

**M.E. CHEMICAL ENGINEERING FIRST YEAR SECOND SEMESTER – 2025
ADVANCED MASS TRANSFER**

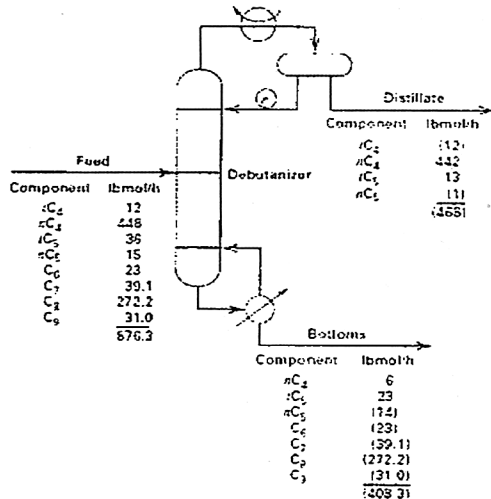
Time: 3 Hours

Full Marks:100

Answer any two questions between 1-3 and 4-6 (total 4 questions to be answered)

Assume any missing data

1. a) Identify light-key, heavy-key, light non key and heavy non key components from the following schematic and justify. [8]



- b) Write what the different steps involved in Naphtali-Sandholm method are to solve multicomponent distillation problems. [17]
2. a) Write down the heuristic of Thiele Geddes method? [15]
 b) What are the basic differences between BP, SR, NR and ISR method? [10]
3. a) A mixture of ortho, meta, and para-mononitrotoluenes containing 45% ortho, 10 mol% meta and 45% mol para mononitrotoluene is to be continuously distilled to give a top product of 98mol% ortho and the bottom is to contain 12% ortho.
 The mixture is to be distilled at a bottom temperature of $T_B = 410\text{K}$ requiring a pressure in the boiler of about 6KN/m^2 . If a reflux ratio of 8 is used, how many ideal plates will be required and what will be the approximate compositions of the product streams? Use Lewis Matheson method to calculate. The volatility of ortho relative to para is 1.7 and of the meta is 1.16 over the temperature range of 380-415kN. [20]
 b) Write MESH equation for multicomponent distillation. Clearly mention the assumptions. [5]
4. a) Water vapor in an air stream is to be adsorbed in a 15-cm-i.d. column packed with 3.1-mm-diameter Alcoa F-200 activated alumina beads of external porosity of 0.6. At a location in the bed where the pressure is 653.3 kPa, temperature is 21°C, gas flow rate is 1.327 kg/minute, and dew-point temperature is 11.2 °C, estimate the external, gas-to-particle mass-transfer and heat-transfer coefficients. At dew point temp vap pr of water is 1.32kPa. $C_p = 1.09\text{KJ/Kg. K}$; $k = 0.0256\text{ J/m.s.K}$; $\mu = 183\text{ micropoise}$ [20]
 b) Derive an expression for the length of unused bed. What is the mass transfer zone in a fixed bed adsorber? [5]
5. a) Derive BET equation and clearly state all the assumptions. [10]
 b) A 70 mol% propane and 30 mol% propylene gas mixture is to be separated into products containing 15 and 85 mol% propane by adsorption in a continuous, countercurrent system operating at 25°C and 1 atm. The adsorbent is silica gel, for which equilibrium data are given below. Determine

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by the McCabe–Thiele method the: (a) adsorbent flow rate per 1,000 m³ of feed gas at 25°C and 1 atm for 1.2 times the minimum, and (b) number of stages required. [15]

Total Pressure, torr	Millimoles of Mixture Adsorbed/g	y _C , Mole Fraction in Gas Phase	x _C , Mole Fraction in Adsorbate
769.2	2.197	0.2445	0.1078
760.9	2.013	0.299	0.2576
767.8	2.052	0.4040	0.2956
761.0	2.041	0.530	0.2816
753.6	1.963	0.5333	0.3655
766.3	1.967	0.5356	0.3120
754.0	1.974	0.6140	0.3591
753.6	1.851	0.6220	0.5550
754.0	1.701	0.6252	0.7007
760.0	1.686	0.7480	0.723
—	2.180	0.671	0.096
760.0	1.993	0.8964	0.253
760.0	1.426	0.921	0.401

6. a) Water containing 3.3 mg/L of trichloroethylene (TCE) is to be treated with activated carbon to obtain an effluent with only 0.01 mg TCE/L. At 25°C, adsorption-equilibrium data for TCE on activated carbon are correlated with the Freundlich equation: [20]

$$q = 67 c^{0.564}$$

where, q = mg TCE/g carbon and c = mg TCE/L solution. TCE is to be removed by slurry adsorption using powdered activated carbon with an average d_p of 1.5 mm. Assume the small-particle absorption rate is controlled by external mass transfer with a Sherwood number of 30. Particle surface area is 5 m²/kg. The molecular diffusivity of TCE in low concentrations in water at 25°C may be obtained from the Wilke–Chang equation.

- a) Determine the minimum amount of adsorbent needed.
- b) For operation in the batch mode with twice the minimum amount of adsorbent, determine the time to reduce TCE content to the desired value.
- c) For operation in the continuous mode using twice the minimum amount of adsorbent, obtain the required residence time.

Wilke Chang Equation: $D_{TCE,B} = \frac{7.4 \times 10^{-8} (\varphi_B \times M_B)^{\frac{1}{2}}}{\mu_B \times \vartheta_{TCE}^{0.6}}$, where $\vartheta_{TCE} = 98.1 \text{ cm}^3/\text{mol}$, $\mu_B = 0.94$, $M_B = 18$, $\varphi_B = 2.6$

b) Explain with the aid of diagrams Brauner’s five types of gas adsorption isotherms. [5]