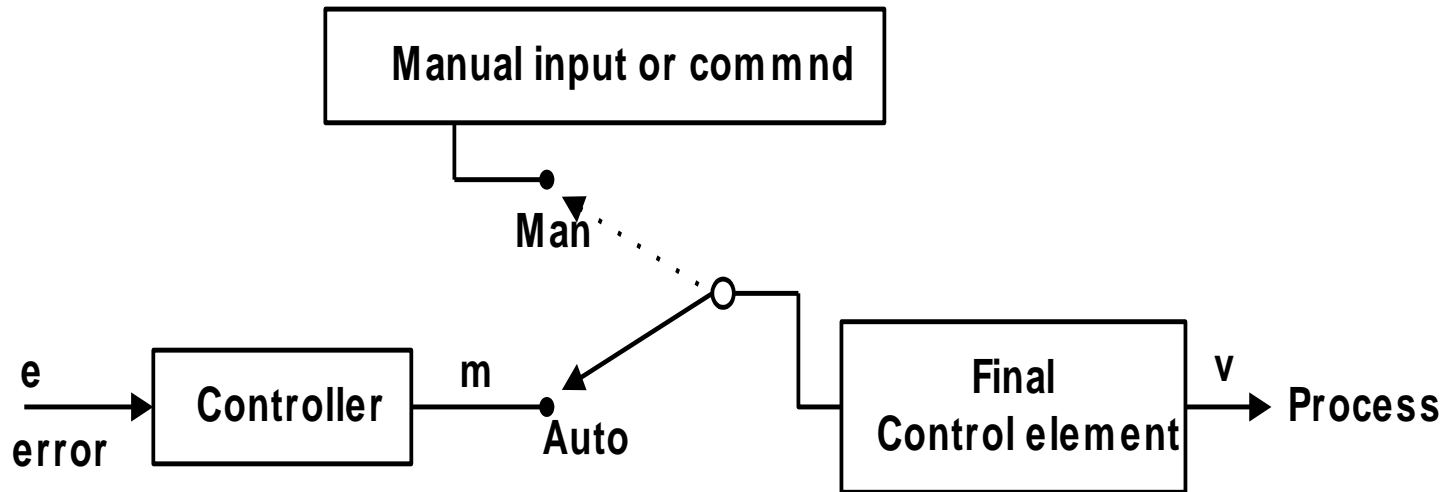
The manual command is driven to equal the controller output when the loop is in **AUTO** mode.

## Automatic/Manual modes of Operations



**When the loop is in MANUAL mode, if there is a steady error existing due to any difference between the set-point of the controller and the process output (under manual control), integral term, in case of PI and PID controllers, may wind-up to a large value, and consequently anti-integral wind-up is necessary for such situations.**

## Automatic/Manual modes of Operations

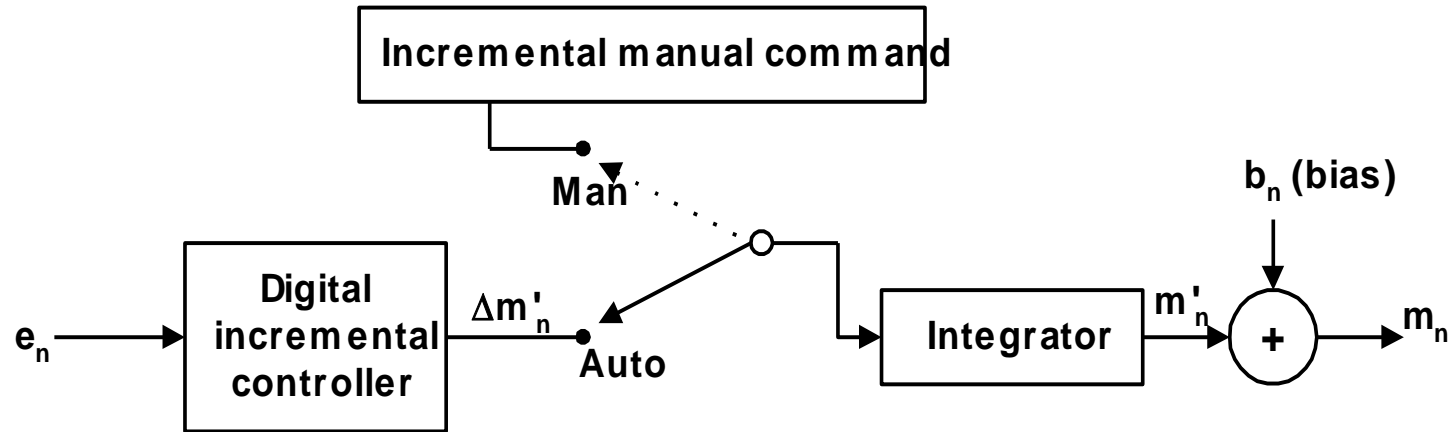


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To provide *bump-less transfer* for all the operating modes, *incremental or velocity* form of controller is used with an additional integrator.

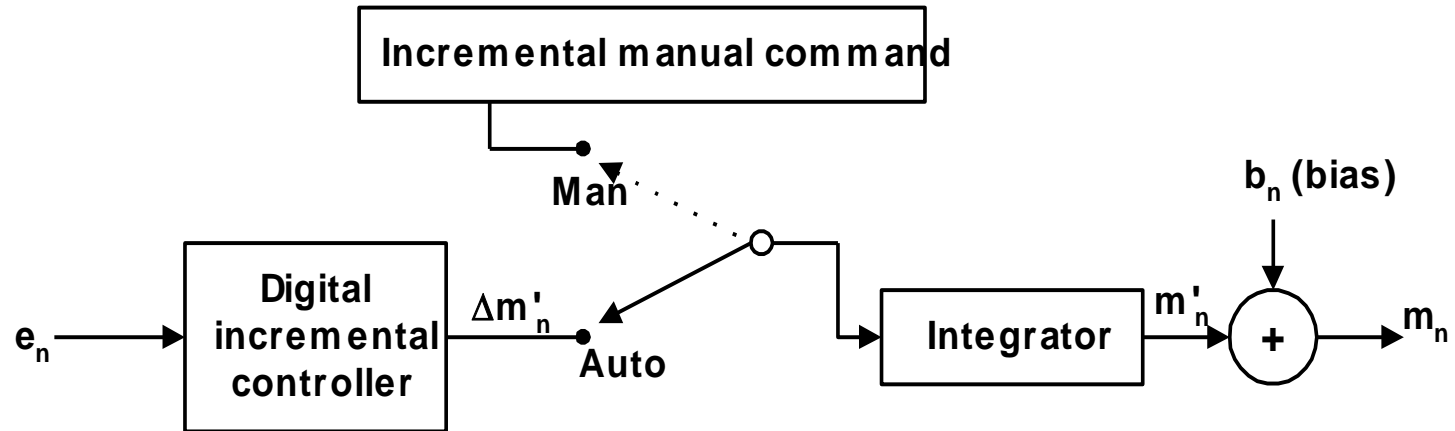
# Automatic/Manual modes of Operations

## Scheme for bump-less transfer



# Automatic/Manual modes of Operations

## Scheme for bump-less transfer



The incremental controller output (without bias) at the nth instant may be expressed as

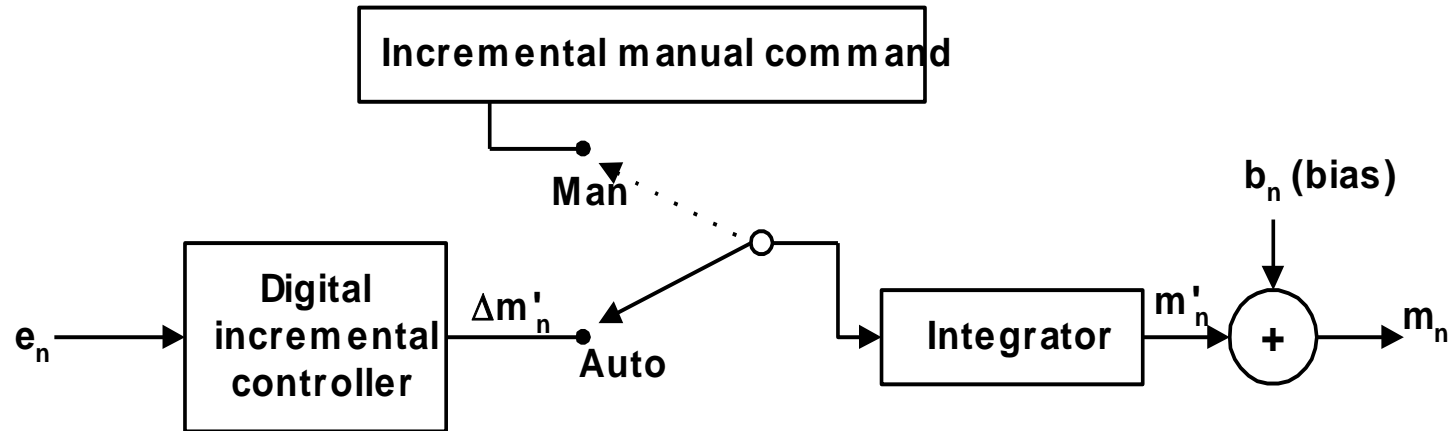
$$\Delta m'_n = m'_n - m'_{n-1}$$

$$= e_n K_p \left( 1 + \frac{\tau}{T_i} + \frac{T_d}{\tau} \right) - e_{n-1} K_p \left( \frac{2T_d}{\tau} + 1 \right) + e_{n-2} \frac{K_p T_d}{\tau} \quad \text{for a PID controller}$$



