Control of Time-delay Systems

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Time-Delay Systems *Example 1*

Temperature Measurement of Heat-Exchanger Output



$$v = velocity$$

$$d = distance$$

$$b(t) = a(t - T_l)$$

$$T_i = \frac{d}{v}$$

Time-Delay Systems

Example 2

Thickness Measurement of Rolled Steel Plate



Difference Between Time-Lag and Time-Delay



✓ In case (c), transfer function of the block = $G(s) = \frac{e^{-sT_l}}{1+sT}$, T = time lag, T_l = delay Problem due to Presence of Time-Delay in a Process Control Loop

 Due to the presence of time-delay, any corrective action from the controller cannot be immediately applied to the process. Thus during that time, process may buildup a deviation, sometimes quite large, due to any load disturbance or change in set-point.



Effect of Time-Delay on Process Loop Response T.F. of a Process with Time-Delay: $\Box = G(s) = G'(s)e^{-sT_l}$

where G'(s) is the transfer function of the delay free part of the process.

Case Study: Proportional Control of a First-Order Process with Time-Delay



 K_p = Proportional Gain of the Controller

T = **Process Time Constant**





✓ *Conclusion:* Time-delay may cause instability even in first-order system for large values of K_p.





σ

K_c: Critical Gain





R(s)



 $K_{p} = K_{\overline{c}}$

Case Study: Proportional Control of a First-Order Process with Time-Delay (contd ...)





✓ The Critical gain falls with increasing T_l .

Bode Plot

Case I: First Order System without Time-Delay



✓ *Conclusion:* The phase plot never crosses – 180° line, hence the system is always stable.

Bode Plot

Case II: First Order System with Time-Delay

Open Loop Transfer Function:
$$G(s) = \frac{K_p e^{-sT_l}}{1+sT} = \left(\frac{K_p}{1+sT}\right) e^{-sT_l} = G_1(s)G_2(s)$$

Frequency Response of Time-Delay Unit:



Bode Plot

Case II: First Order System with Time-Delay

Open Loop Transfer Function:
$$G(s) = \frac{K_p e^{-sT_l}}{1+sT} = \left(\frac{K_p}{1+sT}\right) e^{-sT_l} = G_1(s)G_2(s)$$







The time response from a system with closed loop transfer function :

$$\frac{G_c'(s)G'(s)}{1+G_c'(s)G'(s)}e^{-sT_l} \quad \text{will be } \mathbf{y} (\mathbf{t} - \mathbf{T}_l).$$

✓ Let the same response (i.e. y $(t - T_l)$) be available from a controller $G_c(s)$ and the process with time-delay G(s) in a unity feedback closed loop system.



 $G_{c}(s)$: T.F. of the required controller for the process with time-delay

The Realization of the Controller $G_c(s)$



✓ For the above realization of G_c(s), knowledge of G'(s) and T_l is required.
 ✓ In practice, model estimates of G'(s) and T_l are used.

Model Estimates:
$$\begin{cases} \hat{G}'(s), \text{ model of } G'(s) \\ \hat{T}_l, \text{ model of } T_l \end{cases}$$

The Realization of the Controller $G_c(s)$



 $G'_{c}(s)$: The Controller for Delay-Free Process G'(s)

Realisation of the Closed Loop System with $G_c(s)$ **Scheme I:**



Realisation of the Closed Loop System with $G_c(s)$ **Scheme II:**



Realisation of the Closed Loop System with $G_c(s)$ **Scheme III:**



✓ Smith's method assumes that models are exact, i.e. $\hat{G}'(s) = G'(s)$ and $\hat{T}_l = T_l$. ✓ In practice, there is always some mismatch between the model and the actual parameters, therefore, the closed-loop response may differ depending upon the degree of mismatch.

Realisation of the Closed Loop System with $G_c(s)$ **Scheme III:**



✓ The model of delay free process provides an estimate of output from delay free process for the controller. The estimate is, in fact, the prediction of the process output. Thus the term *Smith's Predictor* is used for such controllers.