# Automatic/Manual modes of Operations

## Scheme for bump-less transfer



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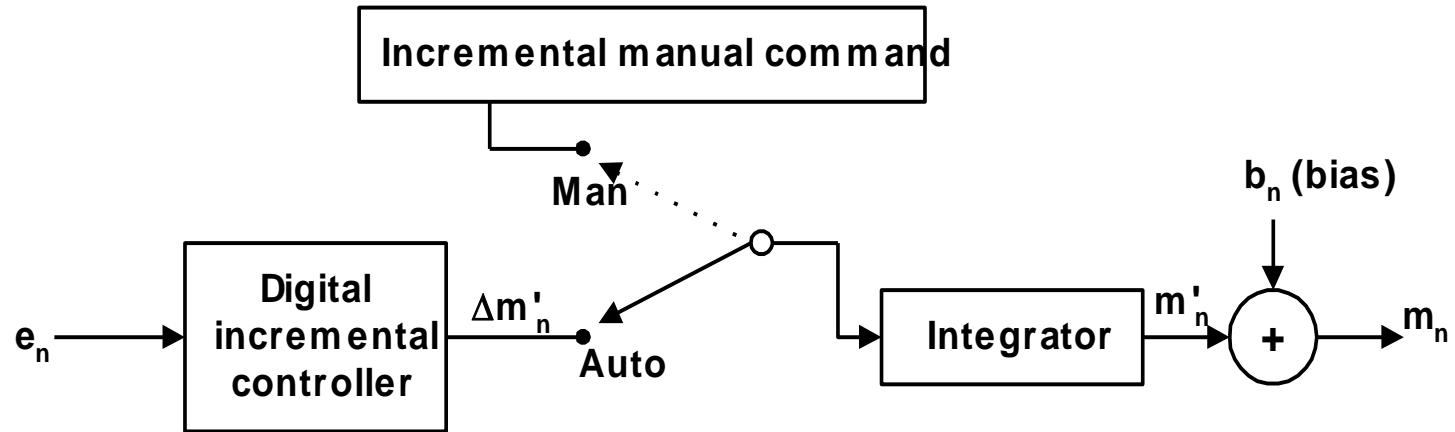
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$$= a_0 e_n + a_1 e_{n-1} + a_2 e_{n-2}$$

# Automatic/Manual modes of Operations

## Scheme for bump-less transfer

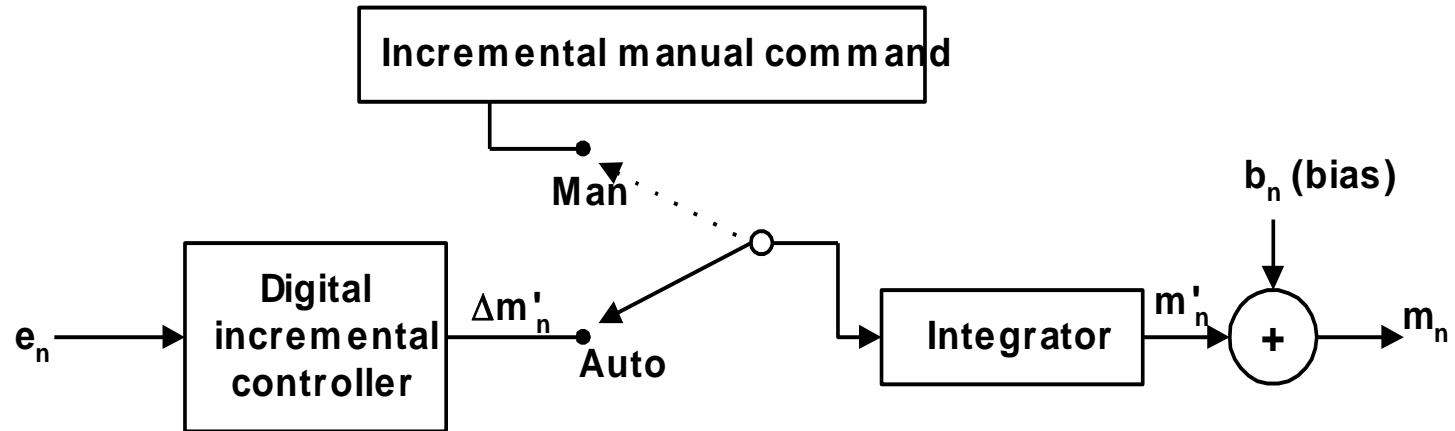


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# Automatic/Manual modes of Operations

## Scheme for bump-less transfer



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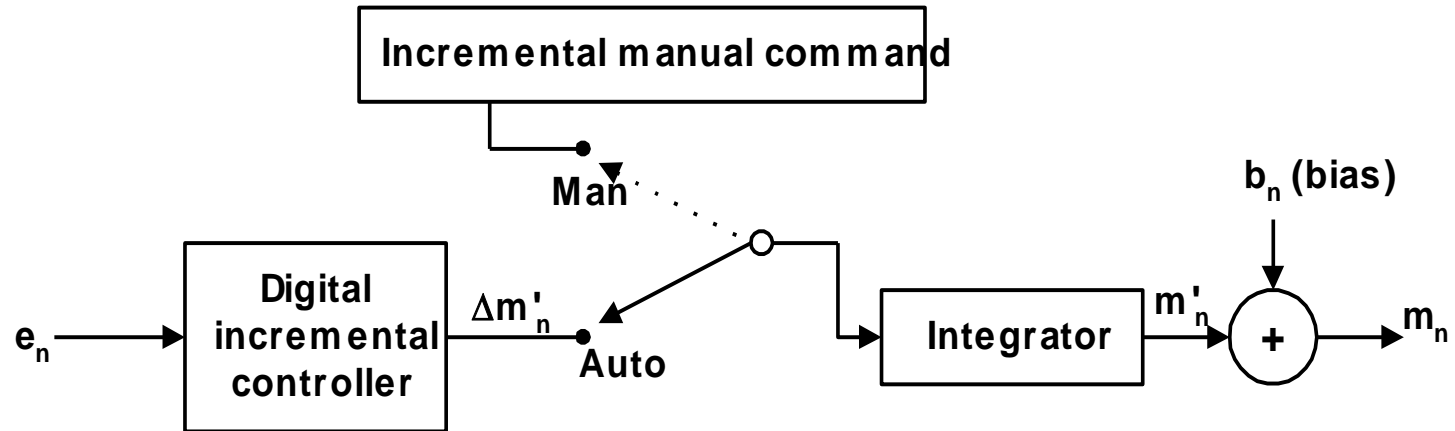


The integrator output may be represented as

$$\begin{aligned} m'_n &= m'_n - m'_{n-1} + m'_{n-1} \\ &= \Delta m'_n + m'_{n-1} \end{aligned}$$

# Automatic/Manual modes of Operations

## Scheme for bump-less transfer

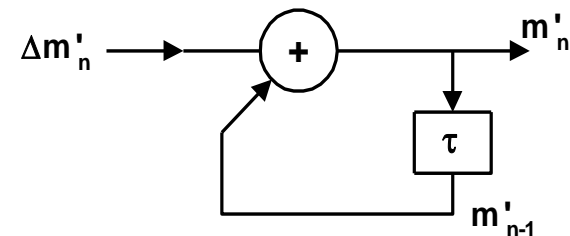


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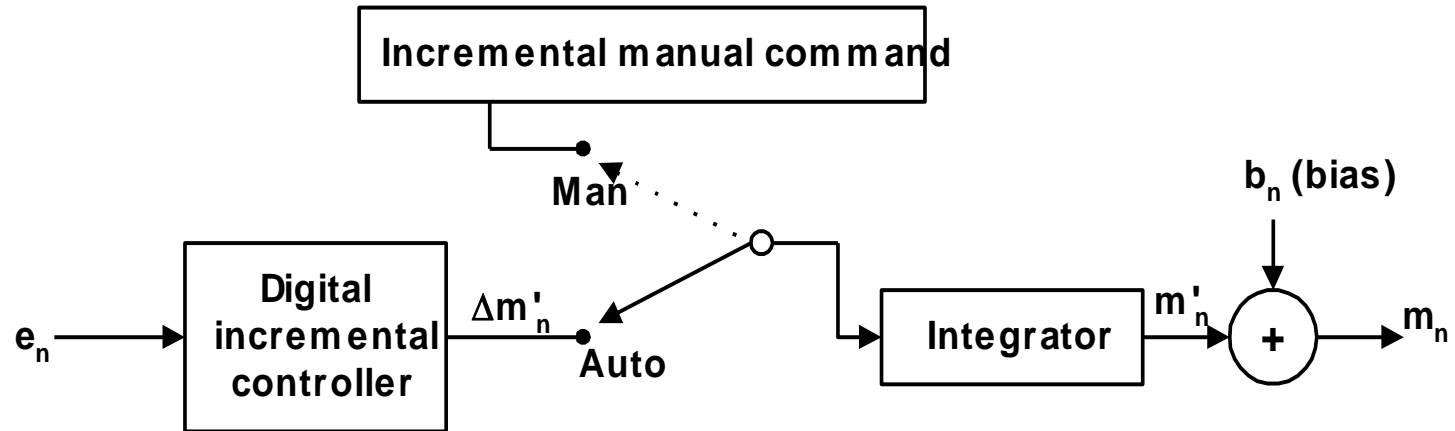
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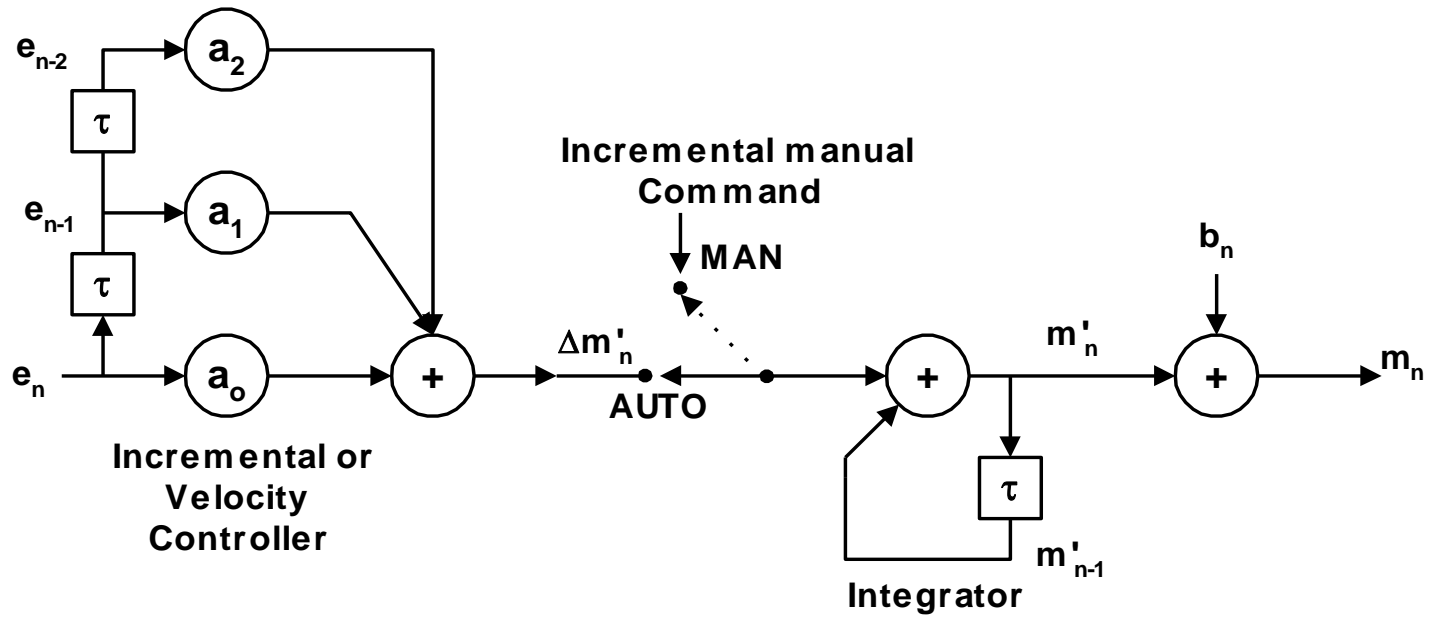
# Automatic/Manual modes of Operations

## Scheme for bump-less transfer



**The presence of integrator at the output ensures a smooth output variation even when the actual manual command is different from the actual controller output under closed-loop control.**

# Realization of the incremental type PID Controller



# Automatic tuning of PID Controllers - the Relay autotuner

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**Suitable for processes with non-zero dead-time.**



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## Z-N settings

Controller	$K_p$	$T_i$	$T_d$
P – Controller	$0.5 K_c$		
PI – Controller	$0.45 K_c$	$T_c/1.2$	
PID – Controller	$0.6 K_c$	$T_c/2$	$T_c/8$

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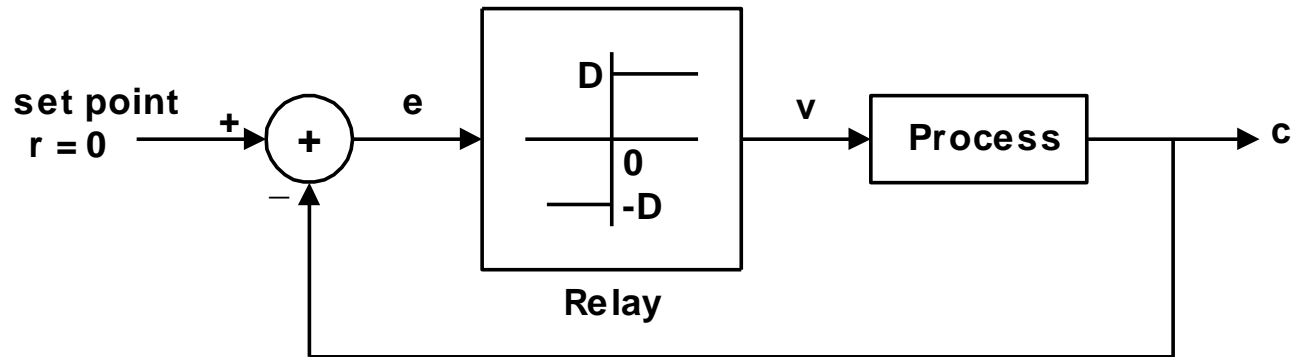
← gain margin: 2

## Automatic tuning of PID Controllers - the Relay autotuner

The critical gain  $K_c$  and critical time period  $T_c$  are determined from an experiment with relay (switching element) feedback.

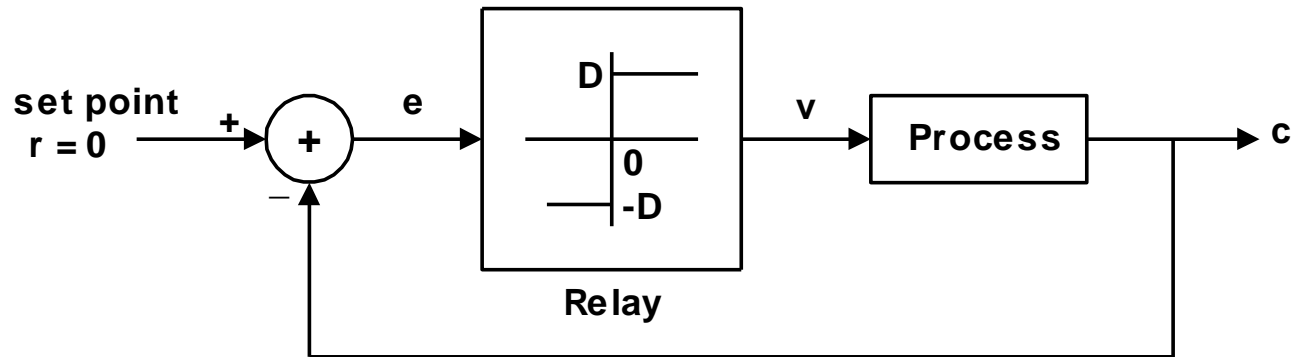
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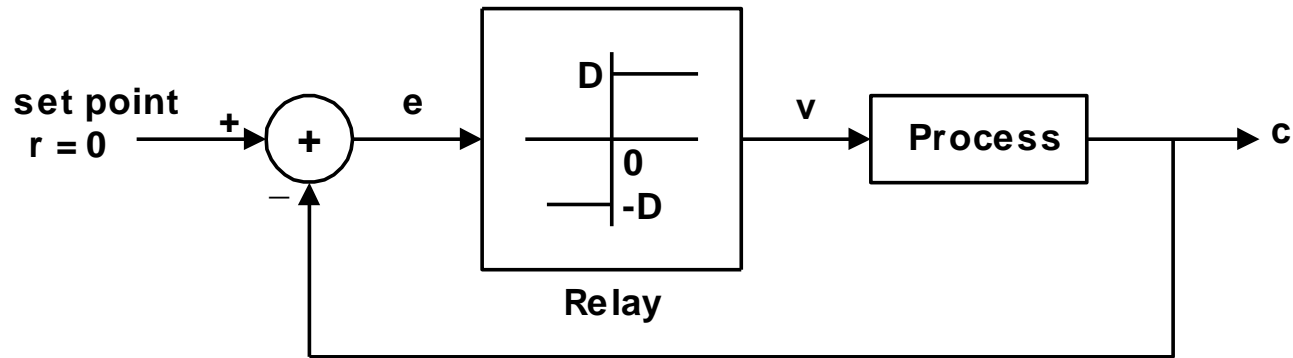


✓The relay control provides ON / OFF control of the process.



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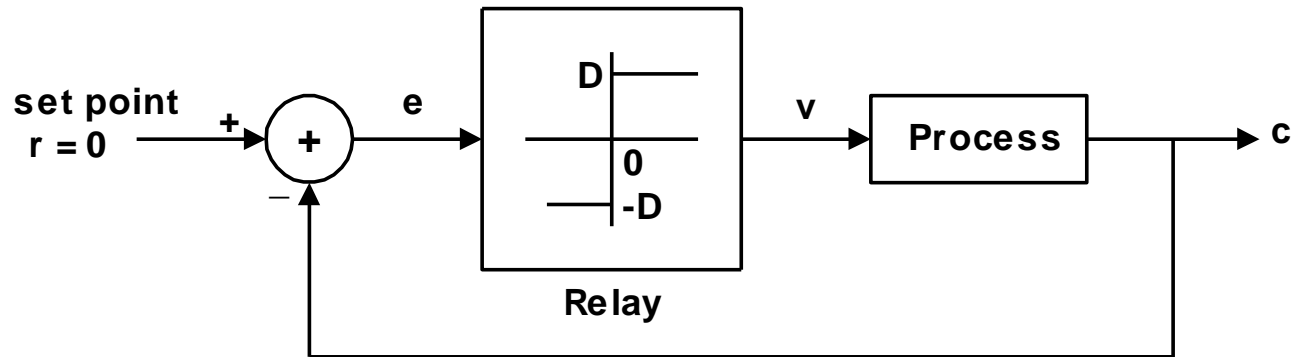


✓The relay control provides ON / OFF control of the process.

✓The input 'r' is set to zero.

## Automatic tuning of PID Controllers - the Relay autotuner

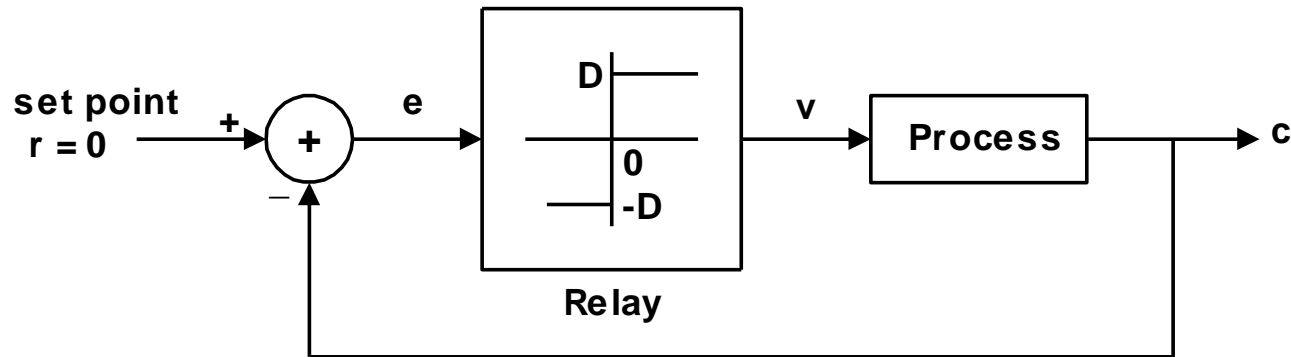
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- ✓ The relay control provides ON / OFF control of the process.
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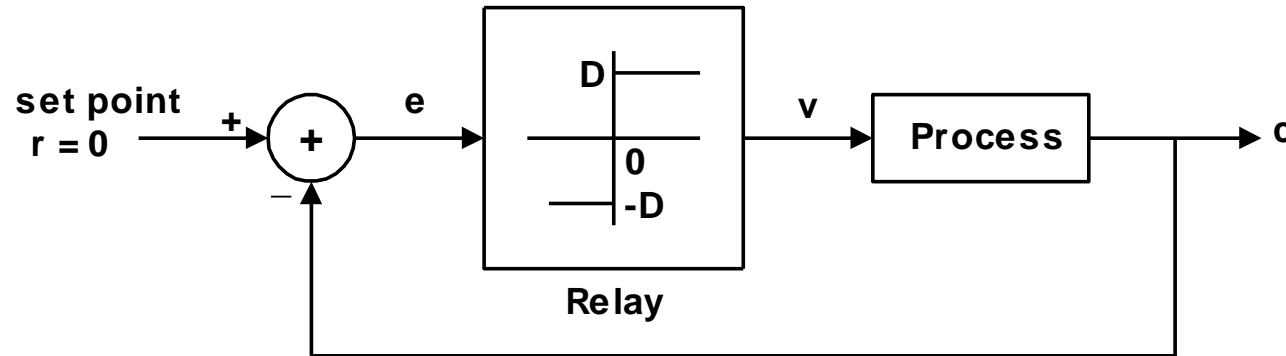
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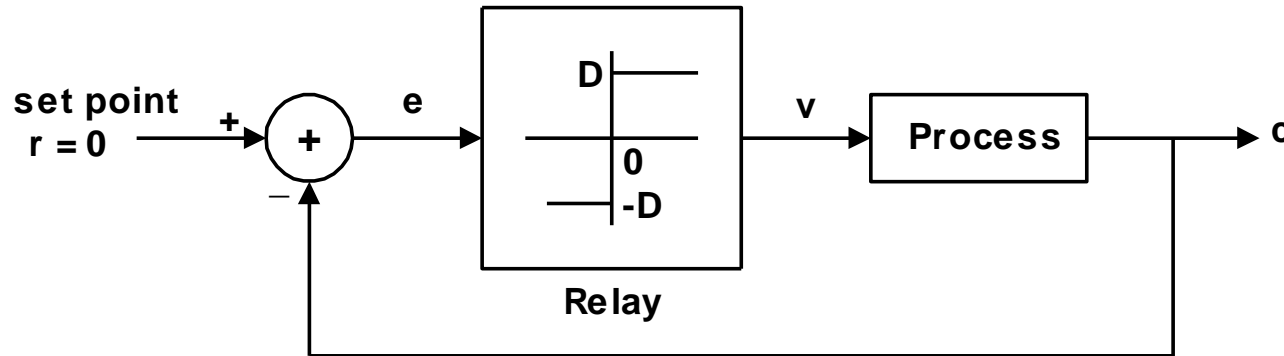
- ✓ The relay control provides ON / OFF control of the process.
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- ✓ The process is driven by a square wave of amplitude 'D'.

# Automatic tuning of PID Controllers - the Relay autotuner



**Assuming the process to be a low-pass system, the process output 'c' contains mainly the fundamental component.**

# Automatic tuning of PID Controllers - the Relay autotuner

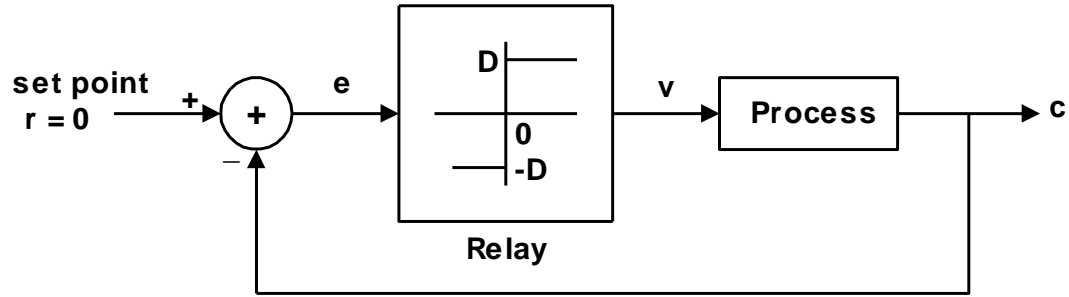


Assuming the process to be a low-pass system, the process output 'c' contains mainly the fundamental component.

Thus the error signal 'e' becomes sinusoidal,

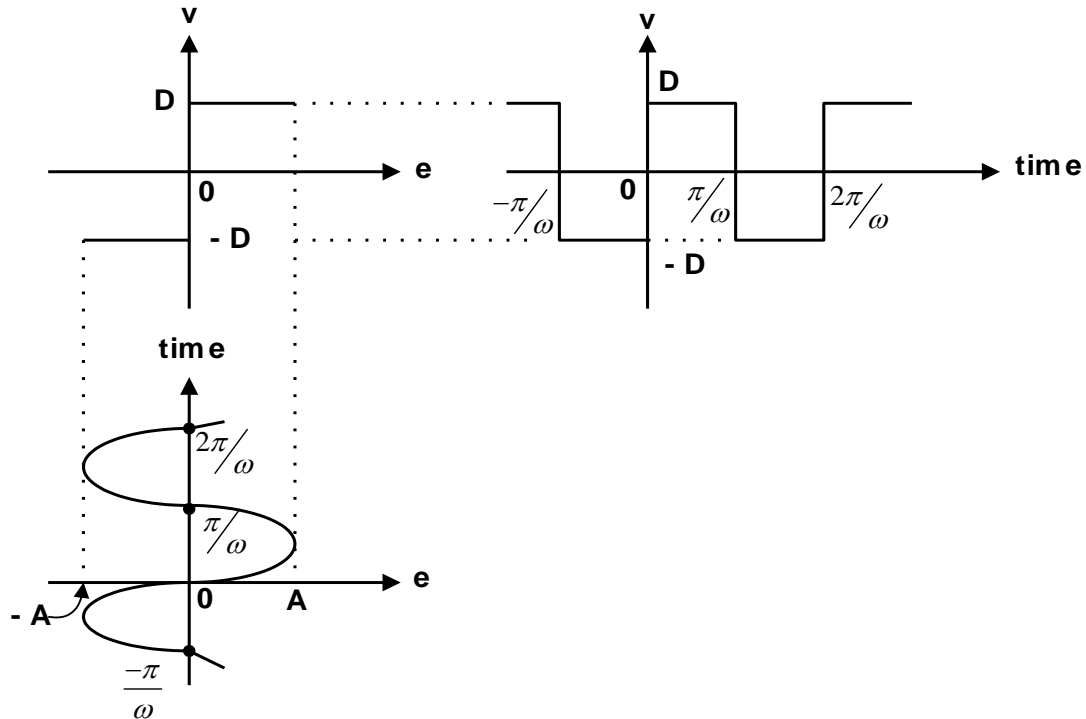
$$e = A \sin \omega t$$

# Automatic tuning of PID Controllers - the Relay autotuner

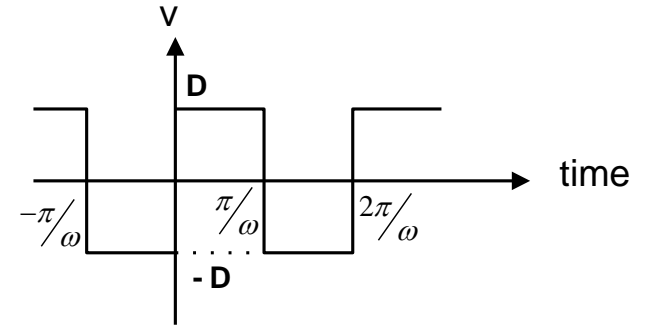
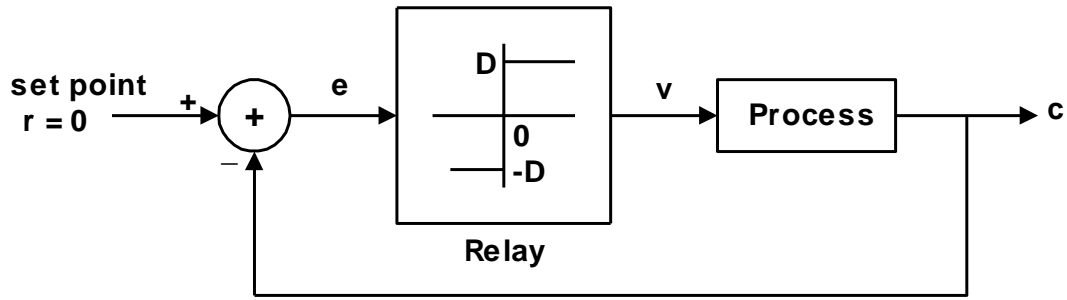


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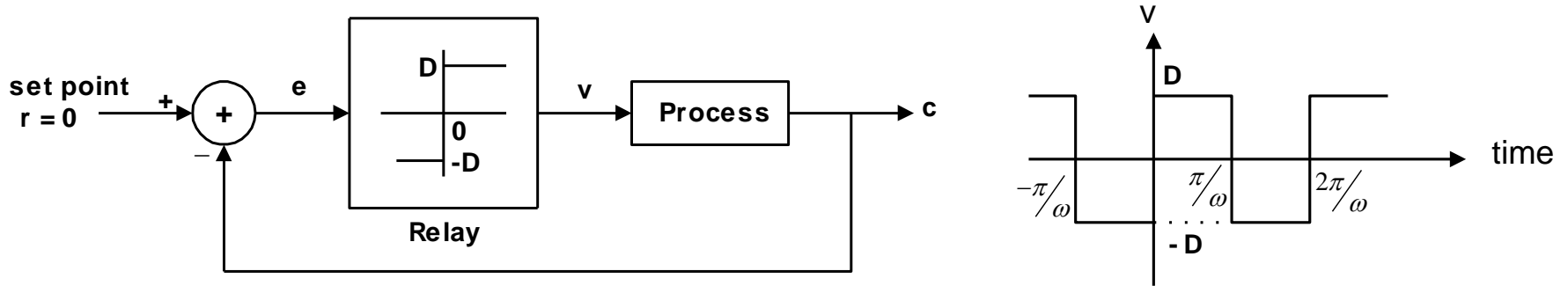
The relay output 'v' may be found out as follows:



# Automatic tuning of PID Controllers - the Relay autotuner



## Automatic tuning of PID Controllers - the Relay autotuner

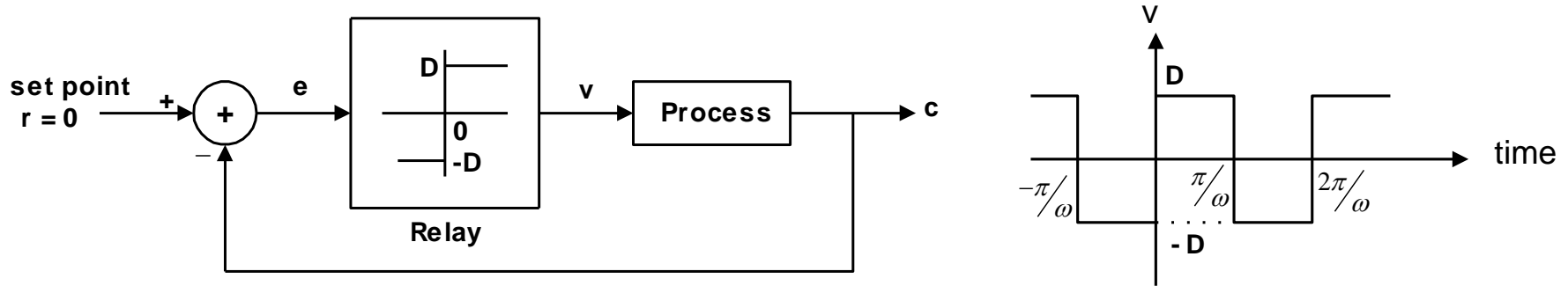


The Fourier series of the relay output ( $v$ ) may be expressed as:

$$v = \frac{4D}{\pi} \left( \sin \omega t + \frac{1}{3} \sin 3\omega t + \frac{1}{5} \sin 5\omega t + \dots \right)$$



## Automatic tuning of PID Controllers - the Relay autotuner

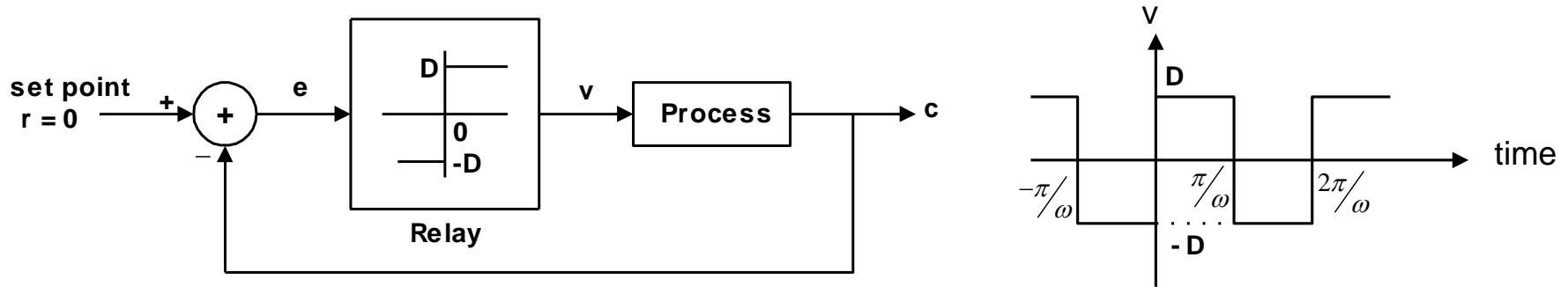


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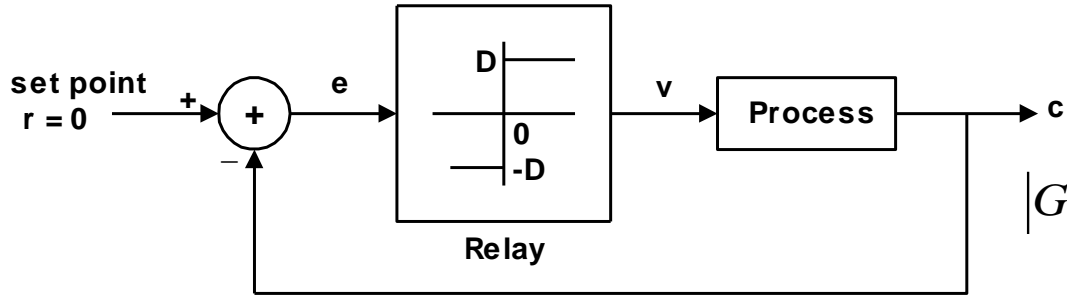
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**The process practically attenuates all higher harmonics other than the fundamental.**

Then the process gain at frequency ' $\omega$ ' becomes

$$|G(\omega)| = \frac{\text{output amplitude}}{\text{input amplitude}} = \frac{A}{\frac{4D}{\pi}} = \frac{\pi A}{4D}$$

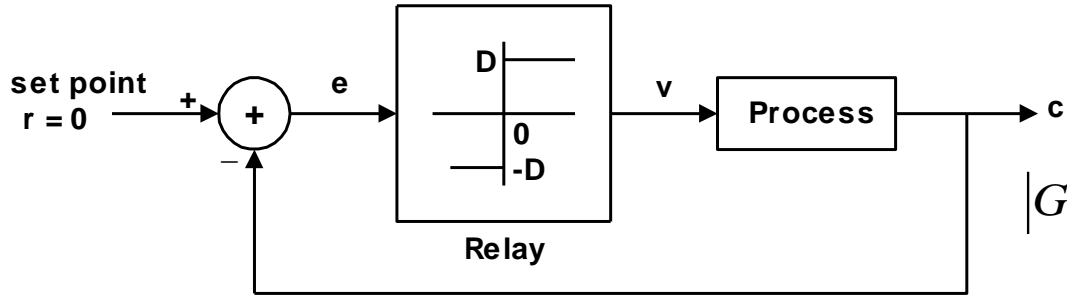
# Automatic tuning of PID Controllers - the Relay autotuner



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# Automatic tuning of PID Controllers - the Relay autotuner

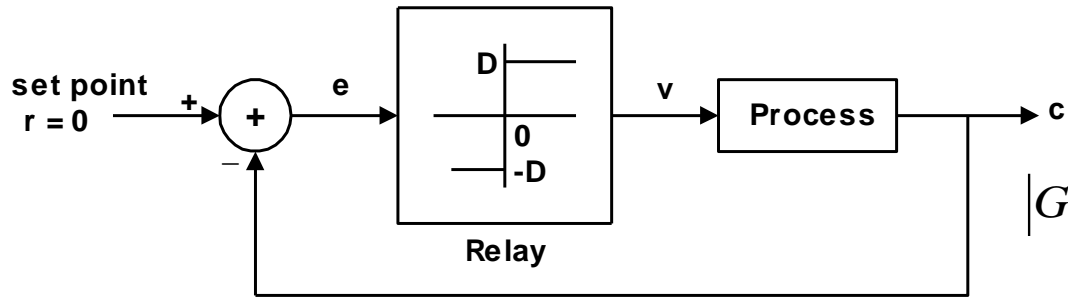


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## Automatic tuning of PID Controllers - the Relay autotuner



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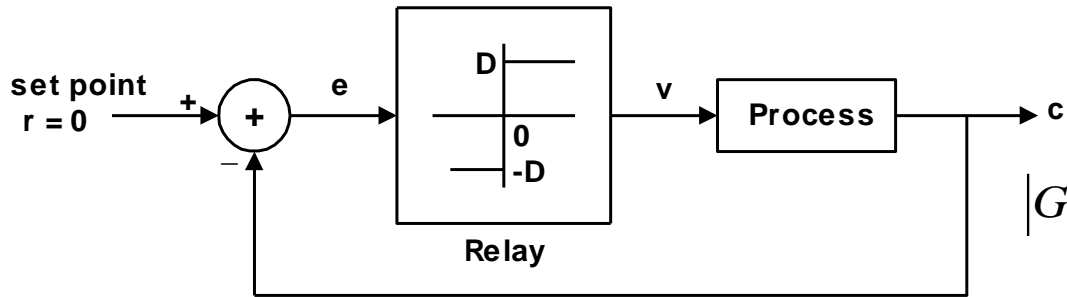
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Thus the gain of the relay controller (i.e. the critical gain) at  $\omega = \omega_c$  is

$$K_c = \frac{1}{|G(\omega_c)|} = \frac{4D}{\pi A} \quad \left[ \text{as } K_c \cdot |G(\omega_c)| = 1 \right]$$

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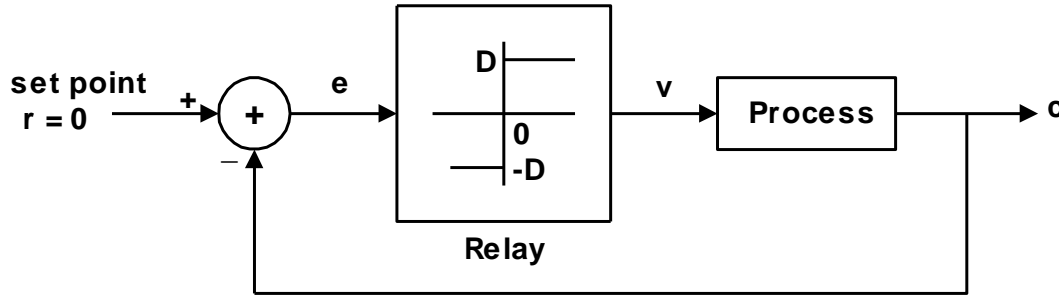
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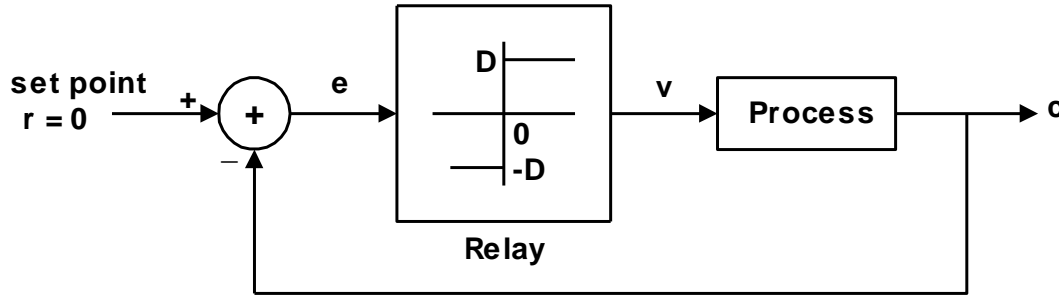
Also  $\angle G(\omega_c) = \pi$ , as relay phase shift is zero.

## Automatic tuning of PID Controllers - the Relay autotuner



Thus by knowing the relay amplitude 'D' and by measuring the amplitude 'A' of the process output 'c', critical gain  $K_c$  may be determined  $\left[ K_c = \frac{4D}{\pi A} \right]$ .

## Automatic tuning of PID Controllers - the Relay autotuner



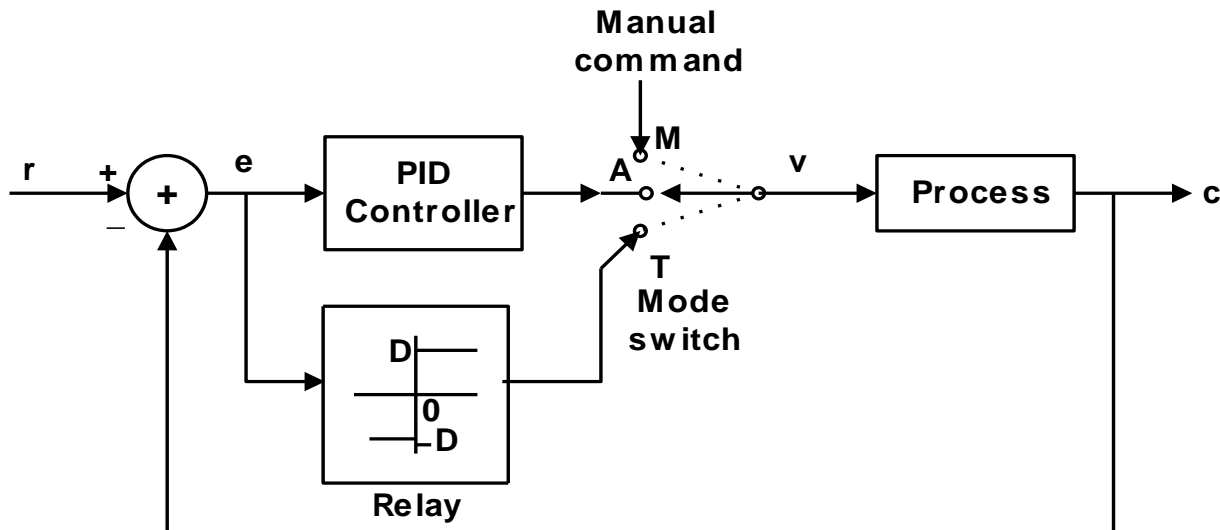
Thus by knowing the relay amplitude 'D' and by measuring the amplitude 'A' of the process output 'c', critical gain  $K_c$  may be determined  $\left[ K_c = \frac{4D}{\pi A} \right]$ .

$T_c$  may be estimated by measuring the frequency of the output oscillation  $\left[ T_c = \frac{2\pi}{\omega_c} \right]$ .



# Block diagram of the Relay autotuner

(The Satt Control Autotuner by Satt Control, Sweden)



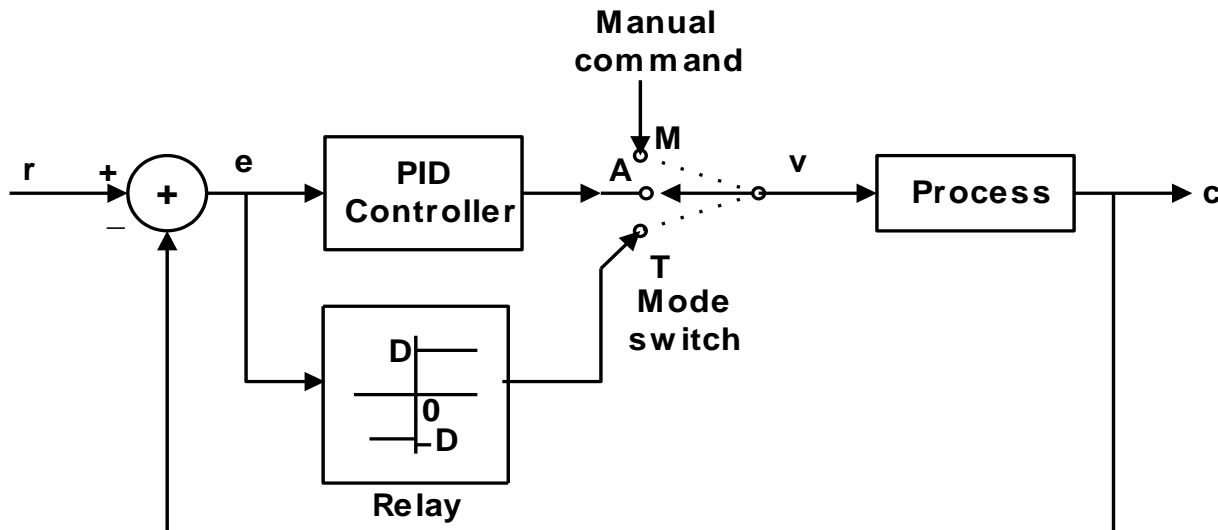
**M** → Manual position

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# Block diagram of the Relay autotuner

(The Satt Control Autotuner by Satt Control, Sweden)



$M \rightarrow$  Manual position

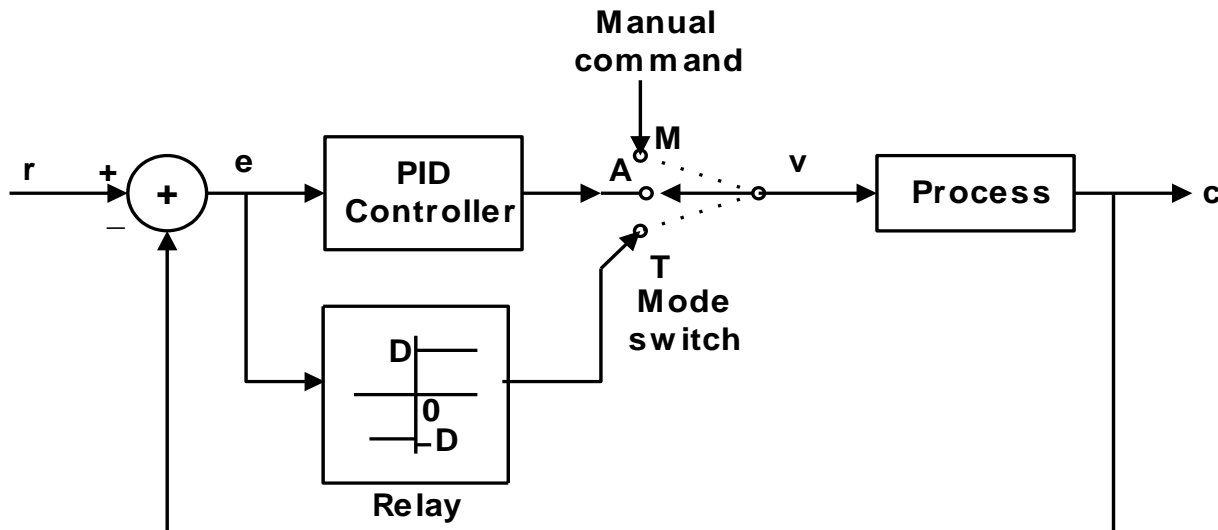
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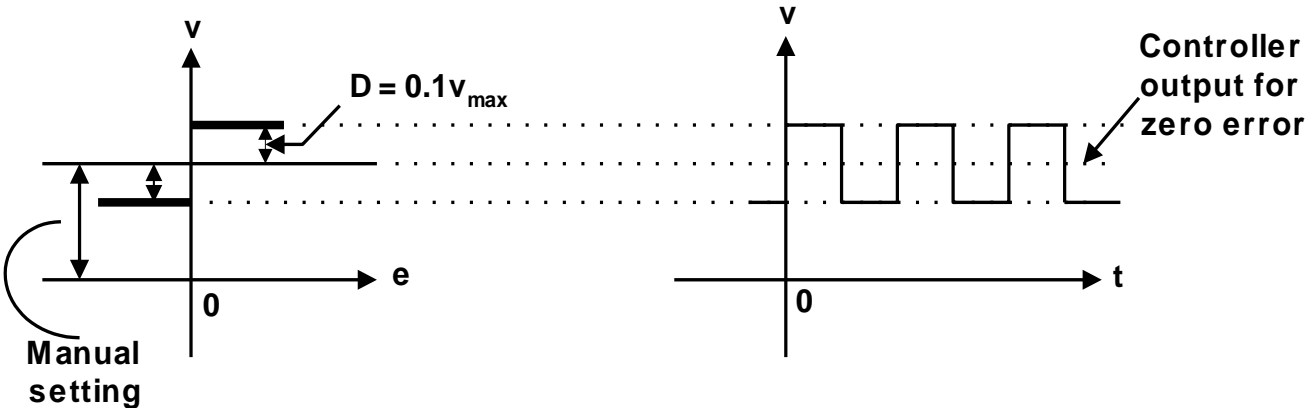
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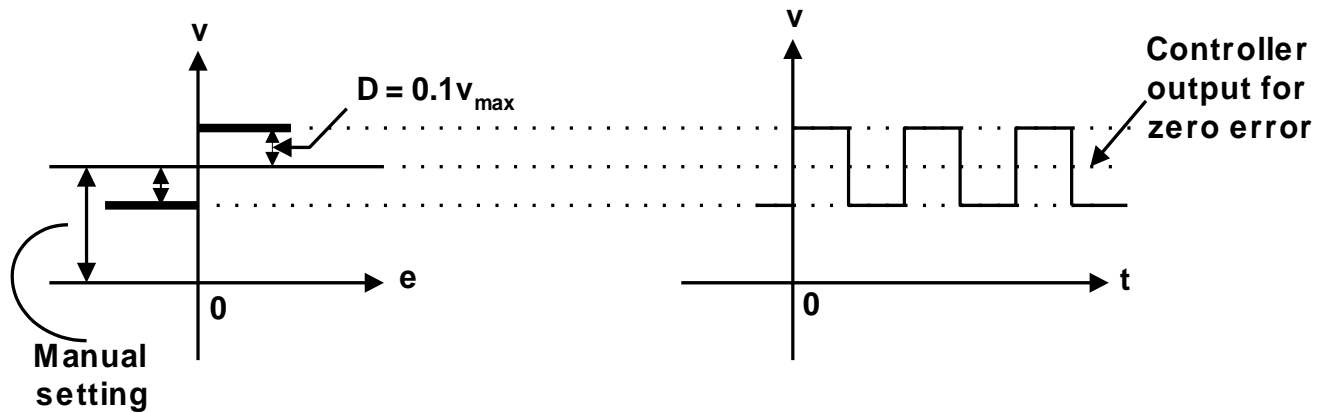
At first, the process is brought to equilibrium state ( $\approx$  zero error), by setting a constant control signal in manual mode.

The tuning is then activated by pushing the mode switch to tune position.

# Modified relay characteristic for a non-zero set-point

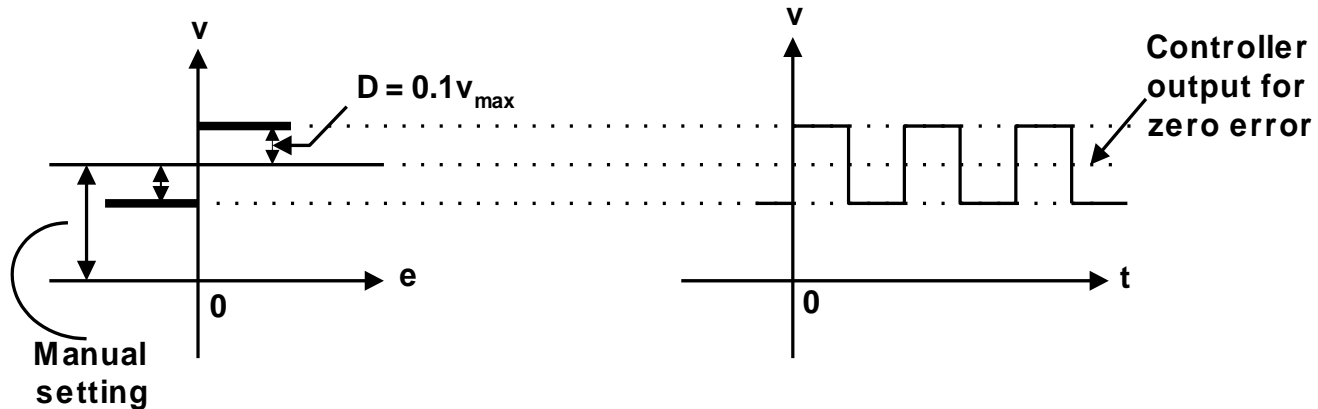


## Modified relay characteristic for a non-zero set-point



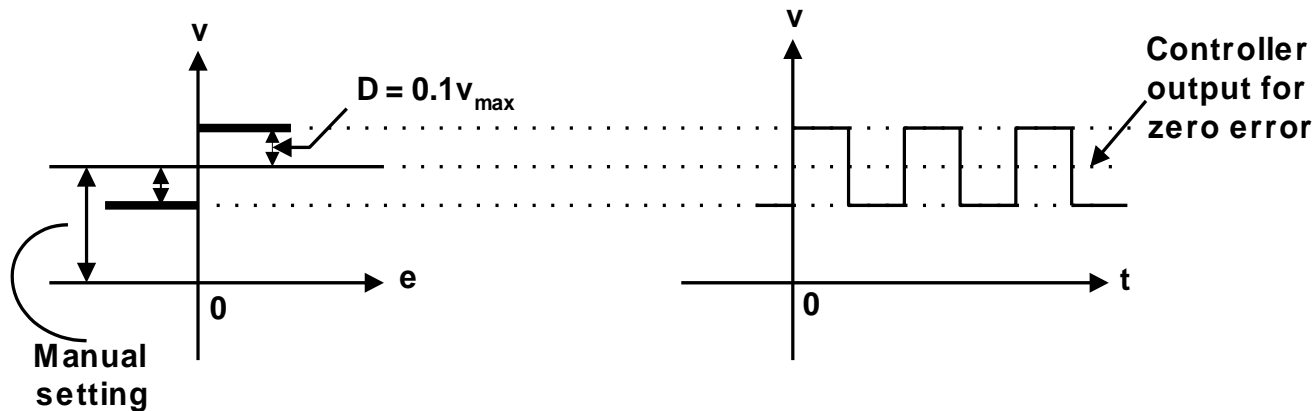
- The relay amplitude 'D' is initially set to 10% of the controller output-range.

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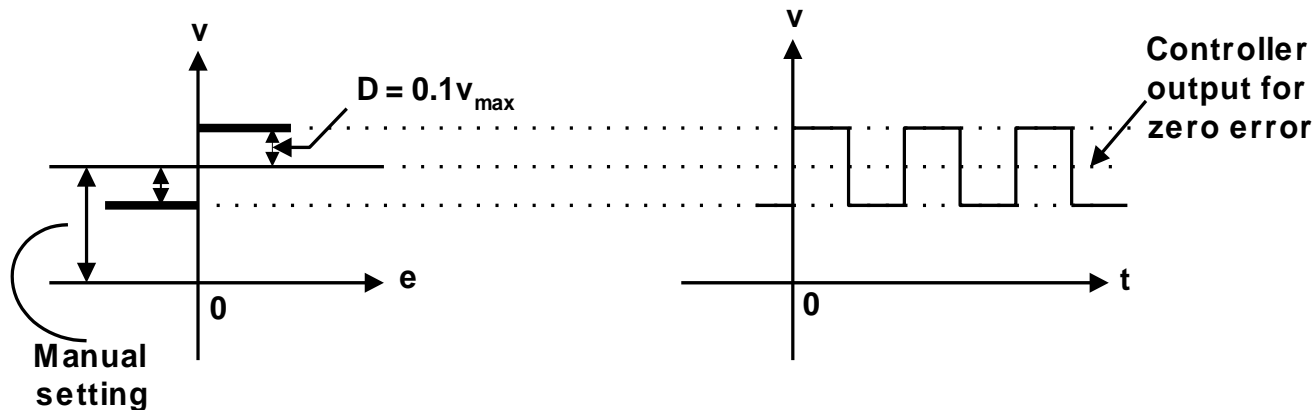
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- This amplitude is adjusted after one and a half period to give oscillation of 2% of the mean output.

## Modified relay characteristic for a non-zero set-point



- The relay amplitude 'D' is initially set to 10% of the controller output-range.
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- This ensures minimum disturbance at the process output due to tuning.

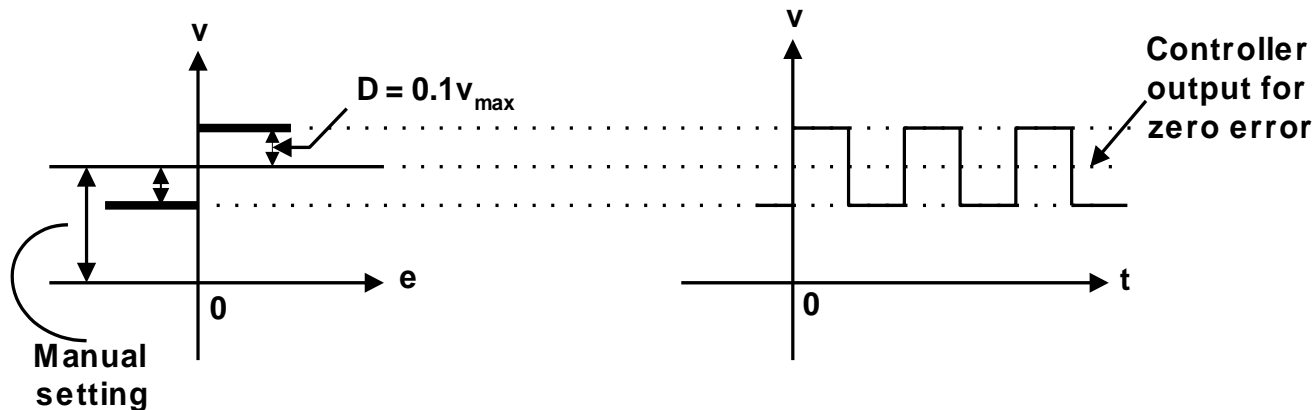
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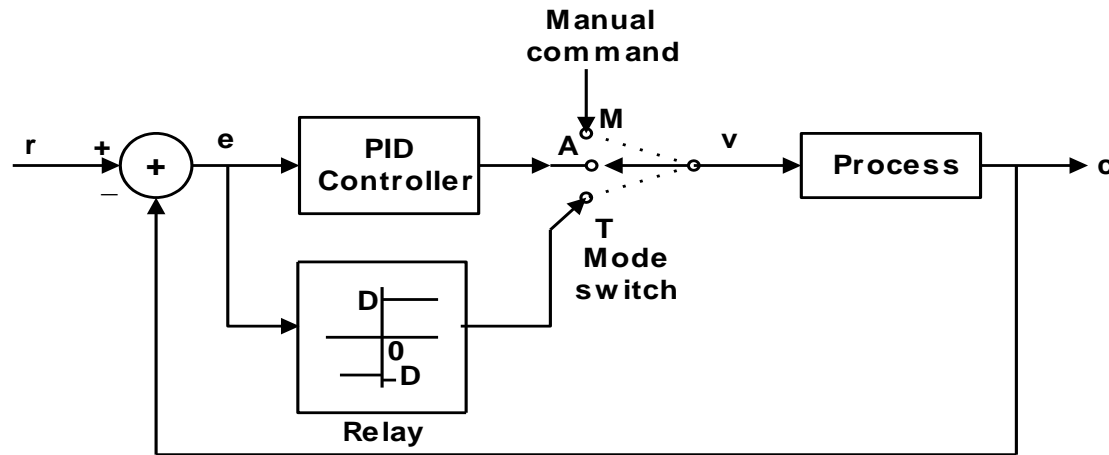


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- This amplitude is adjusted after one and a half period to give oscillation of 2% of the mean output.
- This ensures minimum disturbance at the process output due to tuning.
- This adjustment is done by measuring the change in output during the first one and a half period.
- The modified relay amplitude is stored for the next tuning operation.

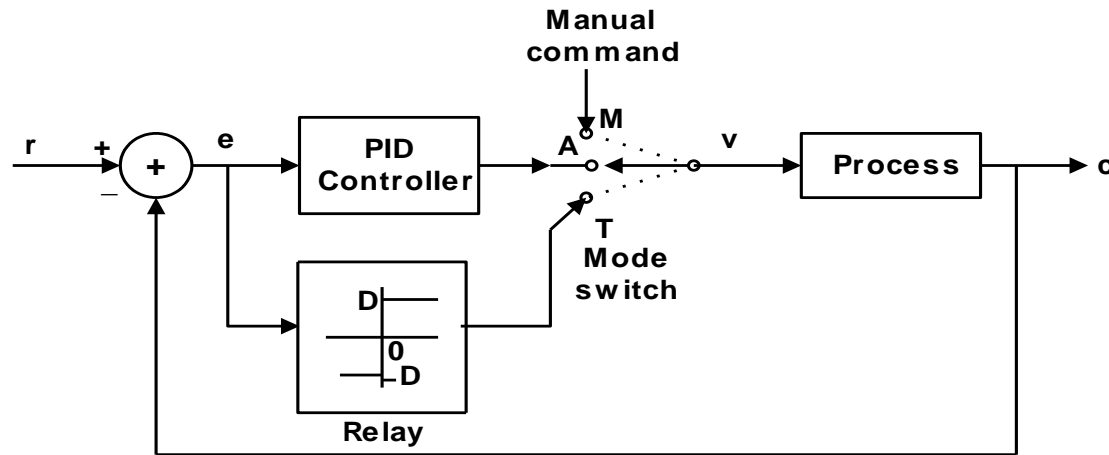
# Satt Control Autotuner



- M → Manual position
- A → Auto position
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The system is automatically switched to Auto mode after estimating the critical gain  $K_c$  and critical time period  $T_c$  during first  $5\frac{1}{2}$  period of oscillation.

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The parameters of PID controller (viz.  $K_p$ ,  $T_i$  and  $T_d$ ) are determined from  $K_c$  and  $T_c$  according to Z-N rule.

## References

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3. **Principles of Process Control** *by* Patranabis
4. **Process Control** *by* Harriott
5. **Process Systems Analysis and Control** *by* Coughanowr and Koppel
6. **Process Control** *by* Pollard
7. **Chemical Process Control** *by* Stephanopoulos
8. **Modern Control Engineering** *by* Ogata
9. **Applied Process Control** *by* Chidambaram

Thank You